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# **EUBIOGASFLARE Emissions Test Report**

Prepared for:

# **Packaging Corporation of America**

Packaging Corporation of America 2246 Udell Street Filer City, Michigan 49634

> Project No. 049AS-348563.01 July 3, 2018

BT Environmental Consulting, Inc. 4949 Fernlee Avenue Royal Oak, Michigan 48073 (248) 548-8070



#### **Executive Summary**

BT Environmental Consulting, Inc. (BTEC) was retained by Packaging Corporation of America (PCA) to perform testing for heat content and hydrogen sulfide (H<sub>2</sub>S), of the scrubber biogas routed to the EUBIOGASFLARE (biogas flare). The biogas flare is located at the PCA facility in Filer City, Michigan. Testing was conducted on May 16, 2018.



#### 1.0 Introduction

BT Environmental Consulting, Inc. (BTEC) was retained by Packaging Corporation of America (PCA) to perform testing for heat content and hydrogen sulfide (H<sub>2</sub>S), of the biogas routed to the EUBIOGASFLARE (biogas flare). The biogas flare is located at the PCA facility in Filer City, Michigan. All testing was performed in accordance with BTEC test plan 049AS-348563.

#### 1.1 Purpose of Test

Testing was done to demonstrate compliance with MDEQ permit number is MI-ROP-B3692-2015b, special conditions V.2 and VI.1 of FGBIOGASSYSTEM. The H<sub>2</sub>S limit is 4.49 lb/hr before combustion in a boiler or flare. The SO2 limit is 8.45 lb/hr exiting the boiler or flare and is calculated by assuming complete combustion of H<sub>2</sub>S to SO<sub>2</sub>. PCA is required by permit to document the BTU's in the biogas fuel on an annual basis.

#### 1.2 Test Date

This test program was performed on May 16, 2018.

#### 1.3 Project Contact Information

Affiliation	Address	Contact				
	Packaging Corporation of America	Ms. Sara Kaltunas				
Test Facility	2246 Udell Street	231-510-4689				
	Flier City, Michigan 49634	skaltunas@packagingcorp.com				
Test Facility	Packaging Corporation of America	Mr. Dyllan Walker				
	2246 Udell Street	231-510-4689				
	Flier City, Michigan 49634	dyllanwalker@packagingcorp.com				
Tagt Compony	BT Environmental Consulting, Inc.	Mr. Barry Boulianne				
Test Company	4949 Fernlee Avenue	313-449-2361				
Representative	Royal Oak, Michigan 48073	bboulianne@montrose-env.com				

This test program was performed by Todd Wessel and David Trahan of BTEC. Mr. Dyllan Walker of PCA coordinated the test events for this project.

#### 1.4 Summary of Results

A summary of H<sub>2</sub>S results is presented in Table 1. Detailed results can be found appended to this report.



Table 1
Summary of EUBIOGASFLARE Emission Rates

Sampling Location	Target Analyte	Emission Rate (lb/hr)	Permit Limit (lb/hr)		
	post combustion H <sub>2</sub> S	0.0253	0.0449		
SVBIOGASFLARE	pre combustion H <sub>2</sub> S	2.49	4.49		
	$SO_2$	4.77	8.45		

The average higher heating value (HHV) of the biogas was measured to be 677 British thermal units per dry standard cubic foot (Btu/dscf). Detailed results are contained in Appendix B.

#### 2.0 Process Description

PCA operates the biogas flare as part of the FGBIOGASSYSTEM that is used to combust biogas during upset or malfunction conditions that may occur with the biogas generating system or the combustion boilers. If no upset conditions occur in the process, the biogas is directed to Boiler No. 4 (EUBOILER4A) and combined with natural gas to generate steam for various mill process operations, and for electrical generation.

#### 3.0 Reference Methodologies

Triplicate thirty (30)-minute test runs were performed on the biogas prior to the scrubber in accordance with specifications stipulated in ASTM D-5504 and in accordance with MDEQ requirements.

A minimum vacuum of 5 inches of mercury is required on the evacuated summa canister to ensure proper sample collection. All test runs were stopped once the minimum vacuum was attained.

#### 3.1 Hydrogen sulfide

Hydrogen Sulfide concentrations were determined following ASTM guidelines as described in ASTM D-5504. The samples were extracted using evacuated summa canisters with low flow regulators. The sample stream was vented and aspirated to the summa canister for collection. Samples were labeled and immediately shipped for analysis within the required 24-hour period.

#### 4.0 Quality Assurance

Each promulgated method described above is accompanied by a statement indicating that to obtain reliable results, persons using these methods should have a thorough knowledge of the techniques associated with each. To that end, BTEC attempts to minimize any factors in the field that could increase error by implementing a quality assurance program into every testing activity segment.

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#### 5.0 Discussion of Results

The measured average biogas flare H<sub>2</sub>S emission rates are less than MDEQ permit Number MI-ROP-B3692-2015b requirements.

#### **MEASUREMENT UNCERTAINTY STATEMENT**

Both qualitative and quantitative factors contribute to field measurement uncertainty and should be taken into consideration when interpreting the results contained within this report. Whenever possible, Montrose Air Quality Services, LLC, (MAQS) personnel reduce the impact of these uncertainty factors through the use of approved and validated test methods. In addition, MAQS personnel perform routine instrument and equipment calibrations and ensure that the calibration standards, instruments, and equipment used during test events meet, at a minimum, test method specifications as well as the specifications of our Quality Manual and ASTM D 7036-04. The limitations of the various methods, instruments, equipment, and materials utilized during this test have been reasonably considered, but the ultimate impact of the cumulative uncertainty of this project is not fully identified within the results of this report.

#### Limitations

All testing performed was done in conformance to the ASTM D7036-04 standard. The information and opinions rendered in this report are exclusively for use by PCA. BTEC will not distribute or publish this report without PCA's consent except as required by law or court order. BTEC accepts responsibility for the competent performance of its duties in executing the assignment and preparing reports in accordance with the normal standards of the profession, but disclaims any responsibility for consequential damages.

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Field Technician

This report was reviewed by: Bronden Chaoc

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Table 2
EUBIOGASFLARE H<sub>2</sub>S and SO<sub>2</sub> Concentrations and Emission Rates

 Start
 End

 Test 1
 5/16/2018 14:51
 5/16/2018 15:21

 Test 2
 5/16/2018 15:23
 5/16/2018 15:53

 Test 3
 5/16/2018 15:56
 5/16/2018 16:26

 PH:FI432.PE
 FH:FI432.PE

#### RESULTS

	H₂S Conc.		Average Flow (60°F & 1 atm) Standard flow		v (70°F & 1 atm)	Mass Flow (total)		Emitted <sup>1</sup>		Emitted <sup>2</sup>		
Test 1	2976	ppm	169.00	dcfm	172.250	dscfm	2.706	lb/hr H₂\$	0.0271	lb/hr H₂S	5.093	lb/hr SO <sub>2</sub>
Test 2	2423	ppm	184.00	dcfm	187.538	dscfm	2.398	lb/hr H₂S	0.0240	lb/hr H₂S	4.515	lb/hr SO <sub>2</sub>
Test 3	2933	ppm	158.00	dcfm	161.038	dscfm	2.493	lb/hr H₂S	0.0249	ib/hr H₂S	4.693	lb/hr SO <sub>2</sub>
						Average	2.532	lb/hr H₂S	0.0253	lb/hr H₂S	4.767	lb/hr SO₂

<sup>&</sup>lt;sup>1</sup> Calculated by assuming 99% destruction of H<sub>2</sub>S during combustion

### CALCULATIONS:

Converting PPMvd to lb/hr:

$$\frac{lb-mole\ pollutant}{\mathit{MM}\ lb-mole\ air} \times \frac{lb\ pollutant}{lb-mole\ pollutant} \times \frac{lb-mole\ air}{386.5\ ft^3\ air} \times \frac{ft^3\ air}{min} \times \frac{60\ min}{hr} = lb/hr$$

$$\frac{2933 \ lb - mole \ H2S}{MM \ lb - mole \ biogas} \times \frac{34 \ lbs \ H2S}{1 \ lb - mol \ H2S} \times \frac{1 \ lb - mole \ biogas}{386.5 \ ft^3 \ biogas} \times \frac{161.038 \ ft^3 \ biogas}{min} \times \frac{60 \ min}{hr} = 2.493 \frac{lb}{hr} H2S$$

Converting flow to DSCFM (70°F & 1 atm) from DCFM (60°F & 1 atm):

$$Q_{scfm} = Q_{acfm} \times \frac{460 + 70^{\circ}F}{460 + T_o} \times \frac{P_o}{P_s}$$

$$161.038_{scfm} = 158.00_{acfm} \times \frac{460 + 70^{\circ}F}{460 + 60^{\circ}F} \times \frac{1 \ atm}{1 \ atm}$$

Where:

Po = Pressure at multivariable flow meter (1 atm)

To = Temperature at multivariable flow meter (60°F)

Converting H2S lbs/hr to SO2 lbs/hr:

$$H_2S + 1.5O_2 \rightarrow SO_2 + H_2O$$

$$\frac{lb \; H2S}{hr} \times \frac{1 \; lb - mole \; H2S}{34 \; lbs \; H2S} \times \frac{1 \; lb - mole \; SO2}{1 \; lb - mole \; H2S} \times \frac{64 \; lbs \; SO2}{1 \; lb - mole \; SO2} = \frac{lb}{hr} SO2$$

$$\frac{2.493 \ lb \ H2S}{hr} \times \frac{1 \ lb - mole \ H2S}{34 \ lbs \ H2S} \times \frac{1 \ lb - mole \ SO2}{1 \ lb - mole \ H2S} \times \frac{64 \ lbs \ SO2}{1 \ lb - mole \ SO2} = 4.693 \frac{lb}{hr} SO2$$

<sup>&</sup>lt;sup>2</sup> Calculated by assuming complete combustion of H<sub>2</sub>S to SO<sub>2</sub>

