

## Source Test Report

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AIR QUALITY DIVISIO

Real Alloy Recycling, Inc. Coldwater South 267 N. Fillmore Road Coldwater, MI 49036

Test Dates: April 5-6, 2018

### AST Project No. 2018-0239

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#### 1.0 Introduction

Alliance Source Testing, LLC (AST) was retained by Real Alloy Recycling, Inc. (RAR) to conduct compliance testing at the Coldwater, Michigan (South) facility. The facility is subject to provisions of the National Emission Standards for Hazardous Air Pollutants (NESHAP) for Secondary Aluminum Production found in 40 CFR 63, Subpart RRR and the Michigan Department of Environmental Quality (MDEQ) Permit No. MI-PTI-N5957-2012e. Testing was conducted to determine the emission rates of nitrogen oxides (NOx), sulfur dioxide (SO<sub>2</sub>), total hydrocarbons (THC), particulate matter (PM), particulate matter less than 10 microns (PM10), hydrogen chloride (HCl) and dioxins and furans (D/F) at the reverberatory furnace baghouse (EUIMREVERBFURN-S2) exhaust and the emission rates of NOx, THC, PM, PM10, HCl and hydrogen fluoride (HF) at the reverberatory furnace flue (SVIMREVFLUE-S2) duct.

#### 1,1 Facility Description

RAR is a secondary aluminum production facility (SIC 3341) which produces molten aluminum and recycled scrap ingot (RSI) from the melting and recovery of aluminum from aluminum scrap and aluminum dross. The recovery of aluminum from aluminum scrap and aluminum dross and the subsequent production of aluminum ingot have been defined by the United States Environmental Protection Agency (EPA) as secondary aluminum production processes.

#### **1.2** Source and Control System Descriptions

The reverberatory furnace is need to melt aluminum scrap that has been processed by the existing drying system or directly charged toll or purchased scrap. The furnace is designed as a sidewell melter/holder unit to allow for continuous operation. The toll, purchased and preprocessed scrap is charged to the sidewell of the furnace along with solid flux material,  $Cl_2$  gas and any alloying agents that are required for the production order. Once the materials are molten, the metal flows through a submerged opening to the hearth. Once properly alloyed, the furnace is tapped and the molten aluminum is transferred to refractory lined crucibles for delivery or transferred to sow molds. Once clean charge materials are fed to the main hearth, and no reactive flux materials are used in this section of the furnace.

All emissions from the reverberatory furnace sidewell are captured and directed to a lime injected baghouse system for control of the regulated pollutants. Lime in the baghouse system reduces the concentrations of specific pollutants present in the exhanst gas. The baghouse then captures the reacted lime and other particulate matter from the melting process. Emissions from the reverberatory furnace flue exhaust directly to the atmosphere.



#### 1.3 Project Team

Personnel involved in this project are identified in the following table.

| RAR Personnel  | Jeff Ferg<br>Janine Caldwell  |  |
|----------------|---|--|
| MDEQ Personnel | Jeremy Howe<br>Cody Yazzie  |  |
| AST Personnel  | Kenji Kinoshita<br>Jarret Sproull<br>Ben Updegrave<br>Tyler Branca<br>Stacey Cunningham<br>Brandon Cole<br>Jonathon Cervantes<br>Tyler Mewbourn |  |

#### Table 1-1 Project Team

#### 1.4 Site Specific Test Plan & Notification

Testing was conducted in accordance with the Site-Specific Test Plan (SSTP) submitted to MDEQ on January 26, 2018 and revised February 19, 2018 as well as the MDEQ Test Approval Letter dated March 16, 2018.



#### 2.0 Summary of Results

AST conducted compliance testing at the RAR facility in Coldwater, Michigan (South) on April 5-6, 2018. Testing consisted of determining the emission rates of NOx, SO<sub>2</sub>, THC, PM, PM10, HCl and D/F at the reverberatory furnace baghouse (EUIMREVERBFURN-S2) exhaust and the emission rates of NOx, THC, PM, PM10, HCl and HF at the reverberatory furnace flue (SVIMREVFLUE-S2) duct.

Tables 2-1 and 2-2 provide summaries of the emission testing results with comparisons to the applicable NESHAP and state permit limits. These tables also provide summaries of the process operating and control system data collected during testing. Any difference between the summary results listed in the following tables and the detailed results contained in appendices is due to rounding for presentation.



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|                                    | Table 2-1               |                     |
|------------------------------------|-------------------------|---------------------|
| Summary of Results – Reverberatory | <b>Furnace Baghouse</b> | (EUIMREVERBFURN-S2) |

| Emissions Data                                    |                  |           |          |         |
|---|------------------|-----------|----------|---------|
| Run Number  | Run 1            | Run 2     | Run 3    | Average |
| Date  | 4/5/18           | 4/5/18    | 4/6/18   |         |
| Filterable Particulate Matter Data                |                  |           |          |         |
| Emission Factor, lb/ton                           | 0.077            | 0.075     | 0.037    | 0.063   |
| NESHAP Emission Limit, lb/ton                     |                  |           |          | 0.40    |
| Percent of Limit, %                               |                  |           |          | 16      |
| MDEQ Emission Limit, lb/ton                       |                  |           |          | 0.114   |
| Percent of Limit, %                               |                  |           |          | 55      |
| Total Particulate Matter < 10 Microns Data        |                  |           |          |         |
| Emission Factor, lb/ton                           | 0.12             | 0.11      | 0.084    | 0.10    |
| MDEQ Emission Limit, lb/ton                       |                  |           |          | 0.212   |
| Percent of Limit, %                               |                  |           |          | 49      |
| Hydrogen Chloride Data                            |                  |           |          |         |
| Emission Factor, lb/ton <sup>1</sup>              | 0.0019           | 0.0021    | 0.0020   | 0.0020  |
| NESHAP Emission Limit, lb/ton                     |                  |           |          | 0.40    |
| Percent of Limit, %                               |                  |           |          | <1      |
| Dioxin/Furan Data                                 |                  |           |          |         |
| Emission Factor, grain TEQ/ton <sup>2</sup>       | 2.7E-06          | 4.8E-06   | 3.8E-06  | 3.8E-06 |
| NESHAP Limit, grain TEQ/MG                        |                  |           |          | 2.1E-04 |
| Percent of Limit, %                               |                  |           |          | 2       |
| Nitrogen Oxides Data                              |                  |           |          |         |
| Emission Factor, lb/ton                           | 0.14             | 0.19      | 0.22     | 0.18    |
| MDEQ Emission Limit, lb/ton                       |                  |           |          | 0.398   |
| Percent of Limit, %                               |                  |           |          | 46      |
| Total Hydrocarbons Data (as propane) <sup>3</sup> |                  |           |          |         |
| Emission Factor, lb/ton                           | 0.48             | 0.45      | 0.37     | 0.44    |
| MDEQ Emission Limit, lb/ton                       |                  |           |          | 0.483   |
| Percent of Limit, %                               |                  |           |          | 90      |
| Sulfur Dioxide Data                               |                  |           |          |         |
| Emission Factor, lb/ton                           | 0.065            | 0.057     | 0.013    | 0.045   |
| MDEQ Emission Limit, lb/ton                       |                  |           |          | 0.523   |
| Percent of Limit, %                               |                  |           | <u> </u> | 9       |
| Process Operation                                 | ing / Control Sy | stem Data |          |         |
| Run Number  | Run 1            | Run 2     | Run 3    | Average |
| Date  | 4/5/18           | 4/5/18    | 4/6/18   |         |
| Feed Rate, lb/hr                                  | 13,064           | 12,030    | 10,853   | 11,982  |
| Baghouse Inlet Temperature, °F                    | 88               | 92        | 82       | 87      |
| Flux Percentage, %                                | 4.04             | 4.55      | 1.76     | 3.45    |
| Cl <sub>2</sub> Feed, lb                          | 350              | 493       | 165      | 336     |
| Lime Injection Rate, lb/hr                        | 26.8             | 26.7      | 26.3     | 26.6    |

<sup>1</sup> HCI laboratory results for all three (3) test runs were below the detection limit. The detection limit was used for emission calculation purposes.
 <sup>2</sup> D/F TEQ values were calculated using 1989 NATO TEFs.
 <sup>3</sup> The methane concentration for the gas stream was subtracted from the total hydrocarbon (THC) concentration to determine non-inethane THC.



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| Table 2-2  |
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| Summary of Results – Reverberatory Furnace Flue (SVIMREVFLUE-S2) |

| Emissions Data                          |        |        |        |         |
|---|--------|--------|--------|---------|
| Run Number                              | Run 1  | Run 2  | Run 3  | Average |
| Date                                    | 4/5/18 | 4/5/18 | 4/6/18 |         |
| Particulate Matter Data                 |        |        |        | *****   |
| Emission Factor, lb/ton                 | 0.53   | 0.58   | 0.72   | 0.61    |
| MDEQ Emission Limit, lb/ton             |        |        |        | 0.854   |
| Percent of Limit, %                     |        |        |        | 71      |
| Particulate Matter < 10 Microns Data    |        |        |        |         |
| Emission Factor, lb/ton                 | 2.8    | 3.9    | 2.9    | 3.2     |
| MDEQ Emission Limit, lb/ton             |        |        |        | 1.144   |
| Percent of Limit, %                     |        |        |        | >100    |
| Hydrogen Chloride Data                  |        |        |        |         |
| Emission Factor, lb/ton                 | 1.6    | 2,3    | 1,5    | 1.8     |
| MDEQ Emission Limit, lb/ton             |        |        |        | 1.648   |
| Percent of Limit, %                     |        |        |        | >100    |
| Hydrogen Fluoride Data                  |        |        |        |         |
| Emission Factor, lb/ton                 | 0.025  | 0.011  | 0.014  | 0.017   |
| MDEQ Emission Limit, lb/ton             |        |        |        | 0.126   |
| Percent of Limit, %                     |        |        |        | 13      |
| Nitrogen Oxides Data                    |        |        |        |         |
| Emission Factor, lb/hr                  | 1.0    | 0.96   | 0.94   | 0.97    |
| MDEQ Emission Limit, lb/hr              |        |        |        | 0.171   |
| Percent of Limit, %                     |        |        |        | >100    |
| Total Hydrocarbons Data (as propane) *  |        |        |        |         |
| Emission Factor, lb/ton                 | 0.0084 | 0.016  | 0.0025 | 0.0091  |
| MDEQ Emission Limit, lb/ton             |        |        |        | 0.482   |
| Percent of Limit, %                     |        |        |        | 2       |
| Process Operating / Control System Data |        |        |        |         |
| Run Number                              | Run 1  | Run 2  | Run 3  | Average |
| Date                                    | 4/5/18 | 4/5/18 | 4/6/18 |         |
| Feed Rate, lb/hr                        | 13,064 | 12,030 | 10,853 | 11,982  |
| Baghouse Inlet Temperature, °F          | 88     | 92     | 82     | 87      |
| Flux Percentage, %                      | 4.04   | 4.55   | 1.76   | 3.45    |
| Cl <sub>2</sub> Feed, lb                | 350    | 493    | 165    | 336     |
| Lime Injection Rate, lb/hr              | 26.8   | 26.7   | 26.3   | 26.6    |

\* The methane concentration for the gas stream was subtracted from the total hydrocarbon (THC) concentration to determine non-methane THC.

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Source Test Report Testing Methodology

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#### 3.0 Testing Methodology

The emission testing program was conducted in accordance with the test methods listed in Table 3-1. Method descriptions are provided below while quality assurance/quality control data is provided in Appendix D.

### Table 3-1 Source Testing Methodology

| Parameter                            | U.S. EPA Reference<br>Test Methods | Notes/Remarks                     |
|--------------------------------------|------------------------------------|-----------------------------------|
| Volumetric Flow Rate                 | 1&2                                | Full Velocity Traverses           |
| Oxygen/Carbon Dioxide                | 3A                                 | Instrumental Analysis             |
| Moisture Content                     | 4                                  | Volumetric / Gravimetric Analysis |
| Particulate Matter                   | 5/202                              | Isokinetic Sampling               |
| Sulfur Dioxide                       | 6C                                 | Instrumental Analysis             |
| Nitrogen Oxides                      | 7E                                 | Instrumental Analysis             |
| Dioxins/Furans                       | 23 / ALT-034                       | Isokinetic Sampling               |
| Total Hydrocarbons (Minus Methane)   | 25A                                | Instrumental Analysis             |
| Hydrogen Chloride, Hydrogen Fluoride | 26                                 | Constant Rate Sampling            |
| Gas Dilution System Certification    | 205                                |                                   |

#### 3.1 U.S. EPA Reference Test Methods I and 2 – Sampling/Traverse Points and Volumetric Flow Rate

The sampling location and number of traverse (sampling) points were selected in accordance with U.S. EPA Reference Test Method 1. To determine the minimum number of traverse points, the upstream and downstream distances were equated into equivalent diameters and compared to Figure 1-1 (for isokinetic sampling) and/or Figure 1-2 (measuring velocity alone) in U.S. EPA Reference Test Method 1.

Full velocity traverses were conducted in accordance with U.S. EPA Reference Test Method 2 to determine the average stack gas velocity pressure, static pressure and temperature. The velocity and static pressure measurement system consisted of a pitot tube and inclined manometer. The stack gas temperature was measured with a K-type thermocouple and pyrometer.

#### 3.2 U.S. EPA Reference Test Method 3A – Oxygen/Carhon Dioxide

The oxygen  $(O_2)$  and carbon dioxide  $(CO_2)$  testing was conducted in accordance with U.S. EPA Reference Test Method 3A. Data was collected online and reported in one-minute averages. The sampling system consisted of a stainless-steel probe, Teflon sample line(s), gas conditioning system and the identified gas analyzer. The gas conditioning system was a non-contact condenser used to remove moisture from the stack gas. If an unheated Teflon sample line was used, then a portable non-contact condenser was placed in the system directly after the probe. Otherwise, a heated Teflon sample line was used. The quality control measures are described in Section 3.11.



#### 3.3 U.S. EPA Reference Test Method 4 – Moisture Content

The stack gas moisture content was determined in accordance with U.S. EPA Reference Test Method 4. The gas conditioning train consisted of a series of chilled impingers. Prior to testing, each impinger was filled with a known quantity of water or silica gel. Post testing, the quantities of water and silica gel were measured to determine the amount of moisture condensed during the test run. Alternatively, each impinger was analyzed gravimetrically before and after each test run on the same balance to determine the amount of moisture condensed.

#### 3.4 U.S. EPA Reference Test Methods 5 and 202 – Total Particulate Matter

The total particulate matter (filterable and condensable PM) testing was conducted in accordance with U.S. EPA Reference Test Methods 5 and 202. The complete sampling system consisted of a glass nozzle, glass-lined probe, pre-weighed quartz filter, coil condenser, un-weighed Teflon filter, gas conditioning train, pump and calibrated dry gas meter. The gas conditioning train consisted of a coiled condenser and four (4) chilled impingers. The first, and second impingers were initially empty, the third contained 100 mL of de-ionized water and the last impinger contained 200-300 grams of silica gel. The un-weighed 90 mm Teflon filter was placed between the second and third impingers. The probe liner heating system was maintained at a temperature of  $248 \pm 25^{\circ}$ F, and the impinger temperature was maintained at  $68^{\circ}$ F or less throughout testing. The temperature of the Teflon filter was maintained greater than  $65^{\circ}$ F but less than or equal to  $85^{\circ}$ F.

Following the completion of each test run, the sampling train was leak checked at a vacuum pressure greater than or equal to the highest vacuum pressure observed during the run. The nitrogen purge was omitted due to minimal condensate collected in the dry impingers. After the leak check the impinger contents were measured for moisture gain.

The pre-weighed quartz filter was carefully removed and placed in container 1. The probe, nozzle and front half of the filter holder were rinsed three (3) times with acetone to remove any adhering particulate matter and these rinses were recovered in container 2. All containers were sealed, labeled and liquid levels marked for transport to the identified laboratory for filterable particulate matter analysis.

The contents of impingers 1 and 2 were recovered in container 3. The back half of the filterable PM filter holder, the coil condenser, impingers 1 and 2 and all connecting glassware were rinsed with DIUF water and then rinsed with acetone, followed by hexane. The water rinses were added to container 3 while the solvent rinses were recovered in container 4. The Teflon filter was removed from the filter holder and placed in container 5. The front half of the condensable PM filter holder was rinsed with DIUF water and then with acetone, followed by hexane. The water rinses were added to container 4. All containers were sealed, labeled and liquid levels marked for transport to the identified laboratory for condensable particulate matter analysis.

#### 3.5 U.S. EPA Reference Test Method 6C – Sulfur Dioxide

The sulfur dioxide (SO<sub>2</sub>) testing was conducted in accordance with U.S. EPA Reference Test Method 6C. Data was collected online and reported in one-minute averages. The sampling system consisted of a heated stainless-steel probe, Teflon sample line(s), gas conditioning system and the identified analyzer. The gas conditioning system was a non-contact condenser used to remove moisture from the source gas. If an unheated Teflon sample line was used, then a portable non-contact condenser was placed in the system directly after the probe. Otherwise, a heated Teflon sample line was used. The quality control measures are described in Section 3.11.



#### 3.6 U.S. EPA Reference Test Method 7E – Nitrogen Oxides

The nitrogen oxides (NOx) testing was conducted in accordance with U.S. EPA Reference Test Method 7E. Data was collected online and reported in one-minute averages. The sampling system consisted of a stainless-steel probe, Teflon sample line(s), gas conditioning system and the identified gas analyzer. The gas conditioning system was a non-contact condenser used to remove moisture from the stack gas. If an unheated Teflon sample line was used, then a portable non-contact condenser was placed in the system directly after the probe. Otherwise, a heated Teflon sample line was used. The quality control measures are described in Section 3.11.

#### 3.7 U.S. EPA Reference Test Method 23/Alternative Method 034 – Dioxins/Furans

The dioxins and furans (D/F) testing was conducted in accordance with U.S. EPA Reference Test Method 23 with guidance from Alternative Method 034. The sampling system consisted of a glass nozzle, heated glass-lined probe, glass filter holder with pre-cleaned heated glass-fiber filter, condenser coil, XAD sorbent module, gas conditioning train, pump and calibrated dry gas meter. The gas conditioning system consisted of five (5) chilled impingers. The first impinger was empty. The next two (2) impingers each contained 100 mL of water. The fourth impinger was empty while the fifth impinger was charged with 200-300 grams of silica gel. The probe liner and filter heating systems were maintained at a temperature of  $120 \pm 14^{\circ}$ C (248 ±25°F), and the impinger temperature was maintained below at 20°C (68°F) or less throughout testing.

All glassware leading to the XAD adsorbing resin trap was cleaned and sealed before mobilizing to the site. Glassware cleaning consisted of washing with warm soapy water and rinsing with distilled water and acetone. The sampling train was assembled in the sample recovery area. The glass-fiber filter was placed in a glass filter holder with a Teflon filter support and connected to the condenser coil. All open ends of the sampling train were sealed with Teflon tape prior to complete assembly at the sampling location.

Following the completion of each test run, the sampling train was leak checked at vacuum pressure greater than or equal to the highest vacuum pressure observed during the run and the contents of the impingers were measured for moisture gain. The XAD sorbent module was sealed on both ends and placed on ice. The filter was removed from the filter holder and placed in sample container 1. The nozzle, probe liner, filter holder, condenser and all connecting glassware were triple-rinsed and brushed with acetone, and these rinses were recovered in sample container 2. All glassware cleaned for sample container 2 was also triple-rinsed with toluene and recovered into sample container 3. All containers were sealed, labeled and liquid levels marked for transport to the identified laboratory for analysis.

A field blank was collected after the first test run. A complete sampling system was placed at the sampling location and multiple leak checks were performed on the system similar to an actual testing scenario. The sample train was then moved to the mobile laboratory for recovery. A full set of regent blanks including a filter and a trap were also submitted to the laboratory.

#### 3.8 U.S. EPA Reference Test Method 25A – Total Hydrocarbons

The total hydrocarbons (THC) testing was conducted in accordance with U.S. EPA Reference Test Method 25A. Data was collected online and reported in one-minute averages. The sampling system consisted of a stainless-steel probe, heated Teflon sample line(s) and the identified gas analyzer. Methane concentrations were determined using an FID equipped with a methane cutter. The average methane data was subtracted from the THC data to determine non-methane THC. The quality control measures are described in Section 3.12.



#### 3.9 U.S. EPA Reference Test Method 26 – Hydrogen Chloride and Hydrogen Fluoride

The hydrogen chloride (HCl) and hydrogen fluoride (HF) testing was conducted in accordance with U.S. EPA Reference Test Method 26. The complete sampling system consisted of a glass nozzle, heated glass-lined probe, heated Teflon filter, gas conditioning train, pump and calibrated dry gas meter. The gas conditioning train consisted of four (4) chilled impingers. The first and second impingers contained 100 mL of 0.1 N H<sub>2</sub>SO<sub>4</sub>, the third was initially empty and the fourth contained 200-300 grams of silica gel. The probe liner and filter heating systems were maintained at 248-273°F, and the impinger temperature was maintained at 20°C (68°F) or less throughout the testing.

Following the completion of each test run, the sampling train was leak checked at a vacuum pressure greater than or equal to the highest vacuum pressure observed during the run and the contents of the impingers were measured for moisture gain. The absorbing solution  $(0.1 \text{ N H}_2\text{SO}_4)$  from the first and second impingers was placed into sample container 1. The back-half of the filter holder, first, second and third impingers and all glassware leading to the outlet of the third impinger were rinsed with de-ionized (DI) water. These rinses were also placed in container 1. All containers were sealed, labeled and liquid levels marked for transport to the identified laboratory for analysis.

#### 3.10 U.S. EPA Reference Test Method 205 – Gas Dilution System Certification

A calibration gas dilution system field check was conducted in accordance with U.S. EPA Reference Method 205. Multiple dilution rates and total gas flow rates were utilized to force the dilution system to perform two dilutions on each mass flow controller. The diluted calibration gases were sent directly to the analyzer, and the analyzer response recorded in an electronic field data sheet. The analyzer response agreed within 2% of the actual diluted gas concentration. A second Protocol I calibration gas, with a cylinder concentration within 10% of one of the gas divider settings described above, was introduced directly to the analyzer response agreed within 2%. These steps were repeated three (3) times. Copies of the Method 205 data can be found in the Quality Assurance/Quality Control Appendix.

#### 3.11 Quality Assurance/Quality Control – U.S. EPA Reference Test Methods 3A, 6C and 7E

Cylinder calibration gases used met EPA Protocol 1 (+/- 2%) standards. Copies of all calibration gas certificates can be found in the Quality Assurance/Quality Control Appendix.

Low Level gas was introduced directly to the analyzer. After adjusting the analyzer to the Low-Level gas concentration and once the analyzer reading was stable, the analyzer value was recorded. This process was repeated for the High-Level gas. For the Calibration Error Test, Low, Mid, and High-Level calibration gases were sequentially introduced directly to the analyzer. All values were within 2.0 percent of the Calibration Span or 0.5 ppmv absolute difference.

High or Mid-Level gas (whichever was closer to the stack gas concentration) was introduced at the probe and the time required for the analyzer reading to reach 95 percent or 0.5 ppm (whichever was less restrictive) of the gas concentration was recorded. The analyzer reading was observed until it reached a stable value, and this value was recorded. Next, Low Level gas was introduced at the probe and the time required for the analyzer reading to decrease to a value within 5.0 percent or 0.5 ppm (whichever was less restrictive) was recorded. If the Low-Level gas was zero gas, the response was 0.5 ppm or 5.0 percent of the upscale gas concentration (whichever was less restrictive). The analyzer reading was observed until it reached a stable value and this value was recorded. The measurement system response time and initial system bias were determined from these data. The System Bias was within 5.0 percent of the Calibration Span or 0.5 ppm vabsolute difference



High or Mid-Level gas (whichever was closer to the stack gas concentration) was introduced at the probe. After the analyzer response was stable, the value was recorded. Next, Low Level gas was introduced at the probe, and the analyzer value recorded once it reached a stable response. The System Bias was within 5.0 percent of the Calibration Span or 0.5 ppmv absolute difference or the data was invalidated and the Calibration Error Test and System Bias were repeated.

To determine the number of sampling points, a gas stratification check was conducted prior to initiating testing. The pollutant concentrations were measured at or three points (16.7, 50.0 and 83.3 percent of the measurement line). Each traverse point was sampled for a minimum of twice the system response time.

If the pollutant concentration at each traverse point did not differ more than 5% or 0.5 ppm (whichever was less restrictive) of the average pollutant concentration, then single point sampling was conducted during the test runs. If the pollutant concentration did not meet these specifications but differed less than 10% or 1.0 ppm from the average concentration, then three (3) point sampling was conducted (stacks less than 7.8 feet in diameter - 16.7, 50.0 and 83.3 percent of the measurement line; stacks greater than 7.8 feet in diameter - 0.4, 1.0, and 2.0 meters from the stack wall). If the pollutant concentration differed by more than 10% or 1.0 ppm from the average concentration, then sampling was conducted at a minimum of twelve (12) traverse points. Copies of stratification check data can be found in the Quality Assurance/Quality Control Appendix.

An  $NO_2 - NO$  converter check was performed on the analyzer at the completion of testing. An approximately 50 ppin nitrogen dioxide cylinder gas was introduced directly to the NOx analyzer and the instrument response was recorded in an electronic data sheet. The instrument response was within +/- 10 percent of the cylinder concentration.

A Data Acquisition System with battery backup was used to record the instrument response in one (1) minute averages. The data was continuously stored as a \*.CSV file in Excel format on the hard drive of a computer. At the completion of testing, the data was also saved to the AST server. All data was reviewed by the Field Team Leader before leaving the facility. Once arriving at AST's office, all written and electronic data was relinquished to the report coordinator and then a final review was performed by the Project Manager.

#### 3.12 Quality Assurance/Quality Control – U.S. EPA Reference Test Method 25A

Cylinder calibration gases used met EPA Protocol 1 (+/- 2%) standards. Copies of all calibration gas certificates can be found in the Quality Assurance/Quality Control Appendix.

Within two (2) hours prior to testing, zero gas was introduced through the sampling system to the analyzer. After adjusting the analyzer to the Zero gas concentration and once the analyzer reading was stable, the analyzer value was recorded. This process was repeated for the High-Level gas, and the time required for the analyzer reading to reach 95 percent of the gas concentration was recorded to determine the response time. Next, Low and Mid-Level gases were introduced through the sampling system to the analyzer, and the response was recorded when it was stable. All values were less than +/- 5 percent of the calibration gas concentrations.

Mid-Level gas was introduced through the sampling system. After the analyzer response was stable, the value was recorded. Next, zero gas was introduced through the sampling system, and the analyzer value recorded once it reached a stable response. The Analyzer Drift was less than +/- 3 percent of the span value.



A Data Acquisition System with battery backup was used to record the instrument response in one (1) minute averages. The data was continuously stored as a \*.CSV file in Excel format on the hard drive of a computer. At the completion of testing, the data was also saved to the AST server. All data was reviewed by the Field Team Leader before leaving the facility. Once arriving at AST's office, all written and electronic data was relinquished to the report coordinator and then a final review was performed by the Project Manager.