

January 18, 2022

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Karen Kajiya-Mills **Michigan Department of Environment, Great Lakes, and Energy** Air Quality Division – Technical Programs Unit Constitution Hall, 2<sup>nd</sup> Floor, South 525 West Allegan Street Lansing, Michigan 48909

Rebecca Radulski **Michigan Department of Environment, Great Lakes, and Energy** Air Quality Division – Gaylord Field Office 2100 West M-32 Gaylord, Michigan 49735 radulskir@michigan.gov

#### Apex Project No. 11021-000062.00

Subject: Air Emissions Test Report No. 1 Biofilter Compliance Air Emissions Test Decorative Panels International SRN B1476 416 Ford Avenue Alpena, Michigan Renewable Operating Permit MI-ROP-B1476-2015a

Dear Ms. Kajiya-Mills and Ms. Radulski:

On behalf of Decorative Panels International, Inc., Apex Companies, LLC submits this report for compliance air emissions testing at the Decorative Panels International facility in Alpena, Michigan. The compliance testing was conducted on November 30, 2021.

If you have any questions, please contact us.

Sincerely,

Clouski

David Kawasaki, QSTI Senior Engineer Apex Companies, LLC <u>david kawasaki@apexcos.com</u> Telephone 248.590.5134

Derek R. Wong, Ph.D., P.E. National Account Manager Apex Companies, LLC <u>derek.wong@apexcos.com</u> Telephone 248.875.7581

cc: Timothy Rombach, Senior Environmental Engineer – Decorative Panels International, Inc.

B1476\_test\_20211130

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MICHIGAN DEPARTMENT OF ENVIRONMENT, GREAT LAKES, AND ENERGY AIR QUALITY DIVISION

## **RENEWABLE OPERATING PERMIT**

**REPORT CERTIFICATION** 

Authorized by 1994 P.A. 451, as amended. Failure to provide this information may result in civil and/or criminal penalties.

Reports submitted pursuant to R 336.1213 (Rule 213), subrules (3)(c) and/or (4)(c), of Michigan's Renewable Operating Permit (ROP) program must be certified by a responsible official. Additional information regarding the reports and documentation listed below must be kept on file for at least 5 years, as specified in Rule 213(3)(b)(ii), and be made available to the Department of Environment, Great Lakes, and Energy, Air Quality Division upon request. Source Name Decorative Panels International County Alpena Source Address 416 Ford Avenue City Alpena AQD Source ID (SRN) B1476 ROP No. B1476-2015a ROP Section No. D Please check the appropriate box(es): Annual Compliance Certification (Pursuant to Rule 213(4)(c)) Reporting period (provide inclusive dates): From То 1. During the entire reporting period, this source was in compliance with ALL terms and conditions contained in the ROP, each term and condition of which is identified and included by this reference. The method(s) used to determine compliance is/are the method(s) specified in the ROP. 2. During the entire reporting period this source was in compliance with all terms and conditions contained in the ROP, each term and condition of which is identified and included by this reference, EXCEPT for the deviations identified on the enclosed deviation report(s). The method used to determine compliance for each term and condition is the method specified in the ROP, unless otherwise indicated and described on the enclosed deviation report(s). Semi-Annual (or More Frequent) Report Certification (Pursuant to Rule 213(3)(c)) Reporting period (provide inclusive dates): From То 1. During the entire reporting period, ALL monitoring and associated recordkeeping requirements in the ROP were met and no deviations from these requirements or any other terms or conditions occurred. 2. During the entire reporting period, all monitoring and associated recordkeeping requirements in the ROP were met and no deviations from these requirements or any other terms or conditions occurred. EXCEPT for the deviations identified on the enclosed deviation report(s). Other Report Certification Reporting period (provide inclusive dates): NA То NA From Additional monitoring reports or other applicable documents required by the ROP are attached as described:

Air Emissions Test Report to evaluate compliance of the No. 1 Biofilter source.

This form shall certify that the testing was conducted in accordance with the

approved test plan and that the facility operating conditions were in compliance with

permit requirements.

I certify that, based on information and belief formed after reasonable inquiry, the statements and information in this report and the supporting enclosures are true, accurate and complete

Dan VanMassenhove	Plant Manager	989.356.8540
Name of Responsible Official (print or type)	Title	Phone Number
DanValle	Communication and and a second s	1/28/22
Signature of Responsible Official	RECEIV	Dale
* Photocopy this form as needed.	* FEB 1 6 2022	EQP 5736 (Rev 04/30/2019)
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APEX COMPANIES, LLC



Air Emissions Test Report No. 1 Biofilter Compliance Test



PREPARED FOR: Decorative Panels International, Inc. 416 Ford Street Alpena, Michigan 49707

State Registration No. B1476

Apex Project No. 11021-000062.00 January 18, 2022

Apex Companies, LLC 46555 Humboldt Drive, Suite 103 Novi, Michigan 48377



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## Table of Contents

Execu	tive Summary
1.0	Introduction
1.1	Summary of Test Program
1.2	Key Personnel 1
2.0	Source and Sampling Locations
2.1	Process Description
2.2	Control Equipment Description
2.3	Flue Gas Sampling Locations
2.3.1	No. 1 Biofilter Inlet Sampling Location4
2.3.2	No. 1 Biofilter Outlet Sampling Location4
2.4	Process Sampling Locations
3.0	Summary and Discussion of Results7
3.1	Objectives and Test Matrix7
3.2	Field Test Changes and Issues
3.3	Summary of Results
4.0	Sampling and Analytical Procedures9
4.1	Emission Test Methods9
4.1.1	Volumetric Flowrate (USEPA Methods 1 and 2)9
4.1.2	Molecular Weight (USEPA Method 3)10
4.1.3	Total Hydrocarbons (USEPA Method 25A)10
4.1.4	Gas Dilution (USEPA Method 205)11
4.1.5	Formaldehyde, Methanol, and Moisture Content (USEPA Method 320)12
4.2	Process Data12
5.0	Quality Assurance and Quality Control13
5.1	QA/QC Procedures
5.2	QA/QC Audits
5.2.1	Audit Sample Results QA/QC13
5.2.2	Instrument Analyzer QA/QC13
5.3	Data Reduction and Validation13
5.4	QA/QC Problems
6.0	Limitations15

## **Tables**

1-1	Sources Tested, Parameters, and Test Date	1
1-2	Key Contact Information	2
2-1	Summary of EUPRESS2S Operating Data	3
2-2	Summary of No. 1 Biofilter Operating Data	4
3-1	Sampling and Analytical Matrix	7
3-2	No. 1 Biofilter Hazardous Air Pollutants Emissions Results	8
4-1	Emission Testing Methods	9
5-1	Calibration Gas Cylinder Information	13

## **Figures**

2-1	No. 1 Biofilter Inlet Sampling Location
2-2	No. 1 Biofilter Outlet Sampling Location
4-1	USEPA Method 25A Sampling Train11
4-2	USEPA Method 320 Sampling Train12

## Appendix

#### Tables

1 No. 1 Biofilter Emissions Results

#### **Figures**

- 1 No. 1 Biofilter Inlet Sampling Ports and Traverse Point Locations
- 2 No. 1 Biofilter Outlet Sampling Ports and Traverse Point Locations

#### Graphs

- 1 No. 1 Biofilter Inlet and Outlet Concentrations Run 1
- 2 No. 1 Biofilter Inlet and Outlet Concentrations Run 2
- 3 No. 1 Biofilter Inlet and Outlet Concentrations Run 3

### Appendix

- A Calibration and Inspection Sheets
- **B** Sample Calculations
- C Field Data Sheets
- D Computer-Generated Data Sheets
- E FTIR Data
- F Facility Operating Data

## **Executive Summary**

Decorative Panels International, Inc. (DPI) retained Apex Companies, LLC (Apex) to test air emissions from the No. 1 Biofilter at the DPI facility in Alpena, Michigan. The No. 1 Biofilter controls emissions from the No. 1 Board Press and cooler (EUPRESS2S).

The source is regulated by (1) Michigan Department of Environment, Great Lakes, and Energy (EGLE) Renewable Operating Permit (ROP) No. MI-ROP-B1476-2015a, effective April 6, 2016, and (2) National Emission Standards for Hazardous Air Pollutants (NESHAP): Plywood and Composite Wood Products, 40 CFR 63, Subpart DDDD.

Compliance with the FGMACTDDDD total hazardous air pollutant (HAP) permit limits based on the use of an add-on control device can be demonstrated by one of the following:

1. 90% reduction of total HAP mass emission rate, measured as total hydrocarbons

NUMBER OF STREET

- 2. Total HAP concentration less than 20 ppmvd, measured as total hydrocarbons
- 3. Total HAP reduction so that methanol mass emission rate is reduced by 90%
- 4. Total HAP reduction such that methanol concentration is less than 1 ppmvd, if the uncontrolled methanol concentration entering the control device is greater than 10 ppmvd
- 5. Total HAP reduction so that formaldehyde mass emission rate is reduced by 90%
- 6. Total HAP reduction such that formaldehyde concentration is less than 1 ppmvd, if the uncontrolled formaldehyde concentration entering the control device is greater than 10 ppmvd

Apex measured formaldehyde, methanol, and total hydrocarbons (THC) at the inlet and outlet of the No. 1 Biofilter control device. The testing followed United States Environmental Protection Agency Reference Methods 1 through 3, 25A, 205, and 320.

Detailed results are presented in Table 1 after the Tables Tab of this report. The following table summarizes the results of testing conducted on November 30, 2021.

No. 1 Biofilter Hazardous Air Pollutants
<b>Emissions Results</b>

Parameter	Unit	Average Result Test Runs 1 to 3	Permit Limit
Formaldehyde inlet concentration	ppmv, wet	30.2	
Formaldehyde inlet emission rate	lb/hr	7.6	
Formaldehyde outlet concentration	ppmv, wet	0.65	1+
Formaldehyde outlet emission rate	lb/hr	0.21	
Formaldehyde removal efficiency	%	97	≥90†
Methanol inlet concentration	ppmv, wet	35.0	
Methanol inlet emission rate	lb/hr	9.4	·
Methanol outlet concentration	ppmv, wet	9.5	1+
Methanol outlet emission rate	lb/hr	3.3	
Methanol removal efficiency	%	65	≥90†
THC inlet concentration	ppmv, wet as propane	92.4	
THC inlet emission rate	lb/hr, as propane	34.2	
THC outlet concentration	ppmv, wet as propane	13.5	20†
THC outlet emission rate	lb/hr, as propane	6.5	
THC removal efficiency	%	81	≥90†

THC: total hydrocarbons

ppmv, wet: part per million by volume, wet basis

lb/hr: pound per hour

† Only one of the six permit limits need to be met in order to demonstrate compliance.

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## 1.0 Introduction

#### 1.1 Summary of Test Program

Decorative Panels International (DPI) retained Apex Companies, LLC (Apex) to conduct air emissions testing at the DPI facility in Alpena, Michigan. The No. 1 Biofilter controls emissions from the No. 1 Board Press and cooler (EUPRESS2S).

The purpose of the air emission testing was to evaluate compliance with certain emission limits in (1) Michigan Department of Environment, Great Lakes, and Energy (EGLE) Renewable Operating Permit (ROP) MI-ROP-B1476-2015a, effective April 6, 2016, and (2) National Emission Standards for Hazardous Air Pollutants (NESHAP): Plywood and Composite Wood Products, 40 CFR 63, Subpart DDDD.

Apex measured formaldehyde, methanol, and total hydrocarbons (THC) at the inlet and outlet of the No. 1 Biofilter control device. The testing followed United States Environmental Protection Agency (USEPA) Reference Methods 1 through 3, 25A, 205, and 320.

Table 1-1 lists the emission sources tested, parameters, and test date.

# Table 1-1Sources Tested, Parameters, and Test Date

Source	Test Parameter	Test Date	
No. 1 Biofilter	Formaldehyde	November 30, 2021	
Inlet and Outlet	Methanol		
	Total hydrocarbons (THCs)		

#### 1.2 Key Personnel

The key personnel involved in this test program are listed in Table 1-2. Mr. David Kawasaki, Senior Engineer with Apex, led the emission testing program. Mr. Timothy Rombach, Senior Environmental Engineer with DPI, provided process coordination and recorded operating parameters. Mr. Jeremey Howe, with EGLE, witnessed the testing and verified production parameters were recorded.

Client	Арех
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## Table 1-2 Key Contact Information

# 2.0 Source and Sampling Locations

#### 2.1 Process Description

Decorative Panels International produces a variety of hardboard products including wall paneling, pegboard, and marker board. Hardwood chips, such as aspen, ash, maple, and beech chips, are purchased and stored in an outdoor raw material storage area and reclaimed into silos. The wood chips are cooked and softened in one of four digesters using steam injection and ground into wood pulp fibers.

The pulp fibers are conveyed to a forming machine, which forms a mat of un-pressed hardboard. The mats are processed through a Coe<sup>®</sup> dryer and cut using a trimmer and panel brush. The mats are conveyed to one of two hardboard lines, Line 1 or 3. Line 2 was historically operated but has since been decommissioned.

On the hardboard lines, the mats enter a predryer, a press, cooler, and tempering area. The predryer ensures the mat has the desired moisture content before the mat enters presses that heat and form hardboard. The hardboard is coated with linseed or Oxi-Cure<sup>®</sup> oil in the tempering area. The oil tempers the board thereby increasing its strength and "paintability." Once the board has been tempered, it is superheated to cure the binding resins in the bake ovens (No. 3 Press line only). The hardboard is humidified to approximate atmospheric conditions to limit warping. The boards are inspected, graded, cut, and packed for shipping.

The No. 1 Biofilter controls emissions from the No. 1 Board Press and cooler.

Operating parameters were measured and recorded by DPI personnel during testing. Table 2-1 summarizes the operating conditions during hazardous air pollutant (HAP) compliance testing of the No. 1 Biofilter source. Additional operating parameter data are included in Appendix F.

Test Run	Number of Press Cycles
1	20
2	21
3	21
Average	21

### Table 2-1 Summary of EUPRESS2S Operating Data

#### 2.2 Control Equipment Description

Gaseous emissions from the No. 1 Board Press are controlled by a DynaWave Engineering water scrubber and the No. 1 Biofilter. Emissions from the No. 1 Board Press are captured by a permanent total enclosure that surrounds the press area. The air from the enclosure continuously exhausts through a duct that exits the roof of the building and flows towards the pollution control equipment. The captured air (flue gas) enters the top of the scrubber and flows downwards in the vessel. Inside the vessel, water (containing sodium hydroxide to maintain a neutral pH) is sprayed into the air to remove particulates and humidify the air before the air enters the biofilter. The water is sprayed onto a series of chevrons to increase the air-to-water contact surface area.

As the flue gas mixes with the water, particulates and other pollutants are removed. The water drains to the bottom of the vessel and a portion is recirculated into the system with the remaining portion discharged to the onsite water treatment system. The flue gas exits the top of the scrubber and flows into the No. 1 Biofilter.

The No. 1 Biofilter, manufactured by Monsanto Enviro-Chem., consists of six compartments. The air from the scrubber can be heated by a heat exchanger before being directed into the six-biobed compartments. The compartments contain water sprayers to maintain a moist environment, and layers of Douglas-fir bark from the western United States. The Douglas-fir bark provides an environment where biologically active microbes can oxidize and remove the contaminants.

After passing through the bark, the flue gas is drawn into fans that discharge the gas through stack, SVS2COOLR-STK28.

Biofilter bed temperature and pressure drop were measured and recorded by DPI personnel during testing. Table 2-2 summarizes the operating conditions during testing of the No. 1 Biofilter. Detailed operating parameter data are included in Appendix F.

Test Run	Average Bed Temperature (°F)	Average Bed Pressure Drop (inch H <sub>2</sub> O)
1	75	0.5
2	76	0.5
3	77	0.5

### Table 2-2 Summary of No. 1 Biofilter Operating Data

#### 2.3 Flue Gas Sampling Locations

#### 2.3.1 No. 1 Biofilter Inlet Sampling Location

Two sampling ports oriented at 90° to one another are located in a straight section of a 59.75 inch-internal-diameter duct. The sampling ports are located:

- Approximately 480 inches (8.0 duct diameters) from the nearest downstream disturbance.
- Approximately 528 inches (8.8 duct diameters) from the nearest upstream disturbance.

The sampling ports are accessible via platform. A photograph of the No. 1 Biofilter inlet sampling location is presented in Figure 2-1. Figure 1 in the Appendix depicts the No. 1 Biofilter inlet sampling ports and traverse point locations.

#### 2.3.2 No. 1 Biofilter Outlet Sampling Location

Two sampling ports oriented at 90° to one another are located in a straight section of a 59.25 inch-internal-diameter duct. The sampling ports are located:

- Approximately 200 inches (3.4 duct diameters) from the nearest downstream disturbance.
- Approximately 450 inches (7.6 duct diameters) from the nearest upstream disturbance.

The sampling ports are accessible from the roof of the building. A photograph of the No. 1 Biofilter outlet sampling location is presented in Figure 2-2. Figure 2 in the Appendix depicts the No. 1 Biofilter outlet sampling ports and traverse point locations.

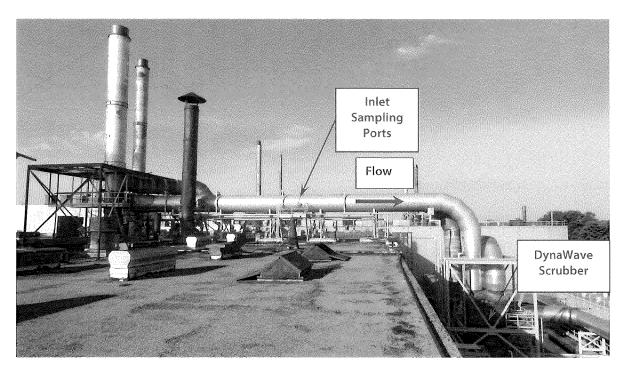


Figure 2-1. No. 1 Biofilter Inlet Sampling Location

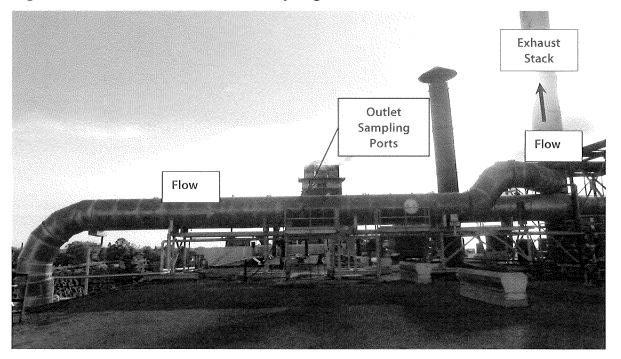


Figure 2-2. No. 1 Biofilter Outlet Sampling Location

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## 2.4 Process Sampling Locations

Process sampling was not required during this test program. A process sample is a sample that is analyzed for operational parameters, such as calorific value of a fuel (e.g., natural gas, coal), organic compound content (e.g., paint coatings), or composition (e.g., polymers).

# 3.0 Summary and Discussion of Results

#### 3.1 Objectives and Test Matrix

The objective of the air emission testing was to evaluate compliance of the No. 1 Biofilter with certain emission limits and requirements in (1) EGLE ROP MI-ROP-B1476-2015a, effective April 6, 2016, and (2) NESHAP: Plywood and Composite Wood Products, 40 CFR 63, Subpart DDDD.

Compliance with the FGMACTDDDD total HAP permit limits based on the use of an add-on control device can be demonstrated by one of the following:

- 1. 90% reduction of total HAP mass emission rate, measured as total hydrocarbons
- 2. Total HAP concentration less than 20 ppmvd, measured as total hydrocarbons
- 3. Total HAP reduction so that methanol mass emission rate is reduced by 90%

4. Total HAP reduction such that methanol concentration is less than 1 ppmvd, if the uncontrolled methanol concentration entering the control device is greater than 10 ppmvd

5. Total HAP reduction so that formaldehyde mass emission rate is reduced by 90%

6. Total HAP reduction such that formaldehyde concentration is less than 1 ppmvd, if the uncontrolled formaldehyde concentration entering the control device is greater than 10 ppmvd

Apex measured formaldehyde, methanol, and THC at the inlet and outlet of the No. 1 Biofilter control device. Table 3-1 summarizes the sampling and analytical matrix.

# Table 3-1Sampling and Analytical Matrix

Source	Sample/Type of Pollutant	Sampling Method	Date (2021)	Run	Start Time	End Time	Analytical Laboratory
No. 1 Biofilter Inlet and Outlet	Flowrate, molecular weight, formaldehyde,	USEPA 1, 2, 3, 25A, 205, and	Nov. 30	1	08:51	09:51	Not applicable
	methanol, THC	320		2	10:11	11:11	••
				3	11:34	12:34	

#### 3.2 Field Test Changes and Issues

Communication between DPI, Apex, and EGLE allowed the testing to be completed, as proposed in the October 4, 2021 Intent-to-Test Plan.

#### 3.3 Summary of Results

The results of testing are presented in Table 3-2. Detailed results are presented in Table 1 after the Tables Tab of this report. Graphs are presented after the Graphs Tab of this report. Sample calculations are presented in Appendix B.

## Table 3-2 No. 1 Biofilter Hazardous Air Pollutants Emissions Results

Parameter	Unit	Run 1	Run 2	Run 3	Average Result	Permit Limit
Formaldehyde inlet concentration	ppmv, wet	26.5	31.9	32.2	30.2	
Formaldehyde inlet emission rate	lb/hr	6.7	8.1	8.0	7.6	
Formaldehyde outlet concentration	ppmv, wet	0.48	0.70	0.78	0.65	1†
Formaldehyde outlet emission rate	lb/hr	0.16	0.22	0.26	0.21	-
Formaldehyde removal efficiency	%	98	97	97	97	≥ <b>90</b> †
Methanol inlet concentration	ppmv, wet	32.6	36.3	36.1	35.0	
Methanol inlet emission rate	lb/hr	8.8	9.9	9.6	9.4	
Methanol outlet concentration	ppmv, wet	6.9	10.0	11.6	9.5	1†
Methanol outlet emission rate	lb/hr	2.4	3.4	4.0	3.3	
Methanol removal efficiency	%	72	65	58	65	≥90†
THC inlet concentration	ppmv, wet as propane	86.8	95.7	94.6	92.4	
THC inlet emission rate	lb/hr, as propane	32.1	35.8	34.6	34.2	
THC outlet concentration	ppmv, wet as propane	11.2	13.8	15.5	13.5	20†
THC outlet emission rate	lb/hr, as propane	5.4	6.5	7.4	6.5	
THC removal efficiency	%	83	82	79	81	≥ <b>90</b> †

THC: total hydrocarbons

ppmv, wet: part per million by volume, wet basis

lb/hr: pound per hour

† Only one of the six permit limits need to be met in order to demonstrate compliance.

Apex Project No. 11021-000062.00 Decorative Panels International, Inc., Alpena, Michigan

8

## 4.0 Sampling and Analytical Procedures

Apex measured emissions in accordance with USEPA sampling methods. Table 4-1 presents the emissions test parameters and sampling methods.

Parameter	No. 1 Biofilter Inlet and Outlet	USEPA Reference		
		Method	Title	
Sampling ports and traverse points	۲	1	Sample and Velocity Traverses for Stationary Sources	
Velocity and flowrate	•	2	Determination of Stack Gas Velocity and Volumetric Flow Rate (Type S Pitot Tube)	
Molecular weight	٠	. 3 /	Gas Analysis for the Determination of Dry Molecular Weight	
Total hydrocarbons	٠	25A	Determination of Total Gaseous Organic Concentration Using a Flame Ionization Analyzer	
Gas dilution	•	205	Verification of Gas Dilution Systems for Field Instrument Calibrations	
Formaldehyde, methanol, and moisture content	•	320	Measurements of Vapor Phase Organic and Inorganic Emissions by Extractive Fourier Transform Infrared	

### Table 4-1 Emission Testing Methods

#### 4.1 Emission Test Methods

#### 4.1.1 Volumetric Flowrate (USEPA Methods 1 and 2)

USEPA Method 1, "Sample and Velocity Traverses for Stationary Sources," was used to evaluate the sampling locations and the number of traverse points for sampling and the measurement of velocity profiles. Figures 1 and 2 in the Appendix depict the source locations and traverse points.

USEPA Method 2, "Determination of Stack Gas Velocity and Volumetric Flow Rate (Type S Pitot Tube)," was used to measure flue gas velocity and calculate volumetric flowrates. S-type Pitot tubes and thermocouple assemblies, calibrated in accordance with Method 2, Section 10.0, were used during testing. Because the dimensions of the Pitot tubes met the requirements outlined in Method 2, Section 10.1, and are within the specified limits, the baseline Pitot tube coefficient of 0.84 (dimensionless) was assigned. The digital manometer and thermometer are calibrated using calibration standards that are traceable to National Institute of Standards and Technology (NIST). Pitot tube inspection sheets are included in Appendix A.

**Cyclonic Flow Check**. Apex has evaluated whether cyclonic flow was present at the sampling locations during previous testing. Cyclonic flow is defined as a flow condition with an average null angle greater than 20°. The direction of flow can be determined by aligning the Pitot tube to obtain zero (null) velocity head reading—the direction would be parallel to the Pitot tube face openings or perpendicular to the null position. By measuring the angle of the Pitot tube face openings in relation to the stack walls when a null angle is obtained, the direction of flow is measured. If the absolute average of the flow direction angles is greater than 20°, the flue gas is considered to be cyclonic at that sampling location and an alternative location should be selected.

The average of the measured traverse point flue gas velocity null angles, during previous testing, were less than 20° at the sampling locations. The measurements indicate the absence of cyclonic flow.

Field data sheets are included in Appendix C. Computer-generated field data sheets are included in Appendix D.

#### 4.1.2 Molecular Weight (USEPA Method 3)

USEPA Method 3, "Gas Analysis for the Determination of Dry Molecular Weight," was used to determine the molecular weight of the flue gas. Flue gas was extracted from the stack through a probe positioned near the centroid of the duct and directed into a Fyrite<sup>®</sup> gas analyzer. The concentrations of carbon dioxide (CO<sub>2</sub>) and oxygen (O<sub>2</sub>) were measured by chemical absorption to within  $\pm 0.5$ %. The average CO<sub>2</sub> and O<sub>2</sub> results of the grab samples were used to calculate molecular weight.

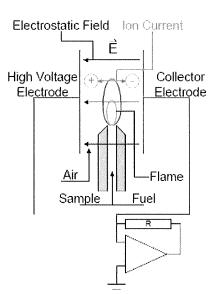
#### 4.1.3 Total Hydrocarbons (USEPA Method 25A)

USEPA Method 25A, "Determination of Total Gaseous Organic Concentration Using a Flame Ionization Analyzer," was used to measure total hydrocarbon concentrations in the flue gas. Samples were collected through a stainless steel probe and heated sample line into an analyzer.

A flame ionization detector (FID) determines the average hydrocarbon concentration in part per million by volume (ppmv) of THC as the calibration gas (i.e., propane). The FID is fueled by 100% hydrogen, which generates a flame with a negligible number of ions. Flue gas is introduced into the FID and enters the flame chamber. The combustion of flue gas generates electrically charged ions. The analyzer applies a polarizing voltage between two electrodes around the flame, producing an electrostatic field. Negatively charged ions, anions, migrate to a collector electrode, while positive charged ions, cations, migrate to a high-voltage electrode. The current between the electrodes is directly proportional to the hydrocarbon concentration in the sample. The flame chamber is depicted at right.

Using the voltage analog signal, measured by the FID, the concentration of THCs was recorded by a data acquisition system (DAS). The average concentration of THCs is reported as the calibration gas (i.e., propane) in equivalent units.

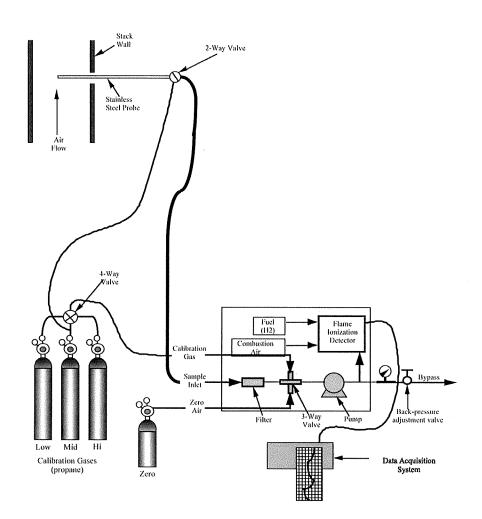
Before testing, the analyzer was calibrated by introducing a zerocalibration range gas (<1% of span value) and high-calibration range



gas (80-90% span value) to the tip of the sampling probe. The span value was set to 1.5 to 2.5 times the expected concentration (e.g., 0-100 ppmv). Next, a low-calibration range gas (25-35% of span value) and mid-calibration range gas (45-55% of span value) were introduced. The analyzers are considered to be calibrated when the analyzer response is ±5% of the calibration gas value.

At the conclusion of a test run, a calibration drift test was performed by introducing the zero- and mid-calibration gas to the tip of the sampling probe. The test run data was considered valid if the calibration drift test demonstrated the analyzers are responding within 3% of the calibration span from pre-test to post-test calibrations.

Figure 4-1 depicts the USEPA Method 25A sampling train.



### Figure 4-1. USEPA Method 25A Sampling Train

#### 4.1.4 Gas Dilution (USEPA Method 205)

USEPA Method 205, "Verification of Gas Dilution Systems for Field Instrument Calibrations," was used to introduce known values of calibration gases into the analyzers. The gas dilution system consists of calibrated orifices or mass flow controllers and dilutes a high-level calibration gas to within ±2% of predicted values. The gas divider is capable of diluting gases at set increments and was evaluated for accuracy in the field in accordance with USEPA Method 205.

Prior to testing, the gas divider dilutions were measured to evaluate that they were within  $\pm 2\%$  of predicted values. Two sets of three dilutions of the high-level calibration gas were performed. In addition, a certified mid-level calibration gas was introduced into an analyzer; this calibration gas concentration was within  $\pm 10\%$  of a gas divider dilution concentration.

Apex Project No. 11021-000062.00 Decorative Panels International, Inc., Alpena, Michigan 11



AIR QUALITY DIVISION

4.1.5 Formaldehyde, Methanol, and Moisture Content (USEPA Method 320)

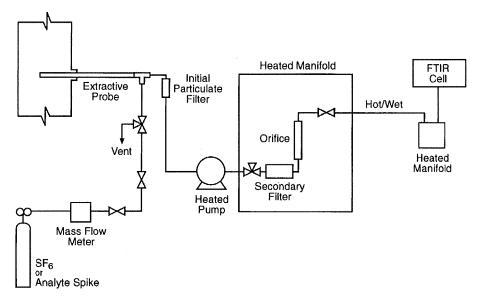
USEPA Method 320, "Measurements of Vapor Phase Organic and Inorganic Emissions by Extractive Fourier Transform Infrared (FTIR) Spectroscopy," was used to measure formaldehyde, methanol, and moisture content in the flue gas. Gaseous samples were withdrawn from the stack and transferred to an MKS Instruments MultiGas 2030 FTIR spectrometer.

The sample gas was directed through a heated probe, heated filter and heated transfer line connected to the FTIR. The probe, filter, transfer line, and FTIR were maintained at 191°C (375°F) during testing. The formaldehyde, methanol, and moisture concentrations were measured based on their infrared absorbance compared to reference spectra. The FTIR analyzer scanned the sample gas approximately once per second. A data point was generated every half minute as the co-addition of 32 scans.

FTIR quality assurance procedures followed USEPA Method 320. A calibration transfer standard (CTS) was analyzed before and after testing. Formaldehyde matrix spiking were performed before and after testing.

The analyte spikes were set to a target dilution ratio of 1:10 or less. Valid tests required spike recoveries to be within the Method 320 allowance of 100±30%.

The FTIR data is included in Appendix E. Figure 4-2 depicts the USEPA Method 320 sampling train.



#### Figure 4-2. USEPA Method 320 Sampling Train

#### 4.2 Process Data

DPI recorded process data during testing. EGLE personnel verified the requested operating and process data were recorded. Process data are included in Appendix F.

# 5.0 Quality Assurance and Quality Control

#### 5.1 QA/QC Procedures

Equipment used in this emissions test program passed quality assurance (QA) and quality control (QC) procedures. Refer to Appendix A for equipment calibrations. Before testing, the sampling equipment was cleaned, inspected, and calibrated according to procedures outlined in the applicable USEPA sampling method and USEPA's "Quality Assurance Handbook for Air Pollution Measurement Systems: Volume III, Stationary Source-Specific Methods."

#### 5.2 QA/QC Audits

Onsite QA/QC procedures (i.e., Pitot tube inspections, calibrations) were performed in accordance with the respective USEPA sampling methods. Equipment inspection and calibration measurements are presented in Appendix A.

#### 5.2.1 Audit Sample Results QA/QC

QA audit samples were not proposed during this test program. Currently, audit samples for the parameters to be measured are not available from the USEPA Stationary Source Audit Program.

#### 5.2.2 Instrument Analyzer QA/QC

The instrument analyzer sampling trains described in Section 4.1 were audited for measurement accuracy and data reliability. The analyzers passed the applicable calibration criteria. Table 5-1 summarizes the gas cylinders used during this test program. Analyzer calibration, bias, and drift data are included in Appendix A.

Parameter	Gas Vendor	Cylinder Serial Number	Cylinder Value	Expiration Date
Air	Airgas	CC469317	** **	07/17/2027
Propane	Airgas	ALM-036155	110.0 ppm	03/02/2028
Propane	Airgas	CC469695	1,113 ppm	03/02/2028
Hydrogen	Airgas	ALM-050640	99.999%	09/23/2029

# Table 5-1Calibration Gas Cylinder Information

#### 5.3 Data Reduction and Validation

The emissions testing Project Manager and/or the QA/QC Officer validated computer spreadsheets. The computer spreadsheets were used to ensure that field calculations were accurate. Random inspection of the field data sheets were conducted to verify data have been recorded appropriately. At the completion of a test, the raw field data were entered into computer spreadsheets to provide applicable onsite emissions calculations. The computer data were checked against the raw field sheets for accuracy during review of the report.

### 5.4 QA/QC Problems

Equipment audits and QA/QC procedures demonstrate sample collection accuracy and compliance for the test runs.

## 6.0 Limitations

The information and opinions rendered in this report are exclusively for use by Decorative Panels International, Inc. Apex Companies, LLC will not distribute or publish this report without consent of Decorative Panels International, Inc. except as required by law or court order. The information and opinions are given in response to a limited assignment and should be implemented only in light of that assignment. Apex Companies, LLC accepts responsibility for the competent performance of its duties in executing the assignment and preparing reports in accordance with the normal standards of the profession, but disclaims any responsibility for consequential damages

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# Tables

Apex Project No. 11021-000062.00 Decorative Panels International, Inc., Alpena, Michigan



# Table 1No. 1 Biofilter Emissions Results

**Decorative Panels International, Inc.** 

Alpena, Michigan

Apex Project No. 11021-000062.00 Sampling Date: November 30, 2021

Parameter		Units	Run 1	Run 2	Run 3	
Sampling	Start Time		8:51-9:51	10:11-11:11	11:34-12:34	Average
Duration		min	60	60	60	J
Inlet						
	Average Gas Stream Volumetric Flowrate	scfm	53,910	54,588	53,408	53,969
1	Gas Stream Percent Moisture Content	%	2.24	2.19	2.12	2.18
	Formaldehyde Concentration	ppmv, as CH <sub>2</sub> O	26.5	31.9	32.2	30.2
	Formaldehyde Concentration	ppmvd, as CH <sub>2</sub> O	27.1	32.6	32.9	30.9
	Formaldehyde Mass Emission Rate	lb/hr, as CH <sub>2</sub> O	6.7	8.1	8.0	7.6
	Methanol Concentration	ppmv, CH <sub>3</sub> OH	32.6	36.3	36.1	35.0
	Methanol Concentration	ppmvd, CH <sub>3</sub> OH	33.3	37.1	36.8	35.7
	Methanol Mass Emission Rate	lb/hr, as CH <sub>3</sub> OH	8.8	9,9	9.6	9.4
	Wiemanor Wass Emission Rate	io/iii, us crigori	0.0	,,,	2.0	2.4
	THC Concentration	ppmv, as propane	86.8	95.7	94.6	92.4
	THC Concentration	ppmv, as carbon	260.4	287.0	283.8	277.1
	THC Concentration	ppmvd, as carbon	266.4	293.4	290.0	283.2
	THC Mass Emission Rate	lb/hr, as propane	32.1	35.8	34.6	34.2
	THC Mass Emission Rate	lb/hr, as carbon	26.3	29.3	28.4	28.0
Outlet		- <u> </u>				
	Gas Stream Volumetric Flowrate	scfm	70,509	68,579	70,090	69,726
	Gas Stream Percent Moisture Content	%	2.80	2.95	3.05	2.93
	Formaldehyde Concentration	ppmv, as CH <sub>2</sub> O	0.48	0.70	0.78	0.65
	Formaldehyde Concentration	ppmvd, as CH <sub>2</sub> O	0.49	0.72	0.80	0.67
	Formaldehyde Mass Emission Rate	lb/hr, as CH <sub>2</sub> O	0.16	0.22	0.26	0.21
	Methanol Concentration	ppmv, CH₃OH	6.9	10.0	11.6	9.5
	Methanol Concentration	ppmvd, CH <sub>3</sub> OH	7.1	10.3	11.0	9.8
	Methanol Mass Emission Rate	lb/hr, as CH <sub>3</sub> OH	2.4	3.4	4.0	3.3
	Methanor Mass Emission Rate		2.4	5.4	4.0	5.5
	THC Concentration	ppmv, as propane	11.2	13.8	15.5	13.5
	THC Concentration	ppmv, as carbon	33.7	41.5	46.4	40.5
	THC Concentration	ppmvd, as carbon	34.7	42.8	47.8	41.7
	THC Mass Emission Rate	lb/hr, as propane	5.4	6.5	7.4	6.5
	THC Mass Emission Rate	lb/hr, as carbon	4.4	5.3	6.1	5.3
Formaldehyde Destruction Efficiency Results		%	98	97	97	<u> </u>
Methanol Destruction Efficiency Results		%	72	65	58	65
No. 1 Biofilter THC Destruction Efficiency Results		%	83	82	79	81
TTO T DIO		hr pound per hour			//	01
		m standard cubic feet per minut	e			
ppmv part per million by volume						
ppmvd part per million by volume dry basis						
	ppin	-IF Per minor of vorane u	-,			

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# **Figures**

