# SOURCE TEST REPORT <br> 2020 NOx, CO, AND PM TESTING FORD MOTOR COMPANY MICHIGAN ASSEMBLY PLANT WAYNE, MICHIGAN 

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For Submittal To:
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## EXECUTIVE SUMMARY

Montrose Air Quality Services (MAQS) was retained by Ford Motor Company (Ford) to evaluate NOx, CO, and PM from the outlet of the Hot Water Generator at the Michigan Assembly Plant in Wayne, Michigan. The emissions test program was conducted from February $6^{\text {th }}-7^{\text {th }}, 2020$. The purpose of this report is to document the results of the test program.

Testing consisted of triplicate 60-minute test runs for NOx and CO. Triplicate 180-minute test runs were conducted for PM. The results of the emission test program are summarized by Table I.

Table I
Overall Results Summary
Test Dates: February 6-7, 2020

| Source | Test Dates | $\mathbf{P M}$ <br> $(\mathbf{l b} / \mathbf{h r})$ | NOx <br> $(\mathbf{I b} / \mathbf{h r})$ | $\mathbf{C O}$ <br> $\mathbf{( \mathbf { l b } / \mathbf { h r } )}$ |
| :---: | :---: | :---: | :---: | :---: |
| Hot Water <br> Generator | February 6-7,2020 | $1.16 \mathrm{E}-02$ | 0.55 | 0.01 |

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## 1. Introduction

Montrose Air Quality Services (MAQS) was retained by Ford Motor Company (Ford) to evaluate NOx, CO, and PM from the outlet of the Hot Water Generator at the Michigan Assembly Plant in Wayne, Michigan. The emissions test program was conducted from February $6^{\text {th }}-7^{\text {th }}, 2020$. The purpose of this report is to document the results of the test program.

## 1.a Identification, Location, and Dates of Test

| System/Stack ID | Exhaust Gas Parameters to be <br> Evaluated | Date |
| :---: | :---: | :--- |
| Hot Water Generator | $\mathrm{NO}_{\mathrm{x}}, \mathrm{CO}$, \& PM Emission Rates | February 6-7, 2020 |

## 1.b Purpose of Testing

The purpose of the emissions test program was to verify $\mathrm{NOx}, \mathrm{CO}$, and PM to demonstrate overall control efficiency to comply with the requirements of Michigan Department of Environmental Quality Air Quality Division Permit No. MI-ROP-A8650-2016 for the Michigan Assembly Plant.

## 1.c Source Description

The source generates hot water for the e-coat and pre-treatment operations.

## 1.d Testing Personnel

Names and affiliations for personnel involved in the emissions test program are summarized by Table 1.

Table 1
Testing Personnel

| Name and Title | Affiliation | Telephone |
| :--- | :--- | :---: |
| Mr. Steve Smith <br> Client Project Manager | MAQS <br> 4949 Fernlee Ave. <br> Royal Oak, MI | (248) 548-8072 |
| Mr. Todd Wessel <br> Client Project Manager | MAQS <br> 4949 Fernlee Ave. <br> Royal Oak, MI | (248) 548-8070 |
| Mr. Dave Trahan <br> Environmental Technician | MAQS <br> 4949 Fernlee Ave. <br> Royal Oak, MI | (248) 548-8070 |


| Ms. Elizabeth Mathews Environmental Engineer | Ford Motor Company <br> Fairlane Plaza North <br> 290 Town Center Drive, Suite 800 <br> Dearborn, Michigan 48126 | (313)495-6054 |
| :---: | :---: | :---: |
| Ms. Susan Hicks Principal Environmental Engineer | Ford Motor Company Fairlane Plaza North 290 Town Center Drive, Suite 800 Dearborn, Michigan 48126 | (313)594-3185 |
| Mr. Mark Dziadosz EGLE <br> Air Quality Division | EGLE - Environmental, Great Lakes, \& Energy SE Michigan District 27700 Donald Ct Warren, MI 48092 | (586)753-3745 |
| Mr. Steve Weiss EGLE <br> Air Quality Division | EGLE - Environmental, Great Lakes, and Energy Michigan AQD, Cadillac Place 3058 W. Grand Blvd, Suite 2-300 Detroit, MI 48202-6058 | (313)456-4688 |

## 2. Summary of Results

Sections 2.a through 2.d summarize the results of the emissions test program.

## 2.a Operating Data

Process operating data for this emissions test program is provided in Appendix D .

## 2.b Applicable Permit

The applicable permit for this emissions test program is Permit No. PTI-192-17.

## 2.c Results

The results of the emissions test program are summarized by Table 2. Detailed data for each test run can be found in Tables 3-4.

Table 2
Overall Results Summary
Test Dates: February 6-7, 2020

| Source | Test Dates | PM <br> $(\mathbf{l b} / \mathbf{h r})$ | NOx <br> $(\mathbf{l b} / \mathbf{h r})$ | CO <br> $(\mathbf{l b} / \mathbf{h r})$ |
| :---: | :---: | :---: | :---: | :---: |
| Hot Water <br> Generator | February 6-7, 2020 | $1.16 \mathrm{E}-02$ | 0.55 | 0.01 |

## 2.d Emission Regulation Comparison

## NA

## 3. Source Description

Sections 3.a through 3.d provide a detailed description of the process.

## 3.a Process Flow Diagram

Due to the simplicity of the process, a process flow diagram is not applicable.

## 3.b Process Description

The source generates hot water for the e-coat and pre treatment operations baths.

## 3.c Raw and Finished Materials

NA

## 3.d Process Capacity

NA

## 3.e Process Instrumentation

Process data was collected by Ford personnel and can be found in Appendix D.

## 4. Sampling and Analytical Procedures

Sections 4.a through 4.d provide a summary of the sampling and analytical procedures used to verify emission rates and removal efficiency.

## 4.a Sampling Train and Field Procedures

## USEPA Methods 1-4

Stack gas velocity traverses were conducted in accordance with the procedures outlined in Methods 1 and 2. An S-type pitot tube with a thermocouple assembly, calibrated in accordance with Method 2, Section 4.1.1, was used to measure exhaust gas velocity pressures (using a manometer) and temperatures at each traverse location. The S-type pitot tube dimensions were within specified limits, therefore, a baseline pitot tube coefficient of 0.84 (dimensionless) was assigned.

A cyclonic flow check was performed at each sampling location. The existence of cyclonic flow is determined by measuring the flow angle at each sample point. The flow angle is the angle between the direction of flow and the axis of the stack. If the average of the absolute values of the flow angles is greater than 20 degrees, cyclonic flow exists. Both
sampling locations were evaluated for cyclonic flow and deemed acceptable for flowrate measurement.

Exhaust gas molecular weight was determined according to Method 3. The equipment used for the Method 3 evaluation consisted of a one-way squeeze bulb with connecting tubing and a set of Fyrite ${ }^{\circledR}$ combustion gas analyzers. $\mathrm{CO}_{2}$ and $\mathrm{O}_{2}$ content was analyzed using the Fyrite ${ }^{\circledR}$ procedure.

Exhaust gas moisture content was evaluated using Method 4 with triplicate test runs conducted at the outlet. Exhaust gas was extracted and passed through (i) two impingers, each with 100 ml deionized (DI) water, (ii) an empty impinger, and (iii) an impinger filled with silica gel. Exhaust gas moisture content was then determined volumetrically (liquid impingers) and gravimetrically (silica gel impinger). A schematic drawing of the Method 4 sampling train is provided as Figure 19.

## USEPA Method 7E

The NOx content of the gas stream was measured using a Teledyne NOx gas analyzer. The gas stream was drawn through a stainless-steel probe with a heated in-line filter to remove any particulate, a heated Teflon ${ }^{\circledR}$ sample line, through a refrigerated Teflon ${ }^{\circledR}$ sample conditioner to remove the moisture from the sample before it entered the NOx analyzer. Data was recorded on a PC equipped with data acquisition software. Recorded NOx concentrations were averaged and reported for the duration of each 60-minute test (as drift corrected per Method 7E). A drawing of the sampling train used for the testing program is presented as Figure 23.

In accordance with Method 7E, a 3-point (zero, mid, and high) bias check and calibration check was performed on the NOx analyzer prior to initiating the test program. Following each test run, a 2-point (zero and high) calibration drift check was performed. The NOx analyzer was operated at the $0-100 \mathrm{ppm}$ range.

## USEPA Method 10

The CO content of the exhaust gas was evaluated according to procedures outlined in 40 CFR 60, Appendix A, Method 10. The CO content of the gas stream was measured using a Teledyne CO gas analyzer. The gas stream was drawn through a stainless-steel probe with a heated in-line filter to remove any particulate, a heated Teflon ${ }^{\circledR}$ sample line, through a refrigerated sample conditioner with a peristaltic pump to remove the moisture from the sample before it entered the analyzer. Data was recorded on a PC equipped with Labview ${ }^{\circledR}$ II data acquisition software. Recorded CO concentrations were averaged and reported for the duration of each 60-minute test (as drift corrected per Method 7E). The analyzer was calibrated for a range of 0 to 100 ppm .

In accordance with Method 10, a 3-point (zero, mid, and high) calibration check was performed on the CO analyzer. Calibration drift checks were performed at the completion of each run.

## Method 5/202

40 CFR 60, Appendix A, Method 5, "Determination of Particulate Emissions from Stationary Sources" and 40 CFR 60, Appendix A, Method 202, "Dry Impinger Method for Determining Condensable Particulate Emissions from Stationary Sources" was used to measure PM concentrations and calculate PM emission rates (see Figure 21 for a schematic of the sampling train). Triplicate 180-minute test runs were conducted for each source.

MAQS' Nutech ${ }^{\circledR}$ Model 2010 modular isokinetic stack sampling system consisted of (1) a stainless-steel nozzle, (2) a steel probe, (3) a heated filter holder, (4) a vertical condenser, (5) an empty pot bellied impinger, (6) an empty modified Greenburg-Smith (GS) impinger, (7) unheated filter holder with a teflon filter, (8) a second modified GS impinger with 100 ml of deionized (DI) water, and a third modified GS impinger containing approximately 300 g of silica gel desiccant, (9) a length of sample line, and (10) a Nutech ${ }^{\circledR}$ control case equipped with a pump, dry gas meter, and calibrated orifice.

A sampling train leak test was conducted before and after each test run. After completion of the final leak test for each test run, the filter was recovered, and the nozzle and the front half of the filter holder assembly were brushed and triple rinsed with acetone. The acetone rinses were collected in a pre-cleaned sample container. The impinger train was then purged with nitrogen for one hour at a flow rate of 14 liters per minute. The CPM filter was recovered and placed in a petri dish. The back half of the filter housing, the condenser, the pot bellied impinger, the moisture drop out impinger, and the front half of the CPM filter housing and all connecting glassware were triple rinsed with deionized (DI) water which was collected in a pre-cleaned sample container. The same glassware was then rinsed with acetone which was collected in a pre-cleaned sample container labeled as the organic fraction. The glassware was then double rinsed with hexane which was added to the same organic fraction sample bottle.

MAQS labeled each container with the test number, test location, and test date, and marked the level of liquid on the outside of the container. In addition, blank samples of the acetone, DI water, hexane, and filter were collected. MAQS personnel carried all samples to MAQS' laboratory (for filter and acetone gravimetric analysis) in Royal Oak, Michigan. DI water and organic samples were hand delivered to Bureau Veritas for analysis.

## 4.b Recovery and Analytical Procedures

All recoveries were performed according to the correct USEPA Method.

## 4.c Sampling Ports

The outlet sampling locations satisfy the minimum criteria for Method 1.

## 4.d Traverse Points

Stack traverse point diagrams are appended as Figure 1.

## 5. Test Results and Discussion

The detailed results can be found in Tables 3 and 4. The hot water generator would shut down intermittently as the process did not require hot water continuously which resulted in brief gaps in the testing. These occurrences were discussed with Mr. Weiss and Mr. Dziadosz.

## 5.a Results Tabulation

The results of the emission test program are detailed in Tables 3-4.

## 5.b Sampling Procedure Variations

Due to the different length of runs for PM and gases, MAQS did a separate flow for run 1 of the gases. Then run 2 and 3 from the PM runs were used for 2 and 3 of the gas runs.

## 5.c Process or Control Device Upsets

No upset conditions occurred during testing.

## 5.d Control Device Maintenance

There has been no major maintenance performed during the past three months.

## 5.e Retest

This test program was not a re-test.

## 5.f Audit Sample Analyses

No audit samples were collected as part of the test program.

## 5.g Calibration Sheets

Relevant equipment calibration documents are provided as Appendix B.

## 5.h Sample Calculations

Sample calculations are provided in Appendix C.

## 5.i Field Data Sheets

Field documents are presented as well as raw analyzer test data (provided electronically on CD) are provided in Appendix A.

## 5.j Laboratory Data

The laboratory data can be found in Appendix E

## REVIEW AND CERTIFICATION

All work, calculations, and other activities and tasks performed and presented in this document were carried out by me or under my direction and supervision. I hereby certify that, to the best of my knowledge, Montrose operated in conformance with the requirements of the Montrose Quality Management System and ASTM D7036-04 during this test project.

Signature: $\qquad$ Date: $\qquad$

Name: $\qquad$ Title: $\qquad$

I have reviewed, technically and editorially, details calculations, results, conclusions, and other appropriate written materials contained herein. I hereby certify that, to the best of my knowledge, the presented material is authentic, accurate, and conforms to the requirements of the Montrose Quality Management System and ASTM D7036-04.

Signature: $\qquad$ Date: $\qquad$

Name: $\qquad$ Title: $\qquad$

## Tables

Table 3
Hot Water Generator NOx and CO Emission Rates
Ford
Wayne, Michigan
MAQS Project 049AS-60143
Sampling Dates: February 6, 2020

| Parameter | Run 1 | Run 2 | Run 3 | Average |
| :---: | :---: | :---: | :---: | :---: |
| Test Run Date | 2/6/2020 | 2/6/2020 | 2/6/2020 |  |
| Test Run Time | 7:23-8:25 | 8:38-9:38 | 10:38-11:38 |  |
| Outlet Flowrate (dscfm) | 2,358 | 2,365 | 2,388 | 2,370 |
| Outlet Oxides of Nitrogen Concentration (ppmv) | 31.04 | 30.23 | 31.77 | 31.01 |
| Outlet NOx Concentration (ppmv, corrected as per USEPA 7E) | 32.29 | 31.39 | 33.17 | 32.28 |
| NOx Emission Rate (lb/hr) | 0.52 | 0.51 | 0.54 | 0.52 |
| NOx Emission Rate (lb/hr) (corrected as per USEPA 7E) | 0.54 | 0.53 | 0.57 | 0.55 |
| Outlet Carbon Monoxide Concentration (ppmv) | -0.48 | 1.00 | -0.39 | 0.04 |
| Outlet CO Concentration (ppmv, corrected as per USEPA 7E) * | 0.00 | 1.49 | 0.11 | 0.53 |
| CO Emission Rate (lb/hr) | 0.00 | 0.01 | 0.00 | 0.00 |
| CO Emission Rate (lb/hr) (corrected as per USEPA 7E) | 0.00 | 0.02 | 0.00 | 0.01 |


| NOx Correction |  |  |  |
| :--- | ---: | ---: | ---: |
| Co | 0.30 | 0.54 | 0.40 |
| Cma | 50.36 | 50.36 | 50.36 |
| $\mathbf{C m}$ | 48.25 | 48.17 | 48.03 |


| CO Correction |  |  |  |
| :--- | ---: | ---: | ---: |
|  |  |  |  |
| Co | -0.28 | -0.48 | -0.50 |
| Cma | 49.84 | 49.84 | 49.84 |
| $\mathbf{C m}$ | 49.05 | 48.89 | 48.92 |

*Run 1 corrected per 7E resulted in a negative number. This was replaced with zero.
scfm $=$ standard cubic feet per minute
$\mathrm{dscfm}=$ dry standard cubic feet per minute
ppmv = parts per million on a volume-to-volume basis
$\mathrm{lb} / \mathrm{hr}=$ pounds per hour
MW = molecular weight ( $\mathrm{CO}=28.01, \mathrm{NOx}=46.01$ )
$24.14=$ molar volume of air at standard conditions ( $70^{\circ} \mathrm{F}, 29.92^{\prime \prime} \mathrm{Hg}$ )
$35.31=\mathrm{ft}^{3}$ per $\mathrm{m}^{3}$
$453600=\mathrm{mg}$ per lb
Response factor obtained from introducing propane into methane analyzer:
$\mathrm{Co}=$ Average of initial and final zero gases
$\mathrm{Cma}=\mathrm{Actual}$ concentration of the calibration gas
$\mathrm{Cm}=$ Average of initial and final calibration gases
$\mathrm{C}_{\mathrm{c}}=\mathrm{KC}_{\text {meas }}$
where $\mathrm{Cc}=$ Concentration as Carbon (ppmv), $\mathrm{K}=$ Carbon equivalent correction factor ( 3 for Propane)
and $\mathrm{C}_{\text {meas }}=$ concentration as measured (as propane)
emission rate calculated on dry basis
${ }^{2}$ emission rate calculated on wet basis

## Equations

$\mathrm{lb} / \mathrm{hr}=\mathrm{ppmv} * \mathrm{MW} / 24.14 * 1 / 35.31 * 1 / 453,600 *$ scfin $* 60$ for VOC
$\mathrm{lb} / \mathrm{hr}=\mathrm{ppmv} * \mathrm{MW} / 24.14$ * 1/35.31 * 1/453,600 * dcfm * 60
Conc $_{\text {@15\%02 }}=$ Conc $*(20.9-15) /\left(20.9-\% O_{2}\right)$

Table 4
Particulate Matter Emission Rates


Figures




Calibration Gas

Figure No. 3

Site:
USEPA Method 7E/10
Ford Michigan Assembly Plant Wayne, Michigan

Sampling Dates:
February 6-7, 2020

Montrose Air Quality Services 4949 Fernlee Ave Royal Oak, Michigan 48073

