



Compliance Emissions Test Report

**Lansing Board of Water & Light
Delta Energy Park Facility
EUCTGHRSG3
Permit to Install 74-18C
Lansing, Michigan
June 1, 2023**

**Report Submittal Date
June 30, 2023**

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Mostardi Platt

Project No. M231206D

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1.0 EXECUTIVE SUMMARY

Mostardi Platt performed a compliance emissions test program on the EUCTGHRSG3 Combined Cycle while firing natural gas at the Lansing Board of Water & Light, Delta Energy Park Facility in Lansing, Michigan. The purpose of the test program is to demonstrate compliance with requirements for emission rate in accordance with Permit to Install 74-18C at maximum achievable load. This report summarizes the results of the test program and test methods utilized.

The test location, test date, and test parameters are summarized below.

| TEST INFORMATION | | |
|------------------|--------------|---|
| Test Location | Test Date | Test Parameters |
| EUCTGHRSG3 | June 1, 2023 | Total Particulate Matter (TPM), Nitrogen Oxide (NO _x), Volatile Organic Compounds (VOC) |

All testing, sampling, analytical, and calibration procedures used for this test program was performed as described in the *Code of Federal Regulations*, Title 40, Part 60, Appendix A (40CFR60), Methods 1, 2, 3A, 4, 5, 7E, and 25A; Method 202, 40CFR51, and Appendix M; and the latest revisions thereof. Selected results of the test program are summarized below. A complete summary of emission test results follows the narrative portion of this report.

Operating data provided by Lansing Board of Water & Light is included in Appendix E.

| Source | Pollutant Tested | Emissions Limit | Emission Rate |
|--------------------------------|--------------------------------------|------------------------------|---------------------------|
| EUCTGHRSG3 (Combined Cycle) | TPM | PM _{2.5} 6.02 lb/hr | 0.652 lb/hr |
| | | PM ₁₀ 6.02 lb/hr | 0.652 lb/hr |
| | NO _x @ 15% O ₂ | 3 ppm @ 15% O ₂ | 2.22 @ 15% O ₂ |
| | NO _x | 60 lb/hr | 4.36 lb/hr |
| | VOC | 3 ppm @ 15% O ₂ | 0.1 @ 15% O ₂ |

The identifications of the individuals associated with the test program are summarized below.

| TEST PERSONNEL INFORMATION | | |
|-------------------------------|---|---|
| Location | Address | Contact |
| Test Coordinator | Lansing Board of Water and Light 1232 Haco Drive PO Box 13007 Lansing, Michigan 48912-1610 | Mr. Nathan Hude Environmental Compliance Specialist (517) 702-6170 (phone) nathan.hude@lbwl.com |
| Test Facility | Lansing Board of Water and Light Delta Energy Park Facility 3725 South Canal Road Lansing, MI 48917 A | |
| Testing Company Supervisor | Mostardi Platt 888 Industrial Drive Elmhurst, IL 60126 | Mr. Jacob Howe Senior Project Manager 630-993-2100 (phone) jhowe@mp-mail.com |

The test crew consisted of A. Benninghoff, E. Thomas, J. Meade and J. Howe of Mostardi Platt.

2.0 TEST METHODOLOGY

Emission testing was conducted following the United States Environmental Protection Agency (USEPA) methods specified in 40CFR60, Appendix A in addition the Mostardi Platt Quality Manual. Schematics of the test section diagrams and sampling trains used are included in Appendix A and B respectively. Calculation nomenclature are included in Appendix C. The computerized reference method test data is included in Appendix D. Process data as provided by Lansing Board of Water & Light are also included in Appendix E.

The following methodologies were used during the test program:

Methods 1 and 2 Volumetric Flowrate Determination

Gas velocity and volumetric flowrate are determined at the stack test location using Reference Methods 1 and 2 from the Method 5 sampling train.

Velocity pressures were determined by traversing the test location with an S-type pitot tube. Temperatures were measured using K-type thermocouples with calibrated digital temperature indicators. The molecular weight and moisture content of the gases are determined to permit the calculation of the volumetric flowrate. Sampling points utilized were determined using Method 1, 40CFR60, following the table below.

| Location | Diameter | Upstream Diameters | Downstream Diameters | Test Parameters | Number of Sampling Points |
|------------|----------|-----------------------|-------------------------|---|---|
| EUCTGHRSG3 | 10 Feet | 1.8 | 5.5 | NOx/VOC/O ₂ /CO ₂ | 12 (stratification) 3 for Runs 2 and 3 |

Method 3A Oxygen and Carbon Dioxide Determination

Stack gas oxygen (O₂) and carbon dioxide (CO₂) concentrations were determined in accordance with USEPA Method 3A, 40CFR60, Appendix A. A Servomex analyzer was used to determine the CO₂ and O₂ concentrations in the manner specified in the Method. The instrument has a paramagnetic detector and the CO₂ and O₂ operate in the nominal range of 0% to 25% with the specific range determined by the high-level calibration gas. High-range calibrations were performed using USEPA Protocol gas. Zero nitrogen (a low ppm pollutant in balance nitrogen calibration gases) was introduced during other instrument calibrations to check instrument zero. High- and a mid-range % CO₂ and O₂ levels in balance nitrogen were also introduced. Zero and mid-range calibrations were performed using USEPA Protocol gas after each test run. Copies of the gas cylinder certifications are found in Appendix H. This testing met the performance specifications as outlined in the Method.

Method 5 Filterable Particulate Matter Determination

Exhaust gas FPM concentrations and emission rates were determined in accordance with Method 5. An Environmental Supply Company sampling train was used to sample stack gas at an isokinetic rate, as specified in the Method. Particulate matter in the sample probe was recovered using an acetone wash. The probe wash and filter catch were analyzed by Mostardi Platt in accordance with the Method. Laboratory analysis data are included in Appendix E. All of the equipment used was calibrated in accordance with the specifications of the Method. Calibration data are presented in Appendix H.

Method 202 Condensable Particulate Determination

Stack gas condensable particulate matter concentrations and emission rates were determined in accordance with USEPA Method 202, in conjunction with Method 5 filterable particulate sampling. This method applies to the determination of condensable particulate matter (CPM) emissions from stationary sources. It is intended to represent condensable matter as material that condenses after passing through a filter and as measured by this method.

The CPM was collected in the impinger portion of the Method 5 (Appendix A, 40CFR60) type sampling trains. The impinger contents were immediately purged after each run with nitrogen (N₂) to remove dissolved sulfur dioxide (SO₂) gases from the impinger contents. The impinger solution was then extracted with hexane. The organic and aqueous fractions were then taken to dryness and the residues weighed. A correction was made for any ammonia present due to laboratory analysis procedures. The total of both fractions represents the CPM.

Laboratory analysis data are included in Appendix E. All the equipment used was calibrated in accordance with the specifications of the Method. Calibration data are presented in Appendix H.

Method 7E Nitrogen Oxides Determination

Stack gas NO_x concentrations and emission rates were determined in accordance with USEPA Method 7E, 40CFR60, Appendix A. A Thermo Scientific Model 42i-HL Chemiluminescence Nitrogen Oxides Analyzer was used to determine nitrogen oxides concentrations, in the manner specified in the Method. The instrument operated in the nominal range of 0 ppm to 100 ppm with the specific range determined by the high-level span calibration gas.

The Model 42i operates on the principle that nitric oxide (NO) and ozone (O₃) react to produce a characteristic luminescence with an intensity linearly proportional to the NO concentration. Infrared light emission results when electronically excited NO₂ molecules decay to lower energy states. Specifically,



Nitrogen dioxide (NO₂) must first be transformed into NO before it can be measured using the chemiluminescent reaction. NO₂ is converted to NO by a molybdenum NO₂-to-NO converter heated to about 329°C. The flue gas sample is drawn into the Model 42i through the sample bulkhead. The sample flows through a capillary, and then to the mode solenoid valve. The solenoid valve routes the sample either straight to the reaction chamber (NO mode) or through the NO₂-to-NO converter and then to the reaction chamber (NO_x mode). A flow sensor prior to the reaction chamber measures the sample flow. Dry air enters the Model 42i through the dry air bulkhead, passes through a flow switch, and then through a silent discharge ozonator. The ozonator generates the ozone needed for the chemiluminescent reaction. At the reaction chamber, the ozone reacts with the NO in the sample to produce excited NO₂ molecules. A photomultiplier tube (PMT) housed in a thermoelectric cooler detects the luminescence generated during this reaction. From the reaction chamber, the exhaust travels through the ozone (O₃) converter to the pump and is released through the vent.

The NO and NO_x concentrations calculated in the NO and NO_x modes are stored in memory. The difference between the concentrations is used to calculate the NO₂ concentration. The Model 42i outputs NO, NO₂, and NO_x concentrations to the front panel display, the analog outputs, and also makes the data available over the serial or ethernet connection.

Stack gas was delivered to the analyzer via a Teflon® sampling line, heated to a minimum temperature of 250°F. Excess moisture in the stack gas was removed using a refrigerated condenser. The entire system was calibrated in accordance with the Method, using USEPA Protocol gases introduced at the probe, before and after each test run. This testing met the performance specifications as outlined in the Method.

A list of calibration gases used and the results of all calibration and other required quality assurance checks are found in Appendix G. Copies of the gas cylinder certifications are found in Appendix H. The NO₂ to NO converter test can be found in Appendix I. This testing met the performance specifications as outlined in the Method.

Method 25A Volatile Organic Compound (VOC) Determination

The Method 25A sampling and measurement system meets the requirements for sampling of volatile organic compounds (VOCs) set forth by the USEPA. In particular, it meets the requirements of USEPA Reference Method 25A, "Determination of Total Gaseous Organic Concentration Using a Flame Ionization Analyzer," 40CFR60, Appendix A. This method applies to the measurement of total gaseous organic concentration of hydrocarbons. With this method, gas samples are extracted from the sample locations through heated Teflon sample lines to the analyzers.

The FIDs used during this program was a Thermo 51i analyzer. It is a highly sensitive FID that provides a direct reading of total organic vapor concentrations with linear ranges of 0-100 ppm by volume. The instrument was calibrated using ultra-zero air and methane in air EPA Protocol standards. The calibrations were performed before and after sampling with calibration checks performed between each test run. Sample times and locations were logged simultaneously on data loggers.

Calculations were performed by computer or by hand. An explanation of the nomenclature and calculations along with the complete test results is included in the appendix. Also appended are calibration data and copies of the raw field data sheets.

RECEIVED

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AIR QUALITY DIVISION
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3.0 TEST RESULT SUMMARIES

Client: Lansing Board of Water & Light
Facility: Delta Energy Park Facility
Test Location: EUCTGHRSG3 (Combined Cycle)
Test Method: 5/202

| Source Condition | Full Load | Full Load | Full Load | |
|--|-----------|-----------|-----------|---------|
| Date | 6/1/23 | 6/1/23 | 6/1/23 | |
| Start Time | 6:26 | 9:04 | 11:51 | |
| End Time | 8:36 | 11:14 | 14:00 | |
| | Run 1 | Run 2 | Run 3 | Average |
| Stack Conditions | | | | |
| Average Gas Temperature, °F | 220.3 | 220.4 | 221.4 | 220.7 |
| Flue Gas Moisture, percent by volume | 10.1% | 10.0% | 8.2% | 9.4% |
| Average Flue Pressure, in. Hg | 28.97 | 28.97 | 28.97 | 28.97 |
| Gas Sample Volume, dscf | 109.761 | 107.199 | 107.188 | 108.049 |
| Average Gas Velocity, ft/sec | 63.440 | 62.530 | 62.400 | 62.790 |
| Gas Volumetric Flow Rate, acfm | 298,955 | 294,666 | 294,053 | 295,891 |
| Gas Volumetric Flow Rate, dscfm | 202,038 | 199,237 | 202,399 | 201,225 |
| Gas Volumetric Flow Rate, scfm | 224,648 | 221,385 | 220,586 | 222,206 |
| Average %CO ₂ by volume, dry basis | 4.5 | 4.5 | 4.5 | 4.5 |
| Average %O ₂ by volume, dry basis | 12.8 | 12.8 | 12.9 | 12.8 |
| Isokinetic Variance | 103.5 | 102.5 | 100.9 | 102.3 |
| Standard Fuel Factor Fd, dscf/mmBtu | 8,710.0 | 8,710.0 | 8,710.0 | 8,710.0 |
| Filterable Particulate Matter (Method 5) | | | | |
| grams collected | 0.00040 | 0.00047 | 0.00126 | 0.00071 |
| grains/acf | 0.0000 | 0.0000 | 0.0001 | 0.0000 |
| grains/dscf | 0.0001 | 0.0001 | 0.0002 | 0.0001 |
| lb/hr | 0.097 | 0.116 | 0.315 | 0.176 |
| lb/1000 lb of stack gas | 0.000 | 0.000 | 0.000 | 0.000 |
| lb/mmBtu (Standard Fd Factor) | 0.0002 | 0.0002 | 0.0006 | 0.0003 |
| Condensable Particulate Matter (Method 202) | | | | |
| grams collected | 0.00282 | 0.00151 | 0.00148 | 0.00194 |
| grains/acf | 0.0003 | 0.0001 | 0.0001 | 0.0002 |
| grains/dscf | 0.0004 | 0.0002 | 0.0002 | 0.0003 |
| lb/hr | 0.687 | 0.371 | 0.370 | 0.476 |
| lb/1000 lb of stack gas | 0.001 | 0.000 | 0.000 | 0.001 |
| lb/mmBtu (Standard Fd Factor) | 0.0013 | 0.0007 | 0.0007 | 0.0009 |
| Total Particulate Matter (5/202) | | | | |
| grams collected | 0.00322 | 0.00198 | 0.00274 | 0.00265 |
| grains/acf | 0.0003 | 0.0001 | 0.0002 | 0.0002 |
| grains/dscf | 0.0005 | 0.0003 | 0.0004 | 0.0004 |
| lb/hr | 0.784 | 0.487 | 0.685 | 0.652 |
| lb/1000 lb of stack gas | 0.001 | 0.001 | 0.001 | 0.001 |
| lb/mmBtu (Standard Fd Factor) | 0.0015 | 0.0009 | 0.0013 | 0.0012 |

| Lansing Board of Water and Light Delta Energy Park EUCTGHRSG3 (Combined Cycle) Reference Method Test Data | | | | | | | | | |
|--|----------|------------|----------|-------------------------|-----------------|----------------------------|-------------------------|--|--------------------------|
| Test No. | Date | Start Time | End Time | NO _x , ppmvd | Flowrate, DSCFM | NO _x , lb/mmBtu | NO _x , lb/hr | NO _x ppmvd @ 15% O ₂ | O ₂ , % (dry) |
| 1 | 6/1/2023 | 6:45 | 7:05 | 2.9 | 202,038 | 0.008 | 4.18 | 2.10 | 12.8 |
| 2 | 6/1/2023 | 7:20 | 7:40 | 3.0 | 202,038 | 0.008 | 4.31 | 2.18 | 12.8 |
| 3 | 6/1/2023 | 7:57 | 8:17 | 3.0 | 202,038 | 0.008 | 4.32 | 2.18 | 12.8 |
| Average Runs 1-3 | | | | 2.9 | 202,038 | 0.008 | 4.27 | 2.15 | 12.8 |
| 4 | 6/1/2023 | 8:42 | 9:02 | 2.9 | 199,237 | 0.008 | 4.20 | 2.15 | 12.8 |
| 5 | 6/1/2023 | 9:25 | 9:45 | 3.0 | 199,237 | 0.008 | 4.29 | 2.19 | 12.8 |
| 6 | 6/1/2023 | 10:01 | 10:21 | 3.0 | 199,237 | 0.008 | 4.25 | 2.18 | 12.8 |
| Average Runs 4-6 | | | | 3.0 | 199,237 | 0.008 | 4.25 | 2.18 | 12.8 |
| 7 | 6/1/2023 | 10:47 | 11:07 | 3.2 | 202,399 | 0.009 | 4.63 | 2.35 | 12.9 |
| 8 | 6/1/2023 | 11:22 | 11:42 | 3.1 | 202,399 | 0.008 | 4.52 | 2.29 | 12.9 |
| 9 | 6/1/2023 | 12:00 | 12:20 | 3.1 | 202,399 | 0.008 | 4.53 | 2.30 | 12.9 |
| Average Runs 7-9 | | | | 3.1 | 202,399 | 0.009 | 4.56 | 2.32 | 12.9 |
| Average Runs 1-9 | | | | 3.0 | 201,225 | 0.008 | 4.36 | 2.22 | 12.8 |

| Lansing Board of Water & Light Delta Energy Park EUCTHRSG3 (Combined Cycle) Gaseous Summary Normal Load | | | | | | | | | | |
|---|----------|------------|----------|-------------|-----------------|----------------|----------------------|--|--|------------------------------------|
| Test No. | Date | Start Time | End Time | Moisture, % | Flowrate, DSCFM | Flowrate, SCFM | O ₂ % dry | THC ppm as C ₃ H ₈ (wet) | THC ppm as C ₃ H ₈ (dry) | VOC ppm @ 15% O ₂ (dry) |
| 1 | 06/01/23 | 06:45 | 08:17 | 10.1 | 202,038 | 224,648 | 12.8 | 0.1 | 0.1 | 0.1 |
| 2 | 06/01/23 | 08:42 | 10:21 | 10.0 | 199,237 | 221,385 | 12.8 | 0.1 | 0.1 | 0.1 |
| 3 | 06/01/23 | 10:47 | 12:20 | 8.2 | 202,399 | 220,586 | 12.9 | 0.1 | 0.1 | 0.1 |
| Average | | | | 9.4 | 201,225 | 222,206 | 12.8 | 0.1 | 0.1 | 0.1 |

4.0 CERTIFICATION

Mostardi Platt is pleased to have been of service to Lansing Board of Water & Light. If you have any questions regarding this test report, please do not hesitate to contact us at 630-993-2100.

As the program manager, I hereby certify that this test report represents a true and accurate summary of emissions test results and the methodologies employed to obtain those results. The test program was performed in accordance with the test methods and the Mostardi Platt Quality Manual, as applicable.

MOSTARDI PLATT



Jacob Howe

Program Manager



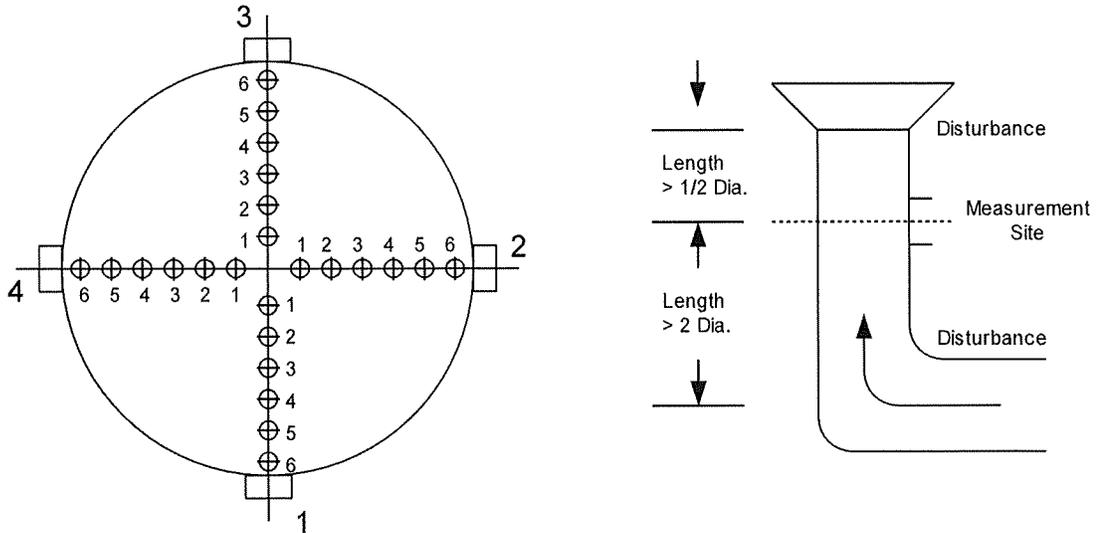
Scott W. Banach

Quality Assurance

APPENDICES

Appendix A - Test Section Diagrams

EQUAL AREA TRAVERSE FOR ROUND DUCTS



Job: Lansing Board of Water & Light
Delta Energy Park
Lansing, MI

Date: June 1, 2023

Test Location: EUCTGHRSG3 (COMB)

Duct Diameter: 10 Feet

Duct Area: 78.54 Square Feet

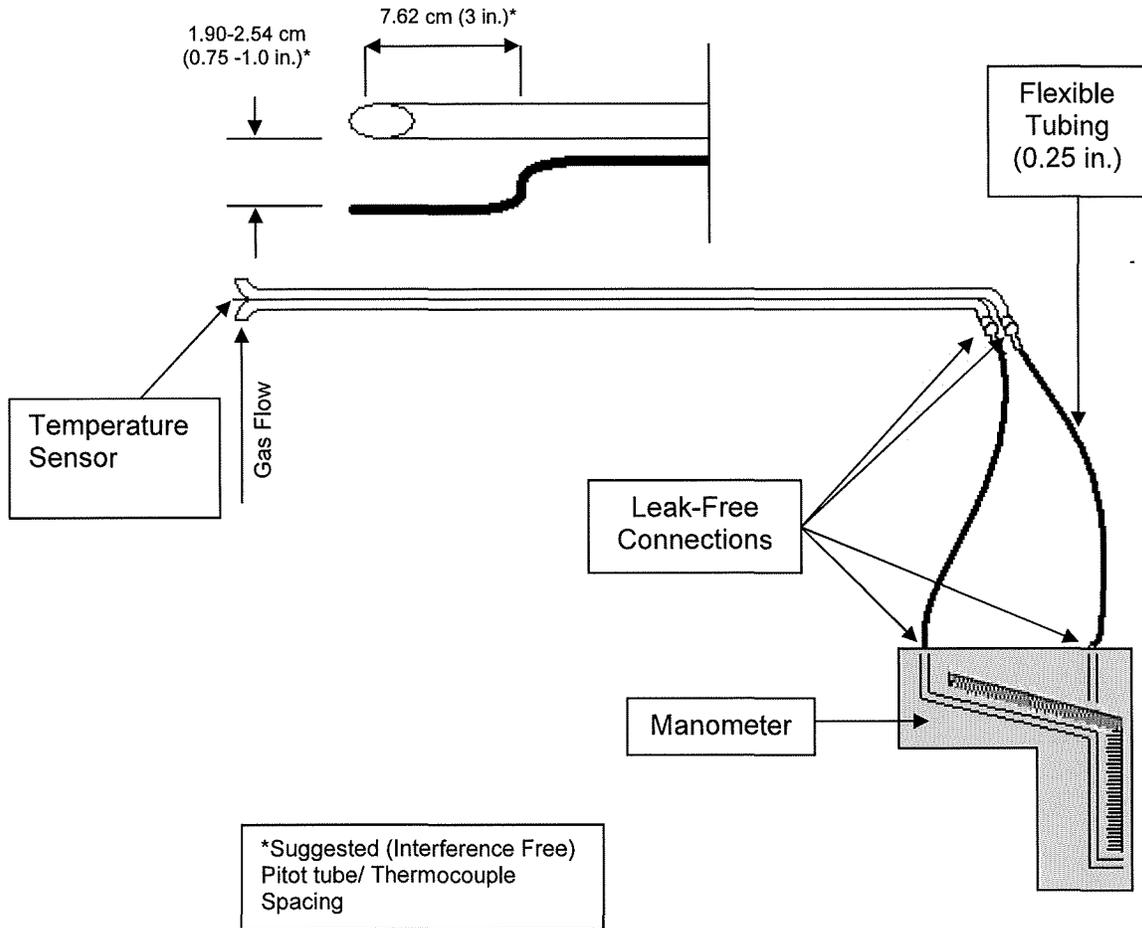
No. Points Across Diameter: 12

No. of Ports: 4

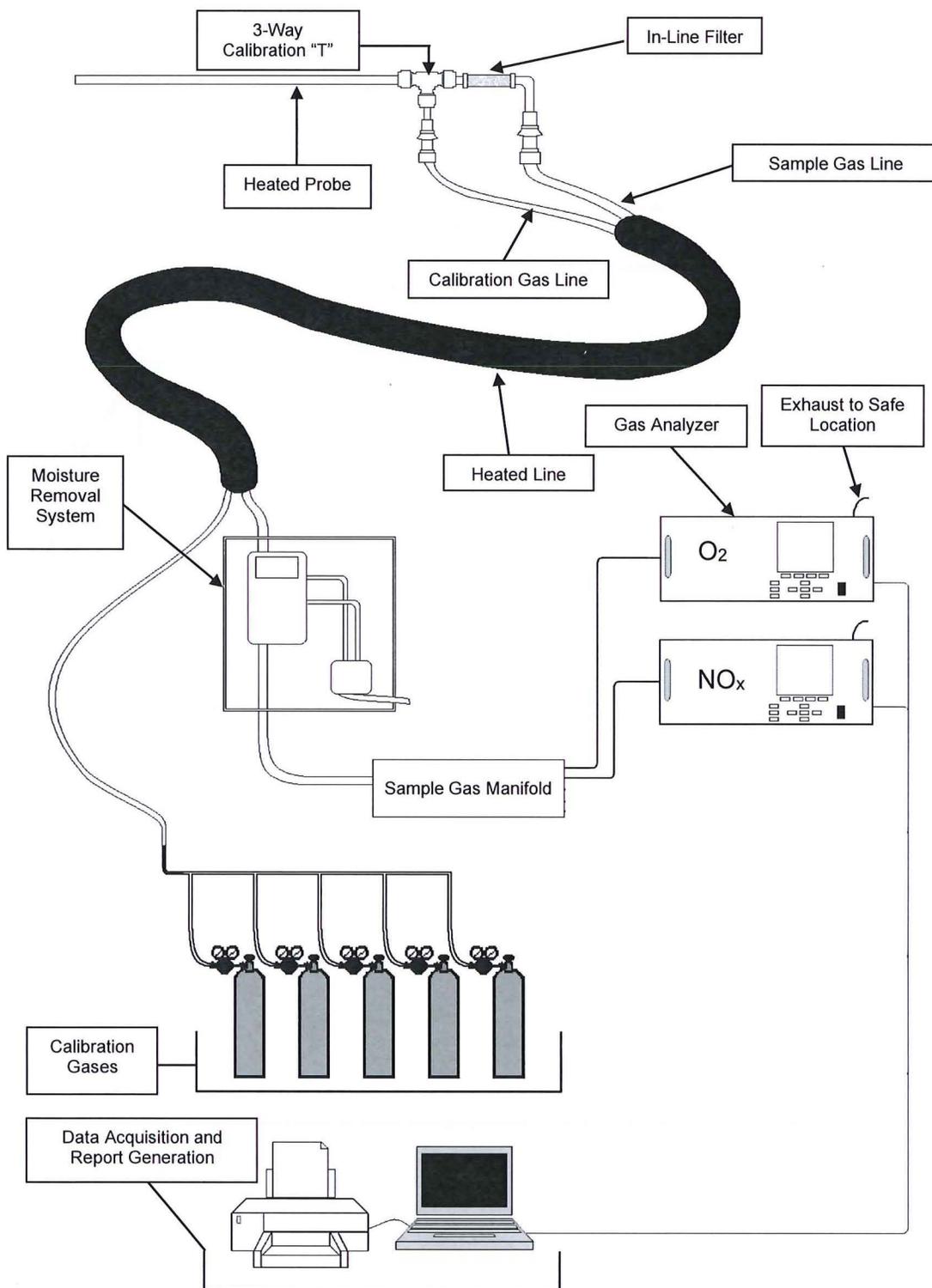
Port Length: 6 Inches

Appendix B - Sample Train Diagrams

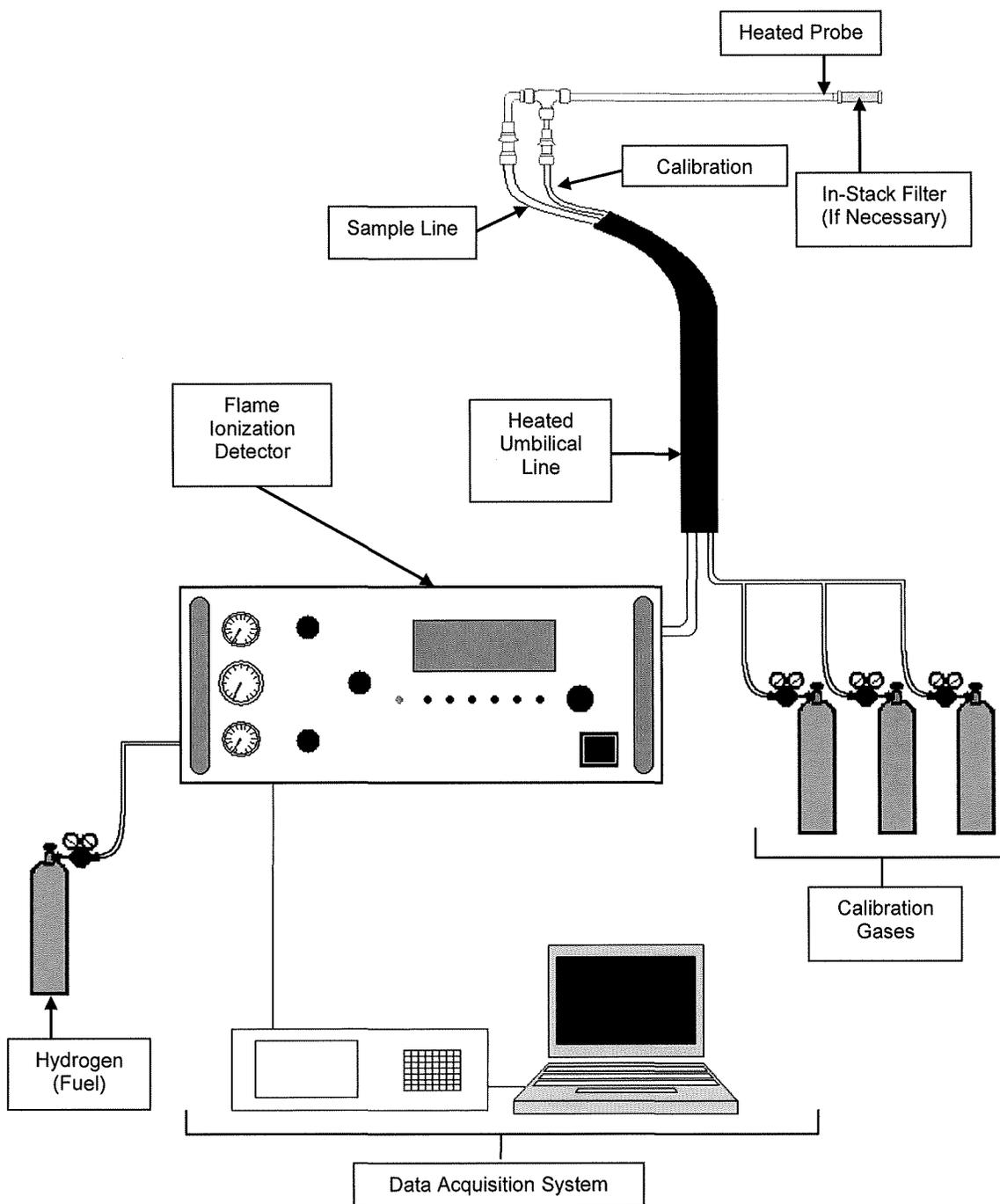
USEPA Method 2 – Type S Pitot Tube Manometer Assembly



USEPA Methods 3A and 7E Extractive Gaseous Sampling Diagram



USEPA Method 25A – Total Gaseous Organic Compound Sample Train



USEPA Method 5/202- Filterable/Condensable Particulate Matter

