

MICHIGAN DEPARTMENT OF ENVIRONMENTAL QUALITY

INTEROFFICE COMMUNICATION

TO: Caryn Owens, Cadillac District Office
Field Operations Section, Air Quality Division

FROM: Jeremy Howe, Cadillac District Office
Field Operations Section, Air Quality Division

DATE: November 14, 2013

SUBJECT: SRN B1824, MI-ROP-B1824-2008b
EUPELLETCOOLING
EUPELLPROD
EU#6BOILER

JH

The report of emission testing at Morton Salt in Manistee has been reviewed. The following sources were tested:

- EU#6BOILER
 - Particulate Matter (PM)
 - Sulfur Dioxide (SO₂)
- EUPELLPROD
 - PM
- EUPELLETCOOLING
 - PM

This testing was required by MI-ROP-B1824-2008b.

The test protocol was received June 26, 2013 and approved July 1, 2013. The testing was performed August 6 and 7, 2013. The report was received September 3, 2013. The results for tests are as follows:

Emission Unit	Pollutant	Permit Limit	Test Result	% of Limit	Unit
EUPELLETCOOLING	PM	0.032	0.004	12.5	lb/1000lb
EUPELLPROD	PM	0.03	0.01	33.3	lb/1000lb dry
EU#6BOILER	PM	0.30	0.02	6.7	lb/1000lb @ 50% EA
EU#6BOILER	SO ₂	2.5	1.4	56.0	lb/mmBtu

Methodology and Results

Testing was performed in accordance with 40 CFR, Part 60, Appendix A, Methods 1, 2, 3A, 4, 5 and 6C. Testing was performed with the EU#6BOILER producing steam at 125 kpph; the facility contact stated that this was its maximum capacity. SO₂ was determined using Method 6C, PM was determined using Method 5.

Report/Testing Issues

- EUPELLETCOOLING
 - Method 1
 - Ports were not aligned at 90 degrees to each other
 - Ports are supposed be aligned at 90 degrees to each other per Section 11.3.1.1
 - Method 2
 - Cyclonic flow check not adequately documented
 - Method 2 cannot be used if cyclonic conditions exist per Section 1.2
- EUPELLPROD
 - Method 1
 - Outside points were located within one inch of stack wall
 - Not allowed per Section 11.3.2.1
 - Method 2
 - Cyclonic flow check not adequately documented
 - Method 2 cannot be used if cyclonic conditions exist per Section 1.2
 - Method 17
 - Run 1 Port 2 Point 1 not sampled isokinetically (119.0%)
 - Run 2 Port 2 Point 7 not sampled isokinetically (82.7%)
 - Run 2 Port 2 Point 6 not sampled isokinetically (121.3%)
 - Run 3 Port 2 Point 6 not sampled isokinetically (116.2%)
 - Method 17 Section 8.1.5 refers to Method 5 for Sample Train Operation
 - A sampling rate of 90%-110% isokinetic must be maintained throughout the sampling run per Method 5 Section 8.5
- EU#6BOILER
 - Method 2
 - Cyclonic flow check not adequately documented
 - Method 2 cannot be used if cyclonic conditions exist per Section 1.2
 - Method 6C
 - Cylinder gases used were outside of SO₂ observed
 - Method 6C Section 7.1 refers to Method 7E Section 7.1 for calibration gas requirements
 - Cylinder gases do not meet requirements in Method 7E Section 7.1

Discussion

Location of traverse points within an inch of the wall does not affect results to an appreciable amount. The points were only a quarter of an inch off and during sampling the probe could be off by this much at any point. Furthermore, being close to the wall could bias the results high as particles collected on the wall could come off and become a part of the sample.

Cyclonic flow check was not documented adequately on any stack. All that was recorded was something to the effect of " Cyc Flow Ck = OK < 5° ". This is not documentation, but a summary. It would be similar if the tester reported only the highest one minute average for SO₂ on each run and used this to compare against the limit. Furthermore, EUPELLETCOOLING cyclonic flow check was not done on both ports. EUPELLETCOOLING also had a strange flow profile in that the highest flow was not in the middle of the stack. EUPELLETCOOLING has a wet scrubber upstream which looked like it was designed to induce cyclonic flow. Adding to the complications EUPELLETCOOLING ports did not allow for sampling in equal areas of the stack since they were at 45 degrees to each other.

Cyclonic flow is a problem and not allowed because either the tester is measuring the flow of the flue gas as it moves up the stack and not catching the particulate because the nozzle is not pointed into the flow or the nozzle is into the flow stream, but the flow being measured is flue gas swirling around the inside of the stack.

It is not uncommon that a couple of points would not be sampled isokinetically. EUPELLETPROD need to be sampled at 24 points, which means the tester had to change points every 2.5 minutes. There is a lot to accomplish at each point, so it is not surprising a couple were off. The vast majority of points passed isokinetics and each run overall passed.

All PM limits were in units of lb/1000lbs. This is a density or concentration unit; flow is not used in the calculations. However, PM has to be sampled isokinetically which involves the flow rate in its calculation and also pointing the probe into the flow. It would be difficult to evaluate a PM result if cyclonic flow existed. However, these tests are not completely useless. No source tested had a result greater than a third of its limit. This means that the results would have to be off by at least two orders of magnitude to show a violation. There are a fair number of safeguards in the methods to allow for a variety of stack conditions and human error and almost no test is done without some issue. Thus, it is difficult to imagine that any of the tested sources are emitting more than their PM limits, even though we may not have the most accurate number to go by.

Finally, SO₂ calibration cylinders were not sized correctly. However, the lowest cylinder (848.9 ppm) corresponded to their EU#6BOILER limit of 2.5 lb/mmBtu. EPA has cylinder values sized in their methods to provide linearity over a wide range. Linearity is not a worry here since their limit was a point and not somewhere between two points.

Of note, EU#6BOILER SO₂ varied a fair amount during the three runs. SO₂ ppm went from 300 to 500 during Run 1, stayed at 500 ppm for Run 2, and went from 500 down to 400 for Run 3. I am not sure what if anything this means, but encourage you to look at the graph in the attachments.

Summary

See the attached summary sheet for results. These results are acceptable with reservation to the AQD and can be used to determine compliance. Please review the process data included in the report to make a final compliance determination.

If you have any questions regarding this review, please contact me by telephone at 231-876-4416, or by e-mail at howej1@michigan.gov

JH:
Attachments



PITOT TRAVERSE DATA FORM	Date: <u>8/6/13</u>
Plant: <u>Mortons Salt</u>	
Source: <u>Pellet Cooler</u>	Staff: <u>BIRD/Erdmanns</u>
Stack Size, Inches <u>1716"</u>	Barometric Pressure, "Hg <u>29.10</u>
Gas Temperature, °F Dry _____ Wet _____	Static Pressure, "H ₂ O <u>-1.8</u>
Pitot Tube# <u>3</u>	Standard S-Type C _p <u>0.82</u>

Point Location Inches	Port	Velocity Pressure "H ₂ O		Port	Velocity Pressure "H ₂ O		Port	Velocity Pressure "H ₂ O		Port	Velocity Pressure "H ₂ O	
		1	2		3	4		5	6		7	8
0.75	1	1.7	80	1			1			1		
2.48	2	1.7	80	2			2			2		
5.03	3	2.1	80	3			3			3		
11.97	4	2.5	80	4			4			4		
14.52	5	3.4	80	5			5			5		
16.25	6	3.7	80	6			6			6		
	7			7			7			7		
	8			8			8			8		
	9			9			9			9		
	10			10			10			10		
	11			11			11			11		
	12			12			12			12		

Wall Thickness	
Zero Point	<u>1.5"</u>
Port Size/Type	<u>3" Coup</u>

The diagram shows a vertical pipe section with a horizontal nozzle at the bottom. A vertical line from the top is labeled '1.5"'. A vertical line from the nozzle is labeled '1.70' with a note 'OK -2'. A vertical line from the nozzle is labeled '1.50'. A note 'NW' is near the nozzle. A handwritten note below the diagram says 'Ports 45° to each other and not 90°'.

Cyc Flow Ck = 0.2 < 5°

1.01140 GRS
1 14310

Nozzle = 0.182

0.182

0.182

Morton Salt Pellet Cooler 2013-08-06

Plant:	<i>Morton Salt</i>	Capacity during Test:	
Permit #:	<i>MI-ROP-B1824-2008b</i>	Design Capacity:	
SRN:	<i>B1824</i>	SCC Code:	
Tested by:	<i>Network</i>	Date Tested:	<i>August 6, 2013</i>
Reviewed By:	<i>Jeremy Howe</i>	Date Reviewed:	<i>November 13, 2013</i>
Pollutants:	<i>PM</i>	Purpose of Test:	<i>Compliance</i>
Source:	<i>EUEPLETECOOLING</i>		

<i>Ib/1000lb, Actual</i>								<i>Notes:</i>
Run #	particulate mg	gas sampled lb/ft ³	gas sampled lb	part conc lb/1000lb	iso %	iso max %	iso min %	
1	9.60	0.07422	4.031	0.005	100.5	102.8	98.2	
2	5.80	0.07408	4.023	0.003	101.4	104.4	98.7	
3	7.30	0.07399	4.019	0.004	101.3	103.2	98.6	
Avg	7.57	0.07410	4.024	0.004				
Limit				0.032				

Duct Diameters	dd	TP Needed	TP Chosen	TP per Diameter				
Upstream from disturbance (dd)	6.35	12		0				
Downstream from disturbance (dd)	8.47	12	12	6				
					6 Traverse Points Needed Each Diameter			
					Comments			
<p>Minimum Number of Traverse Points</p> <p>Duct Diameters Upstream from Flow Disturbance* (Distance A)</p> <p>Duct Diameters Downstream from Flow Disturbance* (Distance B)</p> <p>a Higher Number is for Rectangular Stacks or Ducts</p> <p>* From Point of Any Type of Disturbance (Bend, Expansion, Contraction, etc.)</p> <p>Stack Diameter > 0.61 m (24 in.)</p> <p>Stack Diameter = 0.30 to 0.61 m (12-24 in.)</p> <p>Disturbance</p> <p>Measurement Site</p> <p>Disturbance</p> <p>24 or 25^a</p> <p>20</p> <p>16</p> <p>12</p> <p>8 or 9^a</p> <p>0.5 1.0 1.5 2.0 2.5</p> <p>0 10 20 30 40 50</p> <p>2 3 4 5 6 7 8 9 10</p>								
					Cyclonic flow not documented adequately. Ports not aligned at 90 degrees.			
Traverse Point #	Fraction of Stack	Distance far wall to outside of port	Port Length	Stack Diameter	Distance from far wall	Distance from far wall + port	Consultant Distance from far wall + port	Difference
1	4.4	0.00	0.00	17.00	1.00	1.00	0.75	-0.25
2	14.6	0.00	0.00	17.00	2.48	2.48	2.48	0.00
3	29.6	0.00	0.00	17.00	5.03	5.03	5.03	0.00
4	70.4	0.00	0.00	17.00	11.97	11.97	11.97	0.00
5	85.4	0.00	0.00	17.00	14.52	14.52	14.52	0.00
6	95.6	0.00	0.00	17.00	16.00	16.00	16.25	0.25
7	0.0	0.00	0.00	17.00	0.00	0.00		0.00
8	0.0	0.00	0.00	17.00	0.00	0.00		0.00
9	0.0	0.00	0.00	17.00	0.00	0.00		0.00
10	0.0	0.00	0.00	17.00	0.00	0.00		0.00
11	0.0	0.00	0.00	17.00	0.00	0.00		0.00
12	0.0	0.00	0.00	17.00	0.00	0.00		0.00

<http://www.epa.gov/ttn/emc/promgate/m-01.pdf>

Run 1																
Flow Traverse				Dry Gas Meter			Isokinetics	O2 Content of Gas Stream			20.90	% by Volume		Dry		
Port-Pt	Stack Tp (F)	ΔP (in H2O)	Sq Rt ΔP	Tp In (F)	Tp Out (F)	Samp Vol (ft³)	%	CO2 Content of Gas Stream			0.00	% by Volume		Dry		
Avg	82.3	2.48	1.558	75.8		55.808	100.5	Ar Content of Gas Stream			0.90	% by Volume		Dry		
Start						663.238		N2+CO Content of Gas Stream			78.20	% by Volume		Dry		
1-12	82	3.10	1.761	70	70	668.350	98.8	Diameter of Stack			17.00	in				
1-11	82	3.10	1.761	70	70	673.490	99.3	Cross Sectional Area of Stack			1.58	ft²				
1-10	82	2.50	1.581	75	69	678.270	102.4	DGM Cal Factor	Y		0.9945	Dimensionless				
1-9	82	2.30	1.517	79	70	682.760	99.9	Pitot Tube Cal Factor	Cp		0.82	Dimensionless				
1-8	82	1.90	1.378	82	70	686.930	101.8	Velocity Head of Stack Gas	$\sqrt{\Delta p_{avg}}$		1.56	in H2O				
1-7	82	1.40	1.183	83	71	690.550	102.7	Stack Temp	Ts		82.33	F				
1-6								Absolute Stack Temp	Ts(abs)		542.33	R				
1-5								Stack Static Pressure			-1.80	in H2O				
1-4								Stack Static Pressure	Pg		-0.1324	in Hg				
1-3								Barometric Pressure	Pbar		29.10	in Hg				
1-2								Absolute Stack Pressure	Ps		28.97	in Hg				
1-1								Condensed H2O Vol @ STP	Vwc(std)	EQ 4-1	0.753	SCF				
2-12	82	3.40	1.844	78	71	695.920	98.2	Silica H2O Vol @ STP	Vwsg(std)	EQ 4-2	0.38	SCF				
2-11	83	3.50	1.871	83	72	701.500	100.2	DGM Vol @ STP	Vm(std)	EQ 4-3	53.18	DSCF				
2-10	83	2.90	1.703	85	73	706.620	100.7	Gas Stream H2O Vapor	Bws	EQ 4-4	0.021	Proportion by Vol				
2-9	83	2.10	1.449	85	73	710.960	100.4	Gas Stream Molecular Weight Dry	Md	EQ 3-1	28.94	lb/lb-mol				
2-8	83	1.90	1.378	85	74	715.150	101.8	Gas Stream Molecular Weight Wet	Ms	EQ 2-6	28.72	lb/lb-mol				
2-7	82	1.60	1.265	86	74	719.046	102.8	Gas Collected from Stack @ STP			54.31	SCF		Wet		
2-6								Moisture Collection Time			60	Minutes				
2-5								Gas Collection Rate			0.905	SCFM		Wet		
2-4								Nozzle Diameter			0.182	in				
2-3								Area of Nozzle	An		0.000181	ft²				
2-2								Average Stack Gas Actual Velocity	Vs	EQ 2-7	88	ft/sec	FS	Wet		
2-1								Average Stack Gas Actual Velocity			5,290	ft/min	FM	Wet		
Impingers										Average Stack Gas Actual Velocity		317,394	ft/hr	FH	Wet	
	1	2	3	Total 1-3	Silica	Total		Average Stack Gas Actual Flow			139	ft³/sec	ACFS	Wet		
Final				16.0	16.0	8.0		Average Stack Gas Actual Flow			8,338	ft³/min	ACFM	Wet		
Initial					0.0			Average Stack Gas Actual Flow			500,292	ft³/hr	ACFH	Wet		
Gain	0.0	0.0	16.0	16.0	8.0	24.0		Average Stack Gas Flow @ STP			131	ft³/sec	SCFS	Wet		
Comments										Average Stack Gas Flow @ STP		7,884	ft³/min	SCFM	Wet	
Thousands digit not recorded on intermediate points.										Average Stack Gas Flow @ STP		473,057	ft³/hr	SCFH	Wet	
										Average Stack Gas Dry Flow @ STP		129	ft³/sec	DSCFS	Dry	
										Average Stack Gas Dry Flow @ STP		7,720	ft³/min	DSCFM	Dry	
										Average Stack Gas Dry Flow @ STP	Q	EQ 2-8	463,213	ft³/hr	DSCFH	Dry

Notes: To edit sheet just unprotect it under the "Review" tab. Metric flows: m³/hr = ft³/min x 1.7

Run 2

Flow Traverse										Dry Gas Meter			Isokinetics		O2 Content of Gas Stream			20.90	% by Volume		Dry
Port-Pt	Stack Tp (F)	ΔP (in H2O)	Sq Rt ΔP	Tp In (F)	Tp Out (F)	Samp Vol (ft³)	%	CO2 Content of Gas Stream							0.00	% by Volume		Dry			
Avg	82.8	2.65	1.610	82.0		58.613	101.4	Ar Content of Gas Stream						0.90	% by Volume		Dry				
Start						718.980		N2+CO Content of Gas Stream						78.20	% by Volume		Dry				
1-12	81	3.30	1.817	76	74	724.600	104.4	Diameter of Stack						17.00	in						
1-11	83	3.60	1.897	82	74	730.210	99.6	Cross Sectional Area of Stack						1.58	ft²						
1-10	82	2.90	1.703	87	75	735.340	100.8	DGM Cal Factor	Y					0.9945	Dimensionless						
1-9	82	2.20	1.483	88	76	739.880	102.2	Pitot Tube Cal Factor	Cp					0.82	Dimensionless						
1-8	82	1.90	1.378	89	76	744.120	102.6	Velocity Head of Stack Gas	$\sqrt{\Delta p_{avg}}$					1.61	in H2O						
1-7	82	1.80	1.342	90	77	748.198	101.2	Stack Temp	Ts					82.75	F						
1-6								Absolute Stack Temp	Ts(abs)					542.75	R						
1-5								Stack Static Pressure						-1.80	in H2O						
1-4								Stack Static Pressure	Pg					-0.1324	in Hg						
1-3								Barometric Pressure	Pbar					29.10	in Hg						
1-2								Absolute Stack Pressure	Ps					28.97	in Hg						
1-1								Condensed H2O Vol @ STP	Vwc(std)	EQ 4-1				1.035	SCF						
2-12	82	3.80	1.949	85	77	753.950	98.7	Silica H2O Vol @ STP	Vwsg(std)	EQ 4-2				0.42	SCF						
2-11	83	3.80	1.949	89	78	759.760	99.4	DGM Vol @ STP	Vm(std)	EQ 4-3				55.21	DSCF						
2-10	84	2.80	1.673	91	78	764.840	101.3	Gas Stream H2O Vapor	Bws	EQ 4-4				0.026	Proportion by Vol						
2-9	84	2.10	1.449	90	79	769.330	103.4	Gas Stream Molecular Weight Dry	Md	EQ 3-1				28.94	lb/lb-mol						
2-8	84	1.80	1.342	90	79	773.480	103.2	Gas Stream Molecular Weight Wet	Ms	EQ 2-6				28.66	lb/lb-mol						
2-7	84	1.80	1.342	89	79	777.593	102.4	Gas Collected from Stack @ STP						56.67	SCF		Wet				
2-6								Moisture Collection Time						60	Minutes						
2-5								Gas Collection Rate						0.944	SCFM		Wet				
2-4								Nozzle Diameter						0.182	in						
2-3								Area of Nozzle	An					0.000181	ft²						
2-2								Average Stack Gas Actual Velocity	Vs	EQ 2-7				91	ft/sec	FS	Wet				
2-1								Average Stack Gas Actual Velocity						5,477	ft/min	FM	Wet				
Impingers										Average Stack Gas Actual Velocity					328,593	ft/hr	FH	Wet			
	1	2	3	Total 1-3	Silica	Total		Average Stack Gas Actual Flow						144	ft³/sec	ACFS	Wet				
Final				22.0	22.0	9.0		Average Stack Gas Actual Flow						8,632	ft³/min	ACFM	Wet				
Initial					0.0			Average Stack Gas Actual Flow						517,945	ft³/hr	ACFH	Wet				
Gain	0.0	0.0	22.0	22.0	9.0	31.0		Average Stack Gas Flow @ STP						136	ft³/sec	SCFS	Wet				
Comments										Average Stack Gas Flow @ STP					8,156	ft³/min	SCFM	Wet			
Thousands digit not recorded on intermediate points.										Average Stack Gas Flow @ STP					489,373	ft³/hr	SCFH	Wet			
										Average Stack Gas Dry Flow @ STP					132	ft³/sec	DSCFS	Dry			
										Average Stack Gas Dry Flow @ STP					7,946	ft³/min	DSCFM	Dry			
										Average Stack Gas Dry Flow @ STP			Q	EQ 2-8	476,767	ft³/hr	DSCFH	Dry			

Notes: To edit sheet just unprotect it under the "Review" tab. Metric flows: m³/hr = ft³/min × 1.7

Run 3

Flow Traverse				Dry Gas Meter			Isokinetics	O2 Content of Gas Stream			20.90	% by Volume		Dry
Port-Pt	Stack Tp (F)	ΔP (in H ₂ O)	Sq Rt ΔP	Tp In (F)	Tp Out (F)	Samp Vol (ft ³)	%	CO2 Content of Gas Stream			0.00	% by Volume		Dry
Avg	84.2	2.57	1.585	83.0		57.549	101.3	Ar Content of Gas Stream			0.90	% by Volume		Dry
Start						778.459		N2+CO Content of Gas Stream			78.20	% by Volume		Dry
1-12	81	3.50	1.871	79	78	783.950	98.6	Diameter of Stack			17.00	in		
1-11	84	3.50	1.871	82	78	789.510	100.1	Cross Sectional Area of Stack			1.58	ft ²		
1-10	84	2.90	1.703	86	78	794.660	101.5	DGM Cal Factor	Y		0.9945	Dimensionless		
1-9	84	2.20	1.483	88	78	799.190	102.3	Pitot Tube Cal Factor	Cp		0.82	Dimensionless		
1-8	84	1.90	1.378	88	79	803.440	103.2	Velocity Head of Stack Gas	$\sqrt{\Delta p_{avg}}$		1.59	in H ₂ O		
1-7	84	1.60	1.265	88	79	807.337	103.1	Stack Temp	Ts		84.17	F		
1-6								Absolute Stack Temp	Ts(abs)		544.17	R		
1-5								Stack Static Pressure			-1.80	in H ₂ O		
1-4								Stack Static Pressure	Pg		-0.1324	in Hg		
1-3								Barometric Pressure	Pbar		29.10	in Hg		
1-2								Absolute Stack Pressure	Ps		28.97	in Hg		
1-1								Condensed H ₂ O Vol @ STP	Vwc(std)	EQ 4-1	1.224	SCF		
2-12	84	3.40	1.844	84	79	812.780	99.1	Silica H ₂ O Vol @ STP	Vwsg(std)	EQ 4-2	0.38	SCF		
2-11	85	3.30	1.817	86	79	818.350	103.0	DGM Vol @ STP	Vm(std)	EQ 4-3	54.11	DSCF		
2-10	85	2.90	1.703	88	79	823.450	100.4	Gas Stream H ₂ O Vapor	Bws	EQ 4-4	0.029	Proportion by Vol		
2-9	85	2.20	1.483	90	79	827.960	101.7	Gas Stream Molecular Weight Dry	Md	EQ 3-1	28.94	lb/lb-mol		
2-8	85	1.80	1.342	92	80	832.090	102.7	Gas Stream Molecular Weight Wet	Ms	EQ 2-6	28.63	lb/lb-mol		
2-7	85	1.60	1.265	94	80	836.008	103.2	Gas Collected from Stack @ STP			55.71	SCF		Wet
2-6								Moisture Collection Time			60	Minutes		
2-5								Gas Collection Rate			0.928	SCFM		Wet
2-4								Nozzle Diameter			0.182	in		
2-3								Area of Nozzle	An		0.000181	ft ²		
2-2								Average Stack Gas Actual Velocity	Vs	EQ 2-7	90	ft/sec	FS	Wet
2-1								Average Stack Gas Actual Velocity			5,402	ft/min	FM	Wet
Impingers							Average Stack Gas Actual Velocity							
	1	2	3	Total 1-3	Silica	Total		Average Stack Gas Actual Flow			142	ft ³ /sec	ACFS	Wet
Final				26.0	26.0	8.0		Average Stack Gas Actual Flow			8,514	ft ³ /min	ACFM	Wet
Initial					0.0			Average Stack Gas Actual Flow			510,852	ft ³ /hr	ACFH	Wet
Gain	0.0	0.0	26.0	26.0	8.0	34.0		Average Stack Gas Flow @ STP			134	ft ³ /sec	SCFS	Wet
Comments							Average Stack Gas Flow @ STP							
Thousands digit not recorded on intermediate points.								Average Stack Gas Flow @ STP			8,024	ft ³ /min	SCFM	Wet
								Average Stack Gas Flow @ STP			481,415	ft ³ /hr	SCFH	Wet
								Average Stack Gas Dry Flow @ STP			130	ft ³ /sec	DSCFS	Dry
								Average Stack Gas Dry Flow @ STP			7,793	ft ³ /min	DSCFM	Dry
								Average Stack Gas Dry Flow @ STP	Q	EQ 2-8	467,582	ft ³ /hr	DSCFH	Dry

Notes: To edit sheet just unprotect it under the "Review" tab. Metric flows: m³/hr = ft³/min x 1.7

Morton Salt Pellet Production 2013-08-06

Plant:	<i>Morton Salt</i>	Capacity during Test:	
Permit #:	<i>MI-ROP-B1824-2008b</i>	Design Capacity:	
SRN:	<i>B1824</i>	SCC Code:	
Tested by:	<i>Network</i>	Date Tested:	<i>August 6, 2013</i>
Reviewed By:	<i>Jeremy Howe</i>	Date Reviewed:	<i>November 13, 2013</i>
Pollutants:	<i>PM</i>	Purpose of Test:	<i>Compliance</i>
Source:	<i>EUEPLLPROD</i>		

<i>lb/1000lb, Dry</i>								<i>Notes:</i>
Run #	particulate mg	gas sampled lb/ft ³	gas sampled lb	part conc lb/1000lb	iso %	iso max %	iso min %	
1	16.20	0.07349	3.346	0.01	101.6	119.0	96.2	
2	11.10	0.07311	3.328	0.01	102.0	121.3	82.7	
3	14.70	0.07309	3.328	0.01	102.6	116.2	92.3	
Avg	14.00	0.07323	3.334	0.01				
Limit				0.03				

Duct	Diameters	dd	TP Needed	TP Chosen	TP per Diameter			
Upstream from disturbance (dd)	6.00	12		0				
Downstream from disturbance (dd)	2.00	24	24	12				
						12 Traverse Points Needed Each Diameter		
						Comments		
1. Minimum number of traverse points for particulate traverses.	<p>a Higher Number is for Rectangular Stacks or Ducts</p> <p>* From Point of Any Type of Disturbance (Bend, Expansion, Contraction, etc.)</p> <p>Stack Diameter > 0.61 m (24 in.)</p> <p>Stack Diameter = 0.30 to 0.61 m (12-24 in.)</p>							
						Outside points are less than 1 inch from wall. These need to be located at 1 inch per M-1 11.3.2.1. Cyclonic flow not documented adequately.		
Traverse Point #	Fraction of Stack	Distance far wall to outside of port	Port Length	Stack Diameter	Distance from far wall	Distance from far wall + port	Consultant Distance from far wall + port	Difference
1	2.1	0.00	0.00	36.00	1.00	1.00	0.76	-0.24
2	6.7	0.00	0.00	36.00	2.41	2.41	2.41	0.00
3	11.8	0.00	0.00	36.00	4.25	4.25	4.25	0.00
4	17.7	0.00	0.00	36.00	6.37	6.37	6.37	0.00
5	25.0	0.00	0.00	36.00	9.00	9.00	9.00	0.00
6	35.6	0.00	0.00	36.00	12.82	12.82	12.82	0.00
7	64.4	0.00	0.00	36.00	23.18	23.18	23.18	0.00
8	75.0	0.00	0.00	36.00	27.00	27.00	27.00	0.00
9	82.3	0.00	0.00	36.00	29.63	29.63	29.63	0.00
10	88.2	0.00	0.00	36.00	31.75	31.75	31.75	0.00
11	93.3	0.00	0.00	36.00	33.59	33.59	33.59	0.00
12	97.9	0.00	0.00	36.00	35.00	35.00	35.24	0.24

Run 1														
Flow Traverse				Dry Gas Meter			Isokinetics	O2 Content of Gas Stream			20.90	% by Volume		
Port-Pt	Stack Tp (F)	ΔP (in H2O)	Sq Rt ΔP	Tp In (F)	Tp Out (F)	Samp Vol (ft³)	%	CO2 Content of Gas Stream			0.00	% by Volume	Dry	
Avg	108.8	1.76	1.322	92.3		47.624	101.6	Ar Content of Gas Stream			0.90	% by Volume	Dry	
Start						175.806		N2+CO Content of Gas Stream			78.20	% by Volume	Dry	
1-12	109	1.90	1.378	85	84	177.820	100.4	Diameter of Stack			36.00	in		
1-11	109	1.95	1.396	84	84	179.980	106.4	Cross Sectional Area of Stack			7.07	ft²		
1-10	110	1.95	1.396	86	84	181.950	97.0	DGM Cal Factor	Y		1.0105	Dimensionless		
1-9	110	1.90	1.378	89	84	184.000	102.0	Pitot Tube Cal Factor	Cp		0.82	Dimensionless		
1-8	109	1.90	1.378	91	84	186.050	101.6	Velocity Head of Stack Gas	$\sqrt{\Delta p_{avg}}$		1.32	in H2O		
1-7	110	1.90	1.378	93	85	188.200	106.5	Stack Temp	Ts		108.79	F		
1-6	110	1.75	1.323	95	85	190.080	96.8	Absolute Stack Temp	Ts(abs)		568.79	R		
1-5	110	1.60	1.265	96	85	191.960	101.2	Stack Static Pressure			-0.85	in H2O		
1-4	111	1.50	1.225	97	86	193.740	98.9	Stack Static Pressure	Pg		-0.0625	in Hg		
1-3	111	1.40	1.183	98	86	195.520	102.3	Barometric Pressure	Pbar		29.10	in Hg		
1-2	110	1.25	1.118	99	87	197.190	101.2	Absolute Stack Pressure	Ps		29.04	in Hg		
1-1	108	1.20	1.095	99	87	198.806	99.6	Condensed H2O Vol @ STP	Vwc(std)	EQ 4-1	0.471	SCF		
2-12	109	2.00	1.414	94	87	200.870	99.2	Silica H2O Vol @ STP	Vwsg(std)	EQ 4-2	0.33	SCF		
2-11	109	2.00	1.414	98	88	202.990	101.4	DGM Vol @ STP	Vm(std)	EQ 4-3	44.73	DSCF		
2-10	108	1.90	1.378	100	88	205.070	101.7	Gas Stream H2O Vapor	Bws	EQ 4-4	0.018	Proportion by Vol		
2-9	108	1.95	1.396	101	88	207.140	99.8	Gas Stream Molecular Weight Dry	Md	EQ 3-1	28.94	lb/lb-mol		
2-8	108	1.65	1.285	102	89	209.080	101.5	Gas Stream Molecular Weight Wet	Ms	EQ 2-6	28.75	lb/lb-mol		
2-7	108	1.70	1.304	103	89	211.070	102.5	Gas Collected from Stack @ STP			45.53	SCF	Wet	
2-6	108	2.00	1.414	104	90	213.100	96.2	Moisture Collection Time			60	Minutes		
2-5	108	2.10	1.449	104	90	215.300	101.8	Gas Collection Rate			0.759	SCFM	Wet	
2-4	107	2.00	1.414	105	90	217.450	101.7	Nozzle Diameter			0.182	in		
2-3	107	1.85	1.360	105	91	219.500	100.7	Area of Nozzle	An		0.000181	ft²		
2-2	107	1.55	1.245	105	91	221.400	102.0	Average Stack Gas Actual Velocity	Vs	EQ 2-7	77	ft/sec	FS	Wet
2-1	107	1.30	1.140	105	91	223.430	119.0	Average Stack Gas Actual Velocity			4,590	ft/min	FM	Wet
Impingers								Average Stack Gas Actual Velocity			275,402	ft/hr	FH	Wet
	1	2	3	Total 1-3	Silica	Total		Average Stack Gas Actual Flow			541	ft³/sec	ACFS	Wet
Final				10.0	10.0	7.0		Average Stack Gas Actual Flow			32,445	ft³/min	ACFM	Wet
Initial					0.0			Average Stack Gas Actual Flow			1,946,699	ft³/hr	ACFH	Wet
Gain	0.0	0.0	10.0	10.0	7.0	17.0		Average Stack Gas Flow @ STP			489	ft³/sec	SCFS	Wet
Comments								Average Stack Gas Flow @ STP			29,322	ft³/min	SCFM	Wet
TP 2-1 not sampled isokinetically. Thousandths digit not recorded on intermediate points.								Average Stack Gas Flow @ STP			1,759,334	ft³/hr	SCFH	Wet
								Average Stack Gas Dry Flow @ STP			480	ft³/sec	DSCFS	Dry
								Average Stack Gas Dry Flow @ STP			28,807	ft³/min	DSCFM	Dry
								Average Stack Gas Dry Flow @ STP	Q	EQ 2-8	1,728,394	ft³/hr	DSCFH	Dry
Notes: To edit sheet just unprotect it under the "Review" tab. Metric flows: m³/hr = ft³/min × 1.7														

Run 2																
Flow Traverse				Dry Gas Meter			Isokinetics	O2 Content of Gas Stream			20.90	% by Volume		Dry		
Port-Pt	Stack Tp (F)	ΔP (in H2O)	Sq Rt ΔP	Tp In (F)	Tp Out (F)	Samp Vol (ft ³)	%	CO2 Content of Gas Stream			0.00	% by Volume		Dry		
Avg	109.6	1.74	1.317	96.7		47.758	102.0	Ar Content of Gas Stream			0.90	% by Volume		Dry		
Start					223.495			N2+CO Content of Gas Stream			78.20	% by Volume		Dry		
1-12	109	2.00	1.414	92	91	225.710	106.6	Diameter of Stack			36.00	in				
1-11	110	1.90	1.378	93	91	227.670	96.9	Cross Sectional Area of Stack			7.07	ft ²				
1-10	110	1.85	1.360	96	91	229.850	108.9	DGM Cal Factor	Y		1.0105	Dimensionless				
1-9	110	1.85	1.360	98	91	231.700	92.3	Pitot Tube Cal Factor	Cp		0.82	Dimensionless				
1-8	110	1.75	1.323	100	91	233.720	103.4	Velocity Head of Stack Gas	$\sqrt{\Delta p_{avg}}$		1.32	in H2O				
1-7	110	1.60	1.265	101	91	235.600	100.5	Stack Temp	Ts		109.63	F				
1-6	110	2.00	1.414	101	91	237.720	101.4	Absolute Stack Temp	Ts(abs)		569.63	R				
1-5	110	2.00	1.414	103	91	239.870	102.7	Stack Static Pressure			-0.85	in H2O				
1-4	111	1.95	1.396	103	92	241.980	102.1	Stack Static Pressure	Pg		-0.0625	in Hg				
1-3	111	1.75	1.323	104	92	243.970	101.6	Barometric Pressure	Pbar		29.10	in Hg				
1-2	110	1.40	1.183	103	92	245.780	103.2	Absolute Stack Pressure	Ps		29.04	in Hg				
1-1	110	1.40	1.183	102	92	247.567	102.0	Condensed H2O Vol @ STP	Vwc(std)	EQ 4-1	0.659	SCF				
2-12	110	1.95	1.396	100	92	249.660	101.4	Silica H2O Vol @ STP	Vwsg(std)	EQ 4-2	0.38	SCF				
2-11	111	1.80	1.342	101	92	251.690	102.4	DGM Vol @ STP	Vm(std)	EQ 4-3	44.50	DSCF				
2-10	111	1.95	1.396	101	92	253.800	102.3	Gas Stream H2O Vapor	Bws	EQ 4-4	0.023	Proportion by Vol				
2-9	110	1.85	1.360	103	92	255.900	104.2	Gas Stream Molecular Weight Dry	Md	EQ 3-1	28.94	lb/lb-mol				
2-8	109	2.00	1.414	103	92	258.020	101.0	Gas Stream Molecular Weight Wet	Ms	EQ 2-6	28.69	lb/lb-mol				
2-7	109	1.95	1.396	105	93	259.740	82.7	Gas Collected from Stack @ STP			45.53	SCF		Wet		
2-6	109	1.90	1.378	105	93	262.230	121.3	Moisture Collection Time			60	Minutes				
2-5	109	1.65	1.285	104	93	264.190	102.6	Gas Collection Rate			0.759	SCFM		Wet		
2-4	108	1.50	1.225	104	93	266.040	101.4	Nozzle Diameter			0.182	in				
2-3	108	1.35	1.162	103	93	267.820	102.9	Area of Nozzle	An		0.000181	ft ²				
2-2	108	1.30	1.140	104	93	269.580	103.6	Average Stack Gas Actual Velocity	Vs	EQ 2-7	76	ft/sec	FS	Wet		
2-1	108	1.20	1.095	105	94	271.253	102.3	Average Stack Gas Actual Velocity			4,580	ft/min	FM	Wet		
Impingers										Average Stack Gas Actual Velocity			274,789	ft/hr	FH	Wet
	1	2	3	Total 1-3	Silica	Total		Average Stack Gas Actual Flow			540	ft ³ /sec	ACFS			
Final				14.0	14.0	8.0		Average Stack Gas Actual Flow			32,373	ft ³ /min	ACFM			
Initial					0.0			Average Stack Gas Actual Flow			1,942,369	ft ³ /hr	ACFH			
Gain	0.0	0.0	14.0	14.0	8.0	22.0		Average Stack Gas Flow @ STP			487	ft ³ /sec	SCFS			
Comments										Average Stack Gas Flow @ STP			29,214	ft ³ /min	SCFM	Wet
TP 2-7 and 2-6 not sampled isokinetically. Thousandths digit not recorded on intermediate points.										Average Stack Gas Flow @ STP			1,752,852	ft ³ /hr	SCFH	Wet
										Average Stack Gas Dry Flow @ STP			476	ft ³ /sec	DSCFS	Dry
										Average Stack Gas Dry Flow @ STP			28,549	ft ³ /min	DSCFM	Dry
										Average Stack Gas Dry Flow @ STP	Q	EQ 2-8	1,712,970	ft ³ /hr	DSCFH	Dry
Notes: To edit sheet just unprotect it under the "Review" tab. Metric flows: m ³ /hr = ft ³ /min x 1.7																

Run 3

Flow Traverse		Dry Gas Meter			Isokinetics	O2 Content of Gas Stream			20.90	% by Volume		Dry			
Port-Pt	Stack Tp (F)	ΔP (in H2O)	Sq Rt ΔP	Tp In (F)	Tp Out (F)	Samp Vol (ft³)	%	CO2 Content of Gas Stream			0.00	% by Volume	Dry		
Avg	110.2	1.71	1.302	98.0		47.539	102.6	Ar Content of Gas Stream			0.90	% by Volume	Dry		
Start					271.540			N2+CO Content of Gas Stream			78.20	% by Volume	Dry		
1-12	110	1.90	1.378	94	93	273.670	105.0	Diameter of Stack			36.00	in			
1-11	111	1.90	1.378	96	93	275.700	100.0	Cross Sectional Area of Stack			7.07	ft²			
1-10	111	1.90	1.378	97	93	277.810	103.9	DGM Cal Factor	Y		1.0105	Dimensionless			
1-9	111	1.85	1.360	100	93	279.870	102.5	Pitot Tube Cal Factor	Cp		0.82	Dimensionless			
1-8	111	1.80	1.342	101	93	281.930	103.8	Velocity Head of Stack Gas	√Δpavg		1.30	in H2O			
1-7	111	1.80	1.342	102	93	284.050	106.8	Stack Temp	Ts		110.17	F			
1-6	111	1.60	1.265	103	93	285.940	100.9	Absolute Stack Temp	Ts(abs)		570.17	R			
1-5	111	1.55	1.245	103	93	287.870	104.6	Stack Static Pressure			-0.85	in H2O			
1-4	111	1.40	1.183	104	93	289.570	96.9	Stack Static Pressure	Pg		-0.0625	in Hg			
1-3	110	1.35	1.162	103	93	291.360	103.8	Barometric Pressure	Pbar		29.10	in Hg			
1-2	109	1.20	1.095	104	93	293.050	103.7	Absolute Stack Pressure	Ps		29.04	in Hg			
1-1	109	1.20	1.095	103	93	294.733	103.3	Condensed H2O Vol @ STP	Vwc(std)	EQ 4-1	0.612	SCF			
2-12	108	2.05	1.432	100	93	296.840	99.1	Silica H2O Vol @ STP	Vwsg(std)	EQ 4-2	0.42	SCF			
2-11	108	1.95	1.396	102	93	298.990	103.5	DGM Vol @ STP	Vm(std)	EQ 4-3	44.19	DSCF			
2-10	108	1.90	1.378	103	93	301.100	102.8	Gas Stream H2O Vapor	Bws	EQ 4-4	0.023	Proportion by Vol			
2-9	108	1.80	1.342	104	93	303.120	101.0	Gas Stream Molecular Weight Dry	Md	EQ 3-1	28.94	lb/lb-mol			
2-8	108	1.70	1.304	104	93	305.130	103.4	Gas Stream Molecular Weight Wet	Ms	EQ 2-6	28.69	lb/lb-mol			
2-7	109	1.80	1.342	105	94	307.130	100.0	Gas Collected from Stack @ STP			45.23	SCF	Wet		
2-6	110	1.80	1.342	105	94	309.450	116.2	Moisture Collection Time			60	Minutes			
2-5	111	2.00	1.414	106	94	311.390	92.3	Gas Collection Rate			0.754	SCFM	Wet		
2-4	112	2.00	1.414	106	94	313.420	96.7	Nozzle Diameter			0.182	in			
2-3	112	1.90	1.378	106	94	315.580	105.6	Area of Nozzle	An		0.000181	ft²			
2-2	112	1.40	1.183	106	95	317.380	102.4	Average Stack Gas Actual Velocity	Vs	EQ 2-7	75	ft/sec	FS	Wet	
2-1	112	1.20	1.095	106	94	319.079	104.5	Average Stack Gas Actual Velocity			4,530	ft/min	FM	Wet	
Impingers							Average Stack Gas Actual Velocity						271,797 ft/hr	FH	Wet
Final	1	2	3	Total 1-3	Silica	Total		Average Stack Gas Actual Flow			534	ft³/sec	ACFS	Wet	
Initial				13.0	13.0	9.0		Average Stack Gas Actual Flow			32,020	ft³/min	ACFM	Wet	
Gain	0.0	0.0			0.0			Average Stack Gas Actual Flow			1,921,220	ft³/hr	ACFH	Wet	
								Average Stack Gas Flow @ STP			481	ft³/sec	SCFS	Wet	
Comments							Average Stack Gas Flow @ STP						28,869 ft³/min	SCFM	Wet
TP 2-6 not sampled isokinetically. TP 2-5 was used to compensate isokinetics. Thousandths digit not recorded on intermediate points.							Average Stack Gas Flow @ STP						1,732,120 ft³/hr	SCFH	Wet
							Average Stack Gas Dry Flow @ STP						470 ft³/sec	DSCFS	Dry
							Average Stack Gas Dry Flow @ STP						28,207 ft³/min	DSCFM	Dry
							Average Stack Gas Dry Flow @ STP						1,692,440 ft³/hr	DSCFH	Dry
Notes: To edit sheet just unprotect it under the "Review" tab. Metric flows: m³/hr = ft³/min × 1.7															

Plant:	Morton Salt	Capacity during Test:	≈ 125kpph steam
Permit #:	MI-ROP-B1824-2008b	Design Capacity:	
SRN:	B1824	SCC Code:	
Tested by:	Network	Date Tested:	August 7, 2013
Reviewed By:	Jeremy Howe	Date Reviewed:	November 13, 2013
Pollutants:	SO ₂ , PM	Purpose of Test:	Compliance
Source:	Boiler #6		

<i>lb/1000lb, Actual</i>								<i>Notes:</i>
Run #	particulate mg	gas sampled lb/ft ³	gas sampled lb	part conc lb/1000lb	iso %	iso max %	iso min %	
1	43.10	0.07548	4.142	0.023	100.5	103.1	99.2	
2	38.80	0.07535	4.134	0.021	100.5	105.7	95.7	
3	34.30	0.07505	4.118	0.018	101.1	103.9	99.6	
Avg	38.73	0.07529	4.131	0.021				
Limit				-				

<i>lb/1000lb, Actual @ 50% EA</i>								<i>Notes</i>
Run #	part conc lb/1000lb	Md lb/lb-mol	Bwo %	emission lb/hr	iso %	iso max %	iso min %	
1	0.023	30.12	7.549	0.027	100.5	103.1	99.2	
2	0.021	30.08	7.655	0.024	100.5	105.7	95.7	
3	0.018	30.05	8.440	0.022	101.1	103.9	99.6	
Avg	0.021	30.08	7.881	0.02				
Limit				0.30				

Run 1

Flow Traverse							Dry Gas Meter		Isokinetics		O2 Content of Gas Stream			9.30	% by Volume		Dry
Port-Pt	Stack Tp (F)	ΔP (in H2O)	Sq Rt ΔP	Tp In (F)	Tp Out (F)	Samp Vol (ft³)	%	CO2 Content of Gas Stream						10.25	% by Volume		Dry
Avg	338.4	0.42	0.643	82.8		53.941	100.5	Ar Content of Gas Stream						0.90	% by Volume		Dry
Start						836.342		N2+CO Content of Gas Stream						79.54	% by Volume		Dry
1-1	338	0.41	0.640	73	73	840.730	100.2	Diameter of Stack						78.00	in		
1-2	339	0.46	0.678	77	73	845.410	100.6	Cross Sectional Area of Stack						33.18	ft²		
1-3	340	0.47	0.686	82	73	850.120	99.9	DGM Cal Factor	Y					0.9945	Dimensionless		
1-4	340	0.43	0.656	87	75	854.720	101.3	Pitot Tube Cal Factor	Cp					0.83	Dimensionless		
1-5	338	0.38	0.616	90	75	859.050	100.9	Velocity Head of Stack Gas	√Δpavg					0.64	in H2O		
1-6	338	0.27	0.520	93	76	862.794	103.1	Stack Temp	Ts					338.42	F		
1-7								Absolute Stack Temp	Ts(abs)					798.42	R		
1-8								Stack Static Pressure						-0.58	in H2O		
1-9								Stack Static Pressure	Pg					-0.0427	in Hg		
1-10								Barometric Pressure	Pbar					29.10	in Hg		
1-11								Absolute Stack Pressure	Ps					29.06	in Hg		
1-12								Condensed H2O Vol @ STP	Vwc(std)	EQ 4-1				3.765	SCF		
2-1	329	0.39	0.624	85	77	867.150	99.3	Silica H2O Vol @ STP	Vwsg(std)	EQ 4-2				0.38	SCF		
2-2	338	0.48	0.693	91	78	871.970	99.6	DGM Vol @ STP	Vm(std)	EQ 4-3				50.73	DSCF		
2-3	339	0.51	0.714	95	79	877.000	100.5	Gas Stream H2O Vapor	Bws	EQ 4-4				0.075	Proportion by Vol		
2-4	341	0.46	0.678	97	80	881.770	100.3	Gas Stream Molecular Weight Dry	Md	EQ 3-1				30.12	lb/lb-mol		
2-5	342	0.40	0.632	98	81	886.170	99.2	Gas Stream Molecular Weight Wet	Ms	EQ 2-6				29.21	lb/lb-mol		
2-6	339	0.33	0.574	98	82	890.283	101.6	Gas Collected from Stack @ STP						54.87	SCF		Wet
2-7								Moisture Collection Time						60	Minutes		
2-8								Gas Collection Rate						0.915	SCFM		Wet
2-9								Nozzle Diameter						0.313	in		
2-10								Area of Nozzle	An					0.000534	ft²		
2-11								Average Stack Gas Actual Velocity	Vs	EQ 2-7				44	ft/sec	FS	Wet
2-12								Average Stack Gas Actual Velocity						2,654	ft/min	FM	Wet
Impingers							Average Stack Gas Actual Velocity							159,246	ft/hr	FH	Wet
	1	2	3	Total 1-3	Silica	Total		Average Stack Gas Actual Flow						1,468	ft³/sec	ACFS	Wet
Final				80.0	80.0	8.0		Average Stack Gas Actual Flow						88,071	ft³/min	ACFM	Wet
Initial						0.0		Average Stack Gas Actual Flow						5,284,276	ft³/hr	ACFH	Wet
Gain	0.0	0.0	80.0	80.0	8.0	88.0		Average Stack Gas Flow @ STP						946	ft³/sec	SCFS	Wet
Comments							Average Stack Gas Flow @ STP							56,742	ft³/min	SCFM	Wet
							Average Stack Gas Flow @ STP							3,404,517	ft³/hr	SCFH	Wet
							Average Stack Gas Dry Flow @ STP							874	ft³/sec	DCSFS	Dry
							Average Stack Gas Dry Flow @ STP							52,459	ft³/min	DCSCFM	Dry
							Average Stack Gas Dry Flow @ STP		Q	EQ 2-8				3,147,519	ft³/hr	DCSCFH	Dry

Notes: To edit sheet just unprotect it under the "Review" tab. Metric flows: $m^3/hr = ft^3/min \times 1.7$

Run 2

Flow Traverse			Dry Gas Meter			Isokinetics	O2 Content of Gas Stream			9.79	% by Volume		Dry	
Port-Pt	Stack Tp (F)	ΔP (in H2O)	Sq Rt ΔP	Tp In (F)	Tp Out (F)	Samp Vol (ft³)	%	CO2 Content of Gas Stream			9.86	% by Volume	Dry	
Avg	343.2	0.44	0.664	89.0		56.177	100.5	Ar Content of Gas Stream			0.90	% by Volume	Dry	
Start						890.558		N2+CO Content of Gas Stream			79.45	% by Volume	Dry	
1-1	337	0.41	0.640	82	81	895.280	105.7	Diameter of Stack			78.00	in		
1-2	340	0.50	0.707	88	81	900.010	95.7	Cross Sectional Area of Stack			33.18	ft²		
1-3	344	0.53	0.728	94	81	905.050	99.0	DGM Cal Factor	Y		0.9945	Dimensionless		
1-4	345	0.49	0.700	97	82	909.950	99.9	Pitot Tube Cal Factor	Cp		0.83	Dimensionless		
1-5	346	0.43	0.656	98	82	914.710	103.6	Velocity Head of Stack Gas	√Δpavg		0.66	in H2O		
1-6	339	0.33	0.574	99	83	918.740	99.1	Stack Temp	Ts		343.17	F		
1-7								Absolute Stack Temp	Ts(abs)		803.17	R		
1-8								Stack Static Pressure			-0.58	in H2O		
1-9								Stack Static Pressure	Pg		-0.0427	in Hg		
1-10								Barometric Pressure	Pbar		29.10	in Hg		
1-11								Absolute Stack Pressure	Ps		29.06	in Hg		
1-12								Condensed H2O Vol @ STP	Vwc(std)	EQ 4-1	3.953	SCF		
2-1	339	0.44	0.663	91	83	923.370	99.3	Silica H2O Vol @ STP	Vwsg(std)	EQ 4-2	0.38	SCF		
2-2	345	0.49	0.700	95	84	928.410	102.7	DGM Vol @ STP	Vm(std)	EQ 4-3	52.23	DSCF		
2-3	346	0.53	0.728	98	84	933.520	100.0	Gas Stream H2O Vapor	Bws	EQ 4-4	0.077	Proportion by Vol		
2-4	347	0.45	0.671	100	85	938.210	99.5	Gas Stream Molecular Weight Dry	Md	EQ 3-1	30.08	lb/lb-mol		
2-5	345	0.42	0.648	100	84	942.800	100.6	Gas Stream Molecular Weight Wet	Ms	EQ 2-6	29.15	lb/lb-mol		
2-6	345	0.30	0.548	100	85	946.735	102.0	Gas Collected from Stack @ STP			56.56	SCF	Wet	
2-7								Moisture Collection Time			60	Minutes		
2-8								Gas Collection Rate			0.943	SCFM	Wet	
2-9								Nozzle Diameter			0.313	in		
2-10								Area of Nozzle	An		0.000534	ft²		
2-11								Average Stack Gas Actual Velocity	Vs	EQ 2-7	46	ft/sec	FS	Wet
2-12								Average Stack Gas Actual Velocity			2,751	ft/min	FM	Wet
Impingers								Average Stack Gas Actual Velocity			165,068	ft/hr	FH	Wet
	1	2	3	Total 1-3	Silica	Total		Average Stack Gas Actual Flow			1,522	ft³/sec	ACFS	Wet
Final				84.0	84.0	8.0		Average Stack Gas Actual Flow			91,291	ft³/min	ACFM	Wet
Initial					0.0			Average Stack Gas Actual Flow			5,477,476	ft³/hr	ACFH	Wet
Gain	0.0	0.0	84.0	84.0	8.0	92.0		Average Stack Gas Flow @ STP			974	ft³/sec	SCFS	Wet
Comments								Average Stack Gas Flow @ STP			58,469	ft³/min	SCFM	Wet
								Average Stack Gas Flow @ STP			3,508,120	ft³/hr	SCFH	Wet
								Average Stack Gas Dry Flow @ STP			900	ft³/sec	DSCFS	Dry
								Average Stack Gas Dry Flow @ STP			53,993	ft³/min	DSCFM	Dry
								Average Stack Gas Dry Flow @ STP	Q	EQ 2-8	3,239,556	ft³/hr	DSCFH	Dry

Notes: To edit sheet just unprotect it under the "Review" tab. Metric flows: m³/hr = ft³/min × 1.7

Run 3

Flow Traverse				Dry Gas Meter			Isokinetics	O2 Content of Gas Stream			10.05	% by Volume		Dry
Port-Pt	Stack Tp (F)	ΔP (in H ₂ O)	Sq Rt ΔP	Tp In (F)	Tp Out (F)	Samp Vol (ft ³)	%	CO2 Content of Gas Stream			9.66	% by Volume		Dry
Avg	344.2	0.43	0.656	89.5		55.509	101.1	Ar Content of Gas Stream			0.90	% by Volume		Dry
Start						947.375		N2+CO Content of Gas Stream			79.38	% by Volume		Dry
1-1	343	0.43	0.656	83	83	951.940	100.9	Diameter of Stack			78.00	in		
1-2	346	0.49	0.700	88	83	956.840	101.3	Cross Sectional Area of Stack			33.18	ft ²		
1-3	346	0.51	0.714	93	82	961.820	100.6	DGM Cal Factor	Y		0.9945	Dimensionless		
1-4	347	0.47	0.686	97	83	966.680	101.9	Pitot Tube Cal Factor	Cp		0.83	Dimensionless		
1-5	346	0.42	0.648	99	83	971.380	103.9	Velocity Head of Stack Gas	$\sqrt{\Delta p_{avg}}$		0.66	in H ₂ O		
1-6	341	0.27	0.520	99	84	975.045	100.4	Stack Temp	Ts		344.17	F		
1-7								Absolute Stack Temp	Ts(abs)		804.17	R		
1-8								Stack Static Pressure			-0.58	in H ₂ O		
1-9								Stack Static Pressure	Pg		-0.0427	in Hg		
1-10								Barometric Pressure	Pbar		29.10	in Hg		
1-11								Absolute Stack Pressure	Ps		29.06	in Hg		
1-12								Condensed H ₂ O Vol @ STP	Vwc(std)	EQ 4-1	4.330	SCF		
2-1	341	0.44	0.663	90	84	979.650	99.6	Silica H ₂ O Vol @ STP	Vwsg(std)	EQ 4-2	0.42	SCF		
2-2	342	0.49	0.700	95	84	984.570	100.5	DGM Vol @ STP	Vm(std)	EQ 4-3	51.57	DSCF		
2-3	344	0.51	0.714	98	84	989.630	101.3	Gas Stream H ₂ O Vapor	Bws	EQ 4-4	0.084	Proportion by Vol		
2-4	344	0.47	0.686	100	85	994.490	101.1	Gas Stream Molecular Weight Dry	Md	EQ 3-1	30.05	lb/lb-mol		
2-5	345	0.41	0.640	100	85	999.010	100.8	Gas Stream Molecular Weight Wet	Ms	EQ 2-6	29.04	lb/lb-mol		
2-6	345	0.30	0.548	100	85	1002.884	101.0	Gas Collected from Stack @ STP			56.33	SCF		Wet
2-7								Moisture Collection Time			60	Minutes		
2-8								Gas Collection Rate			0.939	SCFM		Wet
2-9								Nozzle Diameter			0.313	in		
2-10								Area of Nozzle	An		0.000534	ft ²		
2-11								Average Stack Gas Actual Velocity	Vs	EQ 2-7	45	ft/sec	FS	Wet
2-12								Average Stack Gas Actual Velocity			2,727	ft/min	FM	Wet
Impingers								Average Stack Gas Actual Velocity			163,639	ft/hr	FH	Wet
	1	2	3	Total 1-3	Silica	Total		Average Stack Gas Actual Flow			1,508	ft ³ /sec	ACFS	Wet
Final				92.0	92.0	9.0		Average Stack Gas Actual Flow			90,501	ft ³ /min	ACFM	Wet
Initial					0.0			Average Stack Gas Actual Flow			5,430,042	ft ³ /hr	ACFH	Wet
Gain	0.0	0.0	92.0	92.0	9.0	101.0		Average Stack Gas Flow @ STP			965	ft ³ /sec	SCFS	Wet
Comments								Average Stack Gas Flow @ STP			57,890	ft ³ /min	SCFM	Wet
								Average Stack Gas Flow @ STP			3,473,416	ft ³ /hr	SCFH	Wet
								Average Stack Gas Dry Flow @ STP			883	ft ³ /sec	DSCFS	Dry
								Average Stack Gas Dry Flow @ STP			53,004	ft ³ /min	DSCFM	Dry
								Average Stack Gas Dry Flow @ STP	Q	EQ 2-8	3,180,268	ft ³ /hr	DSCFH	Dry

Notes: To edit sheet just unprotect it under the "Review" tab. Metric flows: m³/hr = ft³/min x 1.7

Duct	Diameters	dd	TP Needed	TP Chosen	TP per Diameter																																																																																																																						
Upstream from disturbance (dd)	2.00	12			0																																																																																																																						
Downstream from disturbance (dd)	8.00	12	12		6																																																																																																																						
						6 Traverse Points Needed Each Diameter																																																																																																																					
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<table border="1"> <thead> <tr> <th>Traverse Point #</th> <th>Fraction of Stack</th> <th>Distance far wall to outside of port</th> <th>Port Length</th> <th>Stack Diameter</th> <th>Distance from far wall</th> <th>Distance from far wall + port</th> <th>Consultant Distance from far wall + port</th> <th>Difference</th> </tr> </thead> <tbody> <tr><td>1</td><td>4.4</td><td>0.00</td><td>0.00</td><td>78.00</td><td>3.43</td><td>3.43</td><td>3.43</td><td>0.00</td></tr> <tr><td>2</td><td>14.6</td><td>0.00</td><td>0.00</td><td>78.00</td><td>11.39</td><td>11.39</td><td>11.39</td><td>0.00</td></tr> <tr><td>3</td><td>29.6</td><td>0.00</td><td>0.00</td><td>78.00</td><td>23.09</td><td>23.09</td><td>23.09</td><td>0.00</td></tr> <tr><td>4</td><td>70.4</td><td>0.00</td><td>0.00</td><td>78.00</td><td>54.91</td><td>54.91</td><td>54.91</td><td>0.00</td></tr> <tr><td>5</td><td>85.4</td><td>0.00</td><td>0.00</td><td>78.00</td><td>66.61</td><td>66.61</td><td>66.61</td><td>0.00</td></tr> <tr><td>6</td><td>95.6</td><td>0.00</td><td>0.00</td><td>78.00</td><td>74.57</td><td>74.57</td><td>74.57</td><td>0.00</td></tr> <tr><td>7</td><td>0.0</td><td>0.00</td><td>0.00</td><td>78.00</td><td>0.00</td><td>0.00</td><td>0.00</td><td>0.00</td></tr> <tr><td>8</td><td>0.0</td><td>0.00</td><td>0.00</td><td>78.00</td><td>0.00</td><td>0.00</td><td>0.00</td><td>0.00</td></tr> <tr><td>9</td><td>0.0</td><td>0.00</td><td>0.00</td><td>78.00</td><td>0.00</td><td>0.00</td><td>0.00</td><td>0.00</td></tr> <tr><td>10</td><td>0.0</td><td>0.00</td><td>0.00</td><td>78.00</td><td>0.00</td><td>0.00</td><td>0.00</td><td>0.00</td></tr> <tr><td>11</td><td>0.0</td><td>0.00</td><td>0.00</td><td>78.00</td><td>0.00</td><td>0.00</td><td>0.00</td><td>0.00</td></tr> <tr><td>12</td><td>0.0</td><td>0.00</td><td>0.00</td><td>78.00</td><td>0.00</td><td>0.00</td><td>0.00</td><td>0.00</td></tr> </tbody> </table>						Traverse Point #	Fraction of Stack	Distance far wall to outside of port	Port Length	Stack Diameter	Distance from far wall	Distance from far wall + port	Consultant Distance from far wall + port	Difference	1	4.4	0.00	0.00	78.00	3.43	3.43	3.43	0.00	2	14.6	0.00	0.00	78.00	11.39	11.39	11.39	0.00	3	29.6	0.00	0.00	78.00	23.09	23.09	23.09	0.00	4	70.4	0.00	0.00	78.00	54.91	54.91	54.91	0.00	5	85.4	0.00	0.00	78.00	66.61	66.61	66.61	0.00	6	95.6	0.00	0.00	78.00	74.57	74.57	74.57	0.00	7	0.0	0.00	0.00	78.00	0.00	0.00	0.00	0.00	8	0.0	0.00	0.00	78.00	0.00	0.00	0.00	0.00	9	0.0	0.00	0.00	78.00	0.00	0.00	0.00	0.00	10	0.0	0.00	0.00	78.00	0.00	0.00	0.00	0.00	11	0.0	0.00	0.00	78.00	0.00	0.00	0.00	0.00	12	0.0	0.00	0.00	78.00	0.00	0.00	0.00	0.00	
Traverse Point #	Fraction of Stack	Distance far wall to outside of port	Port Length	Stack Diameter	Distance from far wall	Distance from far wall + port	Consultant Distance from far wall + port	Difference																																																																																																																			
1	4.4	0.00	0.00	78.00	3.43	3.43	3.43	0.00																																																																																																																			
2	14.6	0.00	0.00	78.00	11.39	11.39	11.39	0.00																																																																																																																			
3	29.6	0.00	0.00	78.00	23.09	23.09	23.09	0.00																																																																																																																			
4	70.4	0.00	0.00	78.00	54.91	54.91	54.91	0.00																																																																																																																			
5	85.4	0.00	0.00	78.00	66.61	66.61	66.61	0.00																																																																																																																			
6	95.6	0.00	0.00	78.00	74.57	74.57	74.57	0.00																																																																																																																			
7	0.0	0.00	0.00	78.00	0.00	0.00	0.00	0.00																																																																																																																			
8	0.0	0.00	0.00	78.00	0.00	0.00	0.00	0.00																																																																																																																			
9	0.0	0.00	0.00	78.00	0.00	0.00	0.00	0.00																																																																																																																			
10	0.0	0.00	0.00	78.00	0.00	0.00	0.00	0.00																																																																																																																			
11	0.0	0.00	0.00	78.00	0.00	0.00	0.00	0.00																																																																																																																			
12	0.0	0.00	0.00	78.00	0.00	0.00	0.00	0.00																																																																																																																			

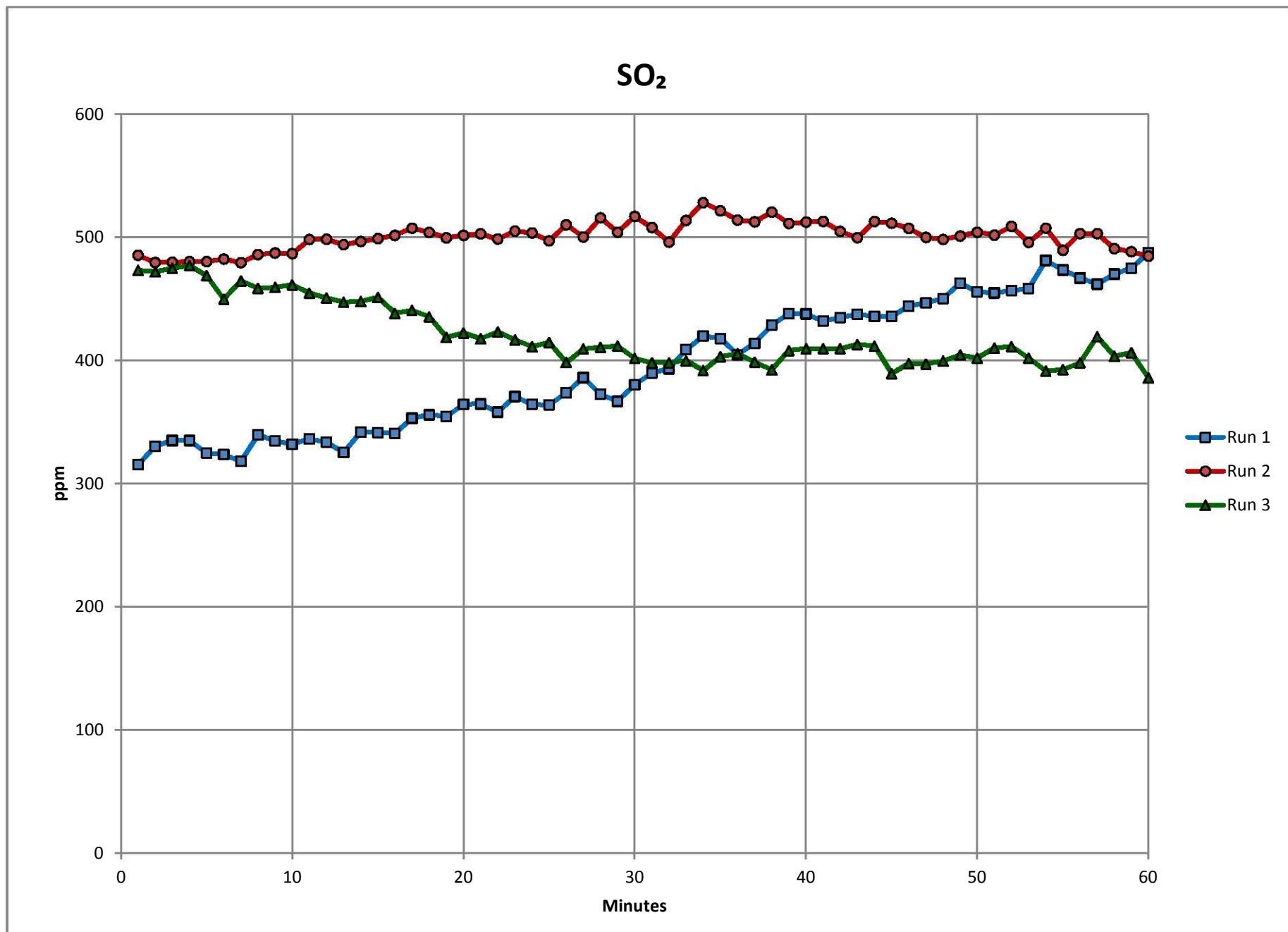
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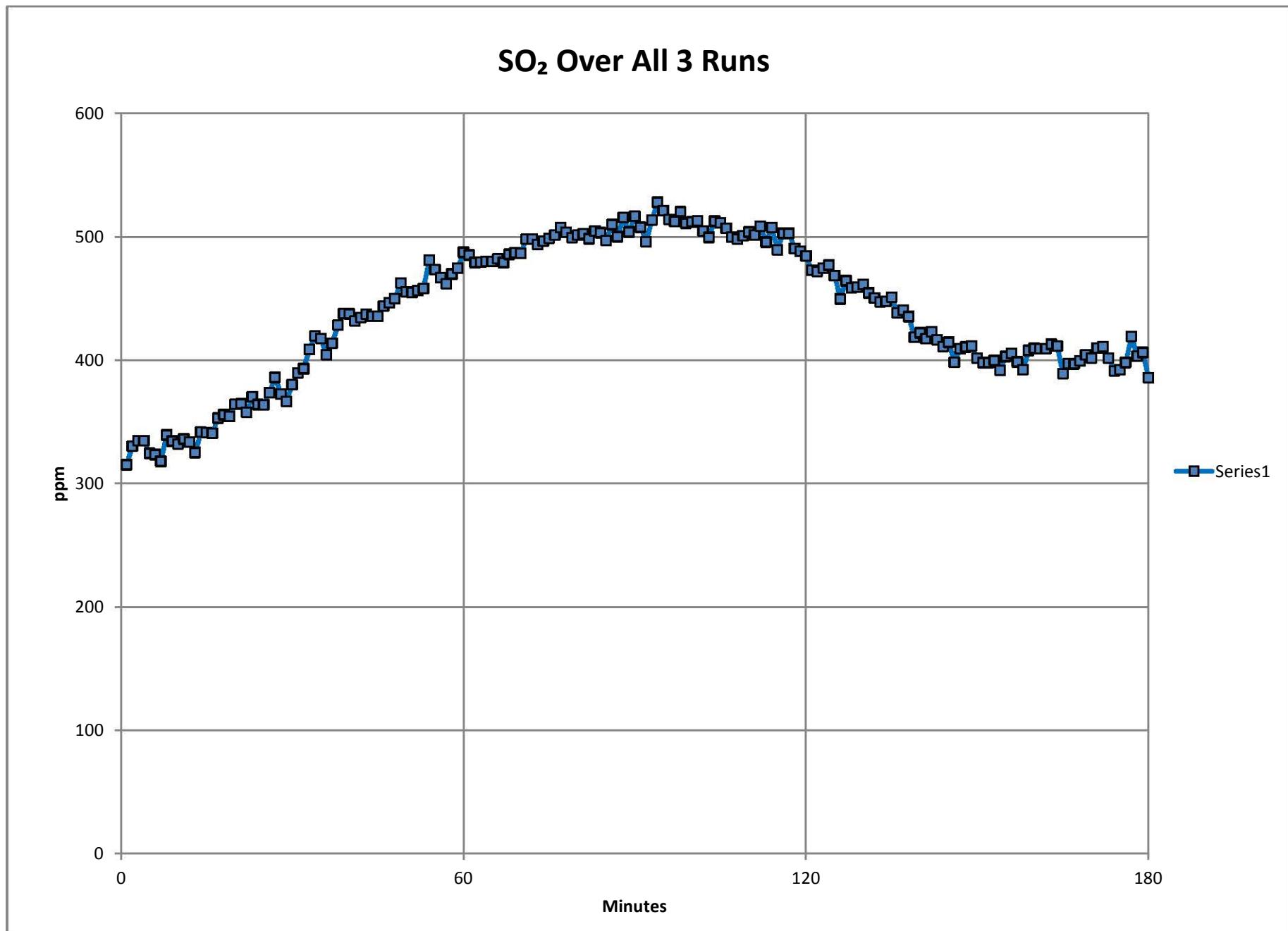
Morton Salt Boiler#6 2013-08-07

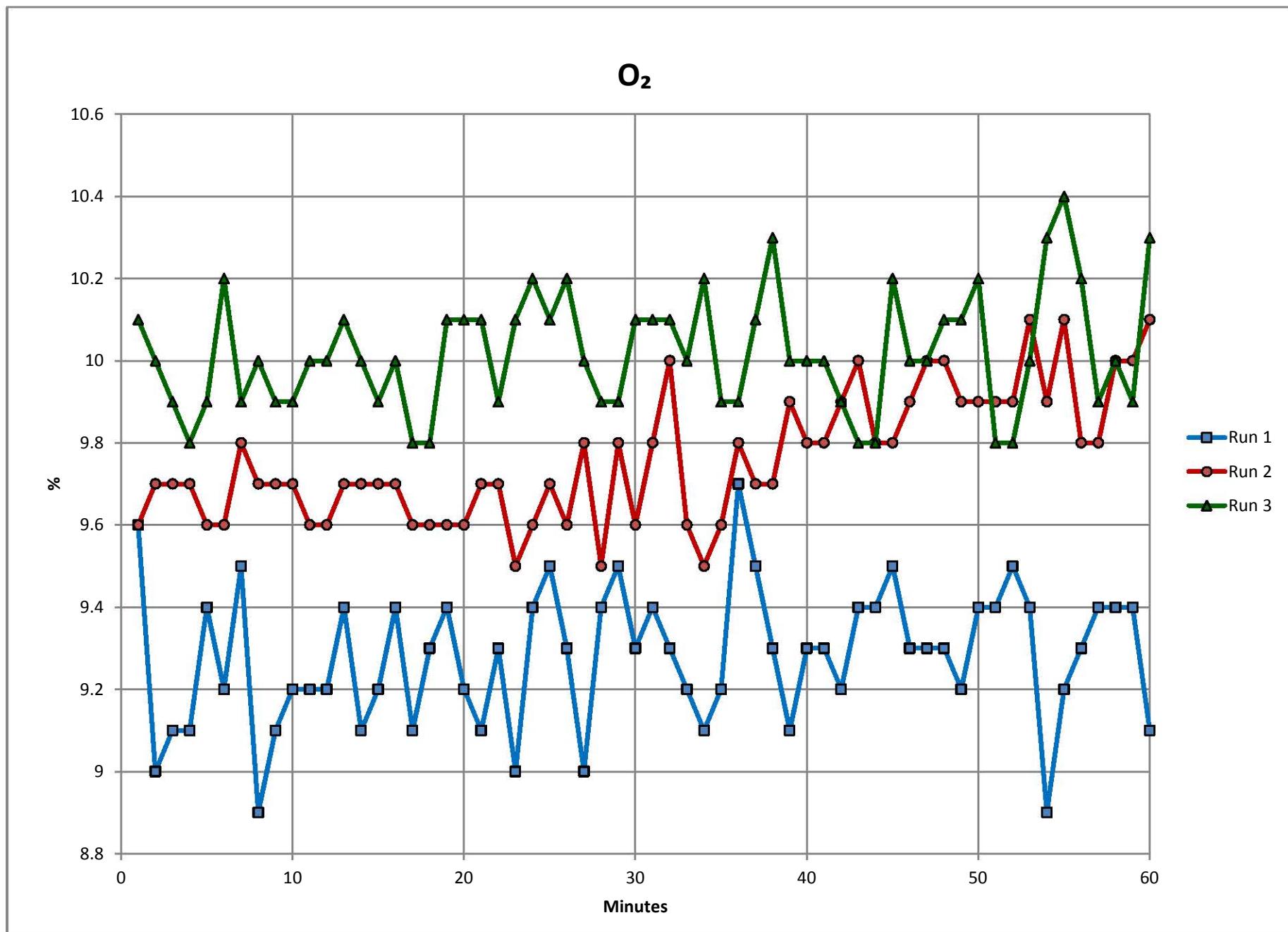
Plant: *Morton Salt*
 Permit #: *MI-ROP-B1824-2008b*
 SRN: *B1824*
 Tested by: *Network*
 Reviewed By: *Jeremy Howe*
 Pollutants: *SO₂, PM*
 Source: *Boiler #6*

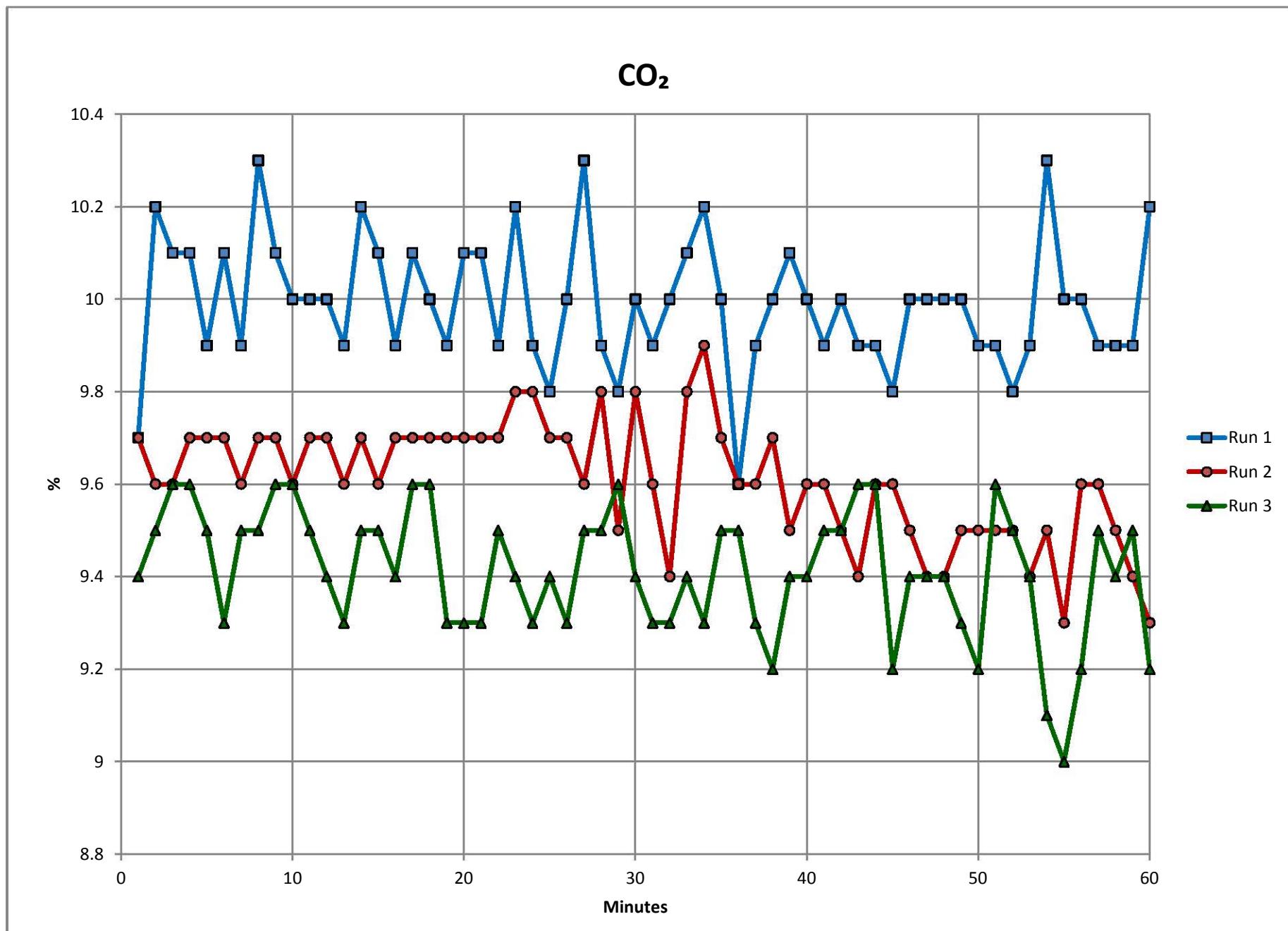
Capacity during Test: *≈ 125kpph steam*
 Design Capacity:
 SCC Code:
 Date Tested: *August 7, 2013*
 Date Reviewed: *November 13, 2013*
 Purpose of Test: *Compliance*

SO₂						
Run #	Corrected ppm	mol wt g/mol	F Factor	O2 %	emission lb/mmBtu	
1	409.58	64	9,780	9.3	1.2	
2	516.89	64	9,780	9.8	1.6	
3	433.54	64	9,780	10.1	1.4	
Avg	453.34	64	9,780	9.7	1.4	
Limit					2.5	









Enter Calibration Data								Check Link to RUNSS worksheet													
Note: ACE, SB and D pass if difference is ≤ 0.5 ppmvd																					
SO₂	0	848.9	1186	2257	ppm	Notes: SO ₂ only 315-550 ppm, but 850 ppm = permit limit of 2.5 lb/mmBtu															
Direct	1.1	840.0	1176.8	2257.0	ppm																
ACE	0.0	-0.4	-0.4	0.0	%																
Limit	2.0	2.0	2.0	2.0	%																
Run	Pre Zero	Post Zero	SBi	SBf	D	Pre Upscale	Post Upscale	SBi	SBf	D	Raw	Co	Cm	Corrected							
#	ppm	ppm	%S	%S	%S	ppm	ppm	%S	%S	%S	ppm	ppm	ppm	ppm							
1	4.6	2.5	0.2	0.1	0.1	809.8	820.5	-1.3	-0.9	0.5	395.1	3.6	815.2	409.6							
2	2.5	2.5	0.1	0.1	0.0	820.5	820.8	-0.9	-0.9	0.0	500.7	2.5	820.7	516.9							
3	2.5	2.3	0.1	0.1	0.0	820.8	821.9	-0.9	-0.8	0.0	420.6	2.4	821.4	433.5							
Avg	3.2	2.4	0.1	0.1	0.0	817.0	821.1	-1.0	-0.8	0.2	438.8	2.8	819.1	453.3							
Limit			5.0	5.0	3.0			5.0	5.0	3.0											
O₂	0	5.98	12.11	20.9	%	Notes															
Direct	0.0	6.1	12.3	20.9	%																
ACE	0.0	0.6	0.9	0.0	%																
Limit	2.0	2.0	2.0	2.0	%																
Run	Pre Zero	Post Zero	SBi	SBf	D	Pre Upscale	Post Upscale	SBi	SBf	D	Raw	Co	Cm	Corrected							
#	%	%	%S	%S	%S	%	%	%S	%S	%S	%	%	%	%	%						
1	0.1	0.1	0.5	0.5	0.0	6.0	6.0	-0.5	-0.5	0.0	9.3	0.1	6.0	9.3							
2	0.1	0.1	0.5	0.5	0.0	6.0	6.0	-0.5	-0.5	0.0	9.8	0.1	6.0	9.8							
3	0.1	0.1	0.5	0.5	0.0	6.0	6.0	-0.5	-0.5	0.0	10.0	0.1	6.0	10.1							
Avg	0.1	0.1	0.5	0.5	0.0	6.0	6.0	-0.5	-0.5	0.0	9.7	0.1	6.0	9.7							
Limit			5.0	5.0	3.0			5.0	5.0	3.0											
CO₂	0	6.019	12.04	20.33	%	Notes															
Direct	0.0	5.8	11.8	20.3	%																
ACE	0.0	-1.1	-1.2	0.0	%																
Limit	2.0	2.0	2.0	2.0	%																
Run	Pre Zero	Post Zero	SBi	SBf	D	Pre Upscale	Post Upscale	SBi	SBf	D	Raw	Co	Cm	Corrected							
#	%	%	%S	%S	%S	%	%	%S	%S	%S	%	%	%	%	%						
1	0.0	0.0	0.0	0.0	0.0	11.8	11.8	0.0	0.0	0.0	10.0	0.0	11.8	10.3							
2	0.0	0.0	0.0	0.0	0.0	11.8	11.8	0.0	0.0	0.0	9.6	0.0	11.8	9.9							
3	0.0	0.0	0.0	0.0	0.0	11.8	11.8	0.0	0.0	0.0	9.4	0.0	11.8	9.7							
Avg	0.0	0.0	0.0	0.0	0.0	11.8	11.8	0.0	0.0	0.0	9.7	0.0	11.8	9.9							
Limit			5.0	5.0	3.0			5.0	5.0	3.0											

